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1 Multi-scale measurements and temporally resolved modeling of methane emissions at 2 natural gas distribution stations

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10 11 **Abstract**

12 Methane (CH₄) emissions from natural gas distribution stations are not well characterized by
13 measurements, contributing to uncertainty in urban emissions inventories and mitigation
14 strategies. We conducted a multi-scale, multi-temporal study of four distribution stations in
15 Calgary, Alberta, combining component- and facility-level measurements with modeling to
16 quantify, attribute, and compare emissions rates. Component-level surveys found low-emitting
17 and readily abatable fugitive emissions, vents, and emissions from catalytic heaters, which
18 accounted for 1.6–40.1% of total emissions. Facility-level measurements using the human-
19 portable flux plane method revealed comparatively higher rates of 3.4×10^{-2} to 7.4 kg CH₄/h that
20 were correlated with throughput, with most emissions attributed to incomplete combustion from
21 line heaters that combust process gas prior to pressure regulation. To compare measured with
22 conventional rate estimates, we developed a Monte Carlo-based modeling framework integrating
23 component-level rates, historical leak detection data, gas throughput, and source-specific
24 emission factors (EFs). Measured rates exceeded modeled rates by factors of 1.6–148.3. Across
25 all measurements, facility-level rates totaled 17.4 kg CH₄/h (10.8–24.1 kg CH₄/h); modeled rates
26 totaled 2.3 kg CH₄/h (0.9–4.2 kg CH₄/h). Overall, results suggest that conventional approaches
27 underestimate distribution station CH₄ emissions because underlying EFs underrepresent
28 emissions from equipment incompletely combusting natural gas.

29
30 **Keywords:** methane emissions, natural gas distribution, transmission distribution transfer
31 stations, city gate stations, detection, quantification, modeling, incomplete combustion

32 33 **1. Introduction**

34 In the U.S. and Canada, natural gas is a prominent fuel used for electricity generation, space and
35 water heating, and cooking in residential and commercial sectors (Canada Energy Regulator
36 (CER), 2024; U.S. Energy Information Administration (EIA), 2024). In major cities and urban
37 areas in these countries, natural gas consumers are abundant and distributed widely, requiring an
38 extensive system of facilities, distribution pipelines, and meters to regulate pressures, deliver the
39 gas, and measure volumes. Methane (CH₄)—the principal component of natural gas and a potent
40 greenhouse gas—can enter the atmosphere from this infrastructure intentionally through venting

41 or unintentionally from leaks or accidents (e.g., hit lines). These releases warm the climate
42 (Szopa et al., 2021) and in cases can degrade urban air quality as an ozone precursor (Monks et
43 al., 2015). CH₄ is also emitted from the exhaust of equipment and appliances that combust
44 natural gas as combustion is never fully complete (Fischer et al., 2018; Merrin and Francisco,
45 2019; Lebel et al., 2020, 2022; Saint-Vincent and Pekney, 2020). In aggregate, the distribution
46 and use of natural gas can be a large source of urban CH₄ emissions in the U.S. and Canada
47 given the scale of infrastructure with potential to emit and large number of end users (Vollrath et
48 al., 2025).

49 At the city scale, atmospheric measurements and source attribution studies show that
50 emissions from natural gas systems contribute substantially to urban CH₄ budgets in the U.S. and
51 Canada, and in many cases dominate the emissions profile (Vollrath et al., 2025). This
52 dominance is not universal; landfills have been identified as a primary source in some cities,
53 such as the San Francisco Bay Area (Jeong et al., 2017; Guha et al., 2020), and suggested by
54 limited ground-based measurements in Montreal and Toronto (Ars et al., 2020; Williams et al.,
55 2022; Gonzalez Moguel et al., 2025). Regardless, natural gas systems can emit large quantities of
56 CH₄ in urban areas, and research is required to better understand the parts of the natural gas
57 system that drive emissions (Zhang et al., 2023; Vollrath et al., 2025).

58 To date, most urban natural gas CH₄ measurements in the U.S. and Canada have focused
59 on detecting subsurface leaks from distribution pipelines using vehicle-based surveys and surface
60 techniques, revealing strong links between pipeline material and leak propensity. This supports
61 mitigation through targeted repairs (e.g., Phillips et al., 2013; Jackson et al., 2014; Lamb et al.,
62 2015; Hendrick et al., 2016; von Fischer et al., 2017; Weller et al., 2020; 2022; Edwards et al.,
63 2021; Vogel et al., 2024). However, pipeline leaks represent only one component of urban natural
64 gas emissions, and studies show that in cities with limited or no cast iron infrastructure, pipeline-
65 related CH₄ emissions are comparatively low (Ars et al., 2020; Weller et al., 2022; Vogel et al.,
66 2024). Other natural gas sources are likely to be important. Measurements of these non-pipeline
67 sources remain limited: (i) distribution stations (Lamb et al., 2015; Hugenholtz et al., 2021), (ii)
68 metering and regulating facilities (Williams et al., 2022), (iii) valve vaults (Gallagher et al.,
69 2015), (iv) farm tap units, (v) customer meters (Williams et al., 2022; Newton et al., 2024;
70 Vollrath et al., 2024), (vi) post-meter leaks (Fischer et al., 2018), and (vii) end-use incomplete
71 combustion emissions (Merrin and Francisco, 2019; Lebel et al., 2020, 2022; Saint-Vincent and
72 Pekney, 2020). Among these, natural gas distribution stations (also referred to as transmission-
73 distribution transfer or city gate stations) are particularly understudied despite being common,
74 above-ground facilities with multiple emission pathways, including fugitives, vented emissions,
75 and equipment with incomplete combustion.

76 Distribution stations primarily exist to decrease gas pressure from transmission lines
77 (~600 psi) into lower pressure neighborhood lines (60-100 psi). Neighborhood lines connect to
78 point of use meter-sets (Vollrath et al., 2024), and beyond this, individual appliances.
79 Neighborhood lines must be fed in different locations throughout a city to maintain pressure and
80 balance gas use. Transmission lines use higher pressures fed by compressor stations to facilitate

81 flow of very large volumes of gas over long distances. Neighborhood lines use lower pressures to
82 provide safe, controlled delivery of smaller gas volumes for customers and reduce leak potential
83 under roads. Although system design varies throughout different cities, this multi-pressure design
84 requires distribution stations throughout a city to feed the neighborhood lines.

85 Decreasing gas pressure at distribution stations through regulators generates immense
86 cooling due to the Joule-Thompson effect, causing issues with gas condensation and icing that
87 are closely related to gas throughput (not necessarily ambient temperature). Line heaters are used
88 to heat the gas before pressure decrease to mitigate these effects. Some distribution stations (such
89 as those in Calgary which are typical of Canadian and U.S. cities) have line heaters and
90 additional equipment to treat, measure, or control gas flows. Line heaters combust process gas,
91 and any incompletely combusted gas—including CH₄—is emitted to the atmosphere in exhaust.
92 Process gas volumes used by line heaters change with station throughput and seasonal operating
93 changes due to demand, resulting in variability to operational and total station CH₄ emissions
94 rates.

95 Measuring and attributing all CH₄ emissions at natural gas distribution stations is
96 challenging, presenting an opportunity to improve the characterization and understanding of
97 emissions. For example, fugitive and vented emissions from components and equipment are
98 typically located closer to the ground and can be measured with conventional measurement
99 methods. In contrast, line heater exhaust containing incompletely combusted CH₄ is emitted from
100 a height of ~5m a.g.l. and is hot and slightly buoyant. Conventional methods typically cannot
101 measure elevated or otherwise difficult- or unsafe-to-measure sources. Thus, to our knowledge,
102 incomplete combustion CH₄ emissions from line heaters are missing from aggregated
103 component-level rates in existing studies of distribution stations in the U.S. and Canada, where
104 rates have been used in national-level inventories (e.g., Lamb et al., 2015; Williams et al., 2022).
105 Outside the fenceline, facility-level methods are one approach to measure emissions from all
106 sources on site, including tall sources like line heaters, and independently confirm emissions.
107 Research has provided a limited number of total estimates at stations (Hugenholtz et al., 2021).
108 However, when CH₄ is measured from a standoff distance downwind, the emissions generally
109 cannot be attributed to specific components and processes on site, hindering a better
110 understanding of where the majority of the emissions are coming from. These examples highlight
111 the limitations of individual methods and the opportunity to address the problem with a broader
112 set of approaches.

113 To advance understanding of CH₄ emissions from these sites, this study combines multi-
114 scale and multi-temporal measurements with modeling at four natural gas distribution stations in
115 Calgary, Alberta, Canada. Notably, we demonstrate the use of the human-portable flux plane
116 method to quantify total station emissions, including incompletely combusted CH₄ from line
117 heaters, representing a novel application of the approach (Vollrath et al., 2026). We attribute
118 emissions using the multi-scale measurements and observations, identifying incomplete
119 combustion from line heaters as the dominant contributor to stations' emissions. To capture
120 temporal variability not typically resolved in estimates based on conventional approaches, we

121 also developed a Monte Carlo-based modeling framework to estimate CH₄ emissions from the
122 stations, enabling a temporally resolved comparison with facility-level measurements. The
123 framework integrates component-level rates from this study, historical leak detection data, gas
124 throughput, and common source-specific emission factors (EFs). Comparison of modeled and
125 facility-level estimates indicated that conventional approaches underestimate CH₄ emissions
126 from distribution stations due to generic EFs substantially underrepresenting incomplete
127 combustion emissions from equipment, with broader implications for estimates of CH₄ emissions
128 from natural gas end use.

129

130 **2. Methodology**

131 *2.1. Background and station selection*

132 The City of Calgary had a population of 1,306,780 in 2021 (City of Calgary, 2025) and relies
133 primarily on natural gas for meeting the city's electricity demand, as well as residential and
134 commercial space heating. The city has a continental climate with strong seasonal temperature
135 variability (mean daily air temperature is 4.5 °C for 1991-2020) and unique weather patterns,
136 including 'chinook' downslope winds from the Rocky Mountains that warm and dry the air.
137 Natural gas demand fluctuates dramatically on weekly and seasonal timescales. According to
138 local gas utility data, 41 distribution stations operate across Calgary to regulate gas pressure and
139 deliver supply to residential, commercial, and industrial users, with two additional stations under
140 construction and a third proposed to accommodate urban growth and rising demand.

141 Distribution stations vary in size, complexity, and throughput, with larger facilities
142 generally having higher potential to emit CH₄ due to more components, larger or more numerous
143 pieces of equipment, and increased operational emissions due to throughput demand. For this
144 study, we selected four stations—three large and one medium-sized—based on their accessibility,
145 suitability for multi-method measurements, and physical characteristics that facilitated accurate
146 facility-level measurements. Selected stations had porous fencelines, limited nearby obstructions,
147 and line heaters with low-exit-velocity exhaust stacks, positioned so that plumes could be
148 effectively captured in the vertical dimension.

149 Figure 1 shows the selected facilities, distributed across the city, with Table 1 detailing
150 basic attributes (see also S1). Stations A and B were large, full-time operations. Stations C and D
151 were smaller and seasonal, with operation dependent on natural gas demand. The primary
152 purpose of these stations is pressure regulation from transmission pressures (~600 psi) to
153 neighborhood line pressures (60-100 psi). In Calgary, point of use meter sets further regulate
154 pressure prior to entering buildings. Gas metering was present at all sites, but Station B had a gas
155 chromatograph to monitor gas composition. To manage cooling associated with pressure
156 reductions, the stations had line heaters, of varying type, number, and size. All stations had
157 equipment inside of process buildings, and to manage cold weather, these building were often
158 equipped with catalytic heaters, although not all were operational. None of these sites had
159 compressors or odorant injection equipment; odorization occurs upstream. None of these sites
160 were dominantly powered by mains electricity, instead using self-generated energy for power.

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Table 1. Simplified site attributes, see S1 for additional discussion.

Equipment / Processes	Station A	Station B	Station C	Station D
Pressure regulation	Yes	Yes	Yes	Yes
Pneumatic valves with vents	Yes	No	Yes	No
Liquid separators	No	Large	Small	Very small
Catalytic heaters	Yes	Yes	Yes, non-operational	No
Self-generated energy (with thermal electric or other generator)	Yes (thermal electric)	Yes (generator)	Yes (thermal electric)	Yes (thermal electric)
Gas chromatograph with vent	No	Yes	No	No
Line heaters	Vacuum-style	Vacuum-style	Vacuum-style	Bath-style
General operation status	Full-time	Full-time	Seasonal	Seasonal
Flow meters	Yes	Yes	Yes	Yes
Process buildings	Yes	Yes	Yes	Yes

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165



166
 167 **Figure 1.** Natural gas distribution stations in Calgary, AB selected for component- and facility-
 168 level measurements.

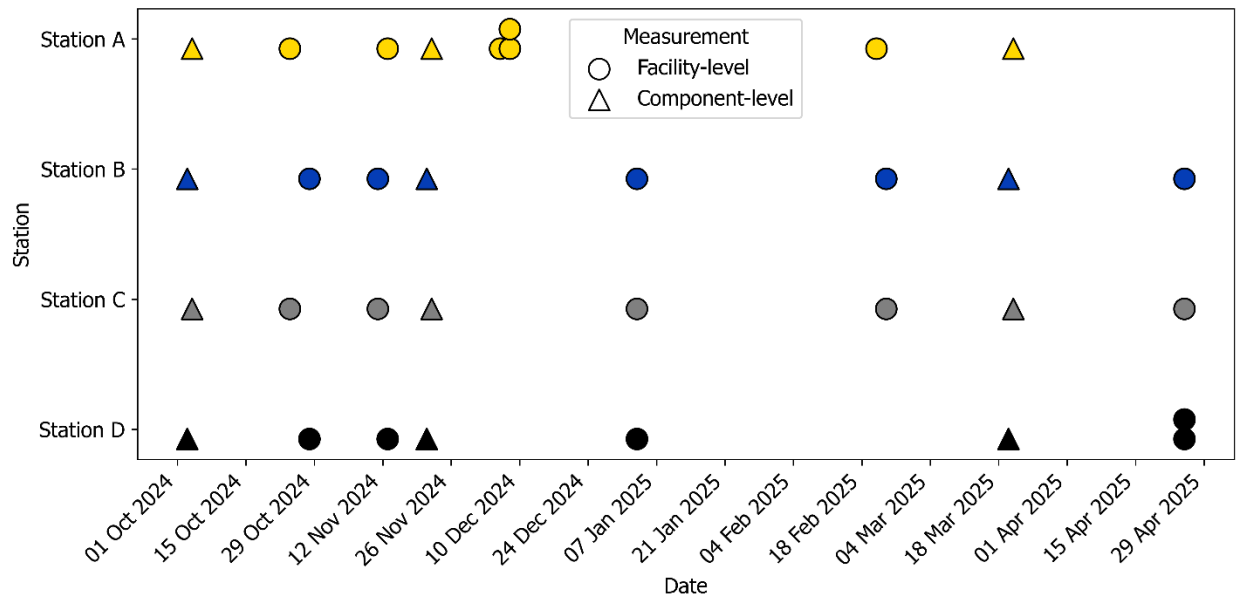
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 171 *2.2. Measurement approach and methods*

172 *2.2.1. Overview*

173 We measured CH₄ emissions at the four stations using a combination of component- and facility-
 174 level techniques. The local natural gas utility provided site access for component-level surveys,
 175 as well as historical leak detection and gas throughput data, while station operators helped
 176 contextualize the survey findings. The primary purpose of the component-level surveys was to
 177 identify CH₄ emission sources and quantify their rates where possible. Each station was surveyed
 178 three times between October 2024 and March 2025, with survey dates summarized alongside
 179 facility-level measurement dates in Figure 2.

180 Facility-level CH₄ emissions were measured from outside station fencelines, four to six
 181 times at each station over a slightly longer period than the component-level surveys (Figure 2).
 182 To investigate short-term variability in emission rates, we conducted two repeat facility-level
 183 measurements approximately one hour apart at Stations A and D on 8 December 2024 and 25
 184 April 2025, respectively (Figure 2).

185



186
 187 **Figure 2.** Timeline of measurements at the stations. Marker color is varied by station and shape
 188 is varied by measurement type—component- or facility-level. Repeat facility-level
 189 measurements were performed approximately one-hour apart at Stations A and D on the 8
 190 December 2024 and 25 April 2025, respectively to explore short-term temporal variability to
 191 CH₄ emissions rates. The repeat measurements are shown in the figure as the stacked circular
 192 markers.

193
 194

195 *2.2.2. Component-level surveys*

196 *2.2.2.1. CH₄ emissions detection*

197 We used a FLIR GF320 optical gas imaging (OGI) camera to detect CH₄ emissions from
 198 components at the four distribution stations. We imaged all infrastructure at the stations with
 199 potential to emit CH₄ from a distance of approximately 3 m or less, consistent with regulatory-
 200 mandated work practices for OGI surveys in the oil and gas production sector (AER, 2020).

201 Zimmerle et al. (2020) found that OGI had a 90% probability of detection (POD) of 1.6
 202 kg CH₄/h for inexperienced operators, ranging to 0.13 kg CH₄/h for experienced operators. The
 203 largest source we quantified in the on-site surveys was emitting between 0.16 kg CH₄/h and 0.23
 204 kg CH₄/h, which was easily detectable with OGI, suggesting either operator experience or good
 205 conditions for OGI surveys. We note that slow survey speeds may have improved our probability
 206 of detecting small leaks with OGI. Some small leaks were detected using mercaptan (CH₃SH)
 207 odor and snoop—a soapy water solution—when OGI effectiveness or efficiency was lower
 208 compared to these methods in some cases (see §3.1 for more details).

209

210 *2.2.2.2. Component-level CH₄ emissions quantification*

211 Detected sources of CH₄ emissions were quantified using a HETEK hi-flow sampler when
 212 emitting at rates sufficient for quantification. This included fugitive emissions (leaks) and vents.

213 We also quantified CH₄ emissions in the exhaust of catalytic heaters, which were accessible from
214 the ground and generally low-temperature such that they could be reliably quantified without
215 damaging the instrument. The hi-flow has a rated accuracy of ±10% and has a rated lower
216 quantifiable limit of 5.0×10^{-3} kg CH₄/h depending on the operating mode. We calibrated the hi-
217 flow several times throughout the study period following manufacturer specifications.

218 We did not quantify CH₄ emissions when the characteristics of the emissions or source
219 height created limitations for the instruments or potential safety issues. CH₄ emissions from the
220 catalyst panels (Festa-Bianchet et al., 2024) on the catalytic heaters at Stations A and B were
221 detected but not quantified due to ambiguity over where the CH₄ was coming from. CH₄ was
222 seeping from multiple locations on the pads and mixing, creating challenges for capturing all
223 emissions. Furthermore, the temperature of the catalyst panels was high and could have damaged
224 the hi-flow bag attachment. We also did not quantify CH₄ emissions from line heater exhaust
225 stacks due to their height and temperature.

226 Some leaks were detected but emitting at rates insufficient for quantification. Also, in the
227 component-level surveys on 20 and 21 of March 2025 (Figure 2), we faced a firmware issue with
228 the hi-flow and could not quantify a number of sources. The issue was resolved and explored in a
229 future update and servicing (A. Mohan, personal communication, April 15, 2025). To mitigate,
230 for very low-emitting leaks we used the lower rated quantification limit of the instrument as the
231 emissions rate. For other sources that could not be quantified on these dates, the rate for the same
232 source quantified in a different survey or the mean of multiple quantifications of the same source
233 (if quantified in > 1 survey) was used as the emissions rate.

234

235 *2.2.3. Facility-level measurements*

236 *2.2.3.1. Pole-based flux plane method*

237 In addition to component-level measurements, we quantified CH₄ emissions at the facility-level
238 in a novel application of the mobile “flux plane” technique—a mass balance method commonly
239 used with quadrotor drones (Corbett and Smith, 2022)—with a human-portable, telescoping
240 pole-based system (see Vollrath et al., 2026). Vollrath et al. (2026) found that the pole-based flux
241 plane method achieved a mean relative error of -10.1% across a series of 44 controlled release
242 tests, where 68% of estimates were within ±38.3% of the release rates—providing an indication
243 of the expectable accuracy of this technique in this application.

244 For this study, all equipment was identical to that used by Vollrath et al. (2026) with the
245 exception of a taller pole to expand vertical coverage to 8.1 m. The line heater plumes were
246 emitted at ~5 m a.g.l. and were slightly buoyant; however, with low exit velocity. We examined
247 weather and wind forecasts to target periods with stable atmospheres and moderate to high wind
248 speeds to limit vertical plume rise.

249 We followed the same work practice to perform the pole measurements as documented in
250 Vollrath et al. (2026); however, real-world use of the method required an additional “screening”
251 step. Upon arriving at the stations, the pole operator studied the wind direction and identified the
252 plume’s location using the kit’s backpack-mounted LI-COR 7810 (LI-7810) trace gas analyzer.

253 This information, along with consideration of the terrain surrounding the stations, was used to
254 optimize the location where the measurements would be performed. A total of 21 facility-scale
255 measurements were performed across the stations over the study period (Figure 2).

256 Overall, data processing and quantification were performed on 20 out of the 21
257 measurements after quality-assuring the data following the protocol developed by Vollrath et al.
258 (2026) for pole-based flux plane measurements (see S2).

259

260 *2.2.3.2. Wind speed and direction*

261 During the facility-level measurements, wind speed and direction were measured from an
262 anemometer deployed nearby in an area free from obstructions. We used a TriSonica Mini (TSM)
263 anemometer at a height of 1.9 m to measure wind from 24 October 2024 to 03 January 2025 but
264 switched to an RM Young (RMY) 81000 at a height of 2.2 m for measurements on 21 February
265 2025 and afterwards. More details on the wind measurements, the approach to address data gaps
266 on two days, and estimating a vertical speed wind profile for quantification with the flux plane
267 method (Vollrath et al., 2026) are provided in S3.

268 Winds speeds were measured with the TSM and RMY on 21 February 2025 for
269 comparison (Figure S1). Mean wind speeds for the CH₄ measurement on this date were 5.0 m/s
270 (standard deviation = 1.8 m/s) and 4.4 m/s (standard deviation = 1.7 m/s) with the TSM and
271 RMY, respectively. Wind speeds from the RMY were adjusted for height using the method in S3
272 to match the height of the TSM. Wind speed is a direct multiplier in quantifying CH₄ emissions
273 rates with the flux plane method (Vollrath et al., 2026). Therefore, results from this single
274 experiment indicate that CH₄ rate estimates would be 14% higher using TSM rather than RMY
275 wind speeds.

276

277 *2.2.4 Monte-Carlo modeling framework*

278 Comparing measurements of CH₄ emissions with conventional (i.e., inventory) estimates can
279 help identify discrepancies to improve estimates and provide new insights on emissions for
280 mitigation. However, in some cases the two are not directly comparable. Emissions vary
281 temporally, and distribution stations have different equipment to meter and regulate gas, both
282 throughout the city of Calgary and internationally. The local gas utility's inventory includes
283 estimates of emissions from their distribution stations, but rates are aggregated and annualized,
284 requiring downscaling. This renders comparison with snapshot facility-level measurements
285 largely unhelpful. To address these issues, we developed a time-resolved Monte Carlo-based
286 modeling framework to produce an emissions estimate at any given time for individual stations.

287 To simplify we use four CH₄ source categories at the stations: fugitives (leaks), vents,
288 catalytic heater exhaust, and line heater exhaust. We generate emissions for each of these sources
289 on a given day using source counts, measurement data (from the component-level and historic
290 leak detection surveys), gas throughput data, source-specific emissions factors (EFs), and
291 knowledge of source characteristics and behavior at the stations (e.g., seasonal operating

292 changes). Each of the four stations were individually modeled owing to their slightly different
293 characteristics, equipment, and operation (see Table 1 and S1).

294 Measured fugitive, vent, and catalytic heater exhaust rates were aggregated into source-
295 specific emissions rate distributions for the model. The vent class had two subtypes: the gas
296 chromatograph at Station B and the pneumatic valve vents at Station A and C (see Table 1 and
297 S1). Rates from these sources were aggregated into separate distributions rather than a single
298 vent distribution due to differences in rate magnitude.

299 We generated a distribution of leak counts using the mean and standard deviation of
300 counts from previous component-level surveys assuming a normal distribution. The stations are
301 visited regularly by operators and are in urban areas with passersby and therefore this
302 distribution is unlikely to be non-normal. Source counts of one or zero are used for vents and
303 catalytic heater exhaust emissions depending on the equipment present and operating at the
304 station being modeled. Either the emissions from the gas chromatograph (Station B) or the
305 pneumatic valve vents (Stations A and C) are simulated. No station had both vent source types.
306 Vents are assumed “on” all year in the model; catalytic heaters are only “on” between October
307 and April and “off” (i.e., not emitting) between May and September.

308 We drew a leak count, N_{leaks} , from the distribution, and for each leak in N_{leaks} , sampled
309 with replacement from the aggregated fugitive CH₄ emissions rate distribution ($n = 28$).
310 Measurement uncertainty, ε_i , was approximated for each rate sampled, R_i , by randomly drawing
311 from an error distribution (with replacement) centered on zero with a standard deviation of 10%,
312 which is the rated accuracy of the HETEK hi-flow. All rates (with uncertainty) were summed to
313 calculate total fugitive CH₄ emissions, E_{fug} , at a station following Eq. (1), and the process was
314 repeated 10,000 times:

$$315 \quad E_{fug} = \sum_{i=1}^{N_{leaks}} (R_i * (1 + \varepsilon_i)) \quad (1)$$

316
317 The procedure was similar for estimating CH₄ from vents, E_{vent} , and catalytic heater exhaust,
318 E_{cat} . The model generated a distribution of possible rates for these sources using the mean and
319 standard deviation of the aggregated rate distributions. We then drew a rate, R , and error, ε ,
320 (from the hi-flow error distribution), with replacement, similar to the method for estimating
321 fugitive emissions. E_{vent} or E_{cat} were estimated as the product of R and $(1 + \varepsilon)$, as vented or
322 catalytic exhaust source counts ≤ 1 at the stations. The process was repeated 10,000 times to
323 generate distributions of potential CH₄ emissions for vents and catalytic heater exhaust
324 accounting for uncertainty.

325
326 CH₄ emissions in line heater exhaust were not quantified with component-level
327 techniques. This is a common limitation with instruments such as the hi-flow (Vollrath et al.,
328 2024). To estimate these emissions in the model, we used daily natural gas throughput data for
329 the stations over the study period, estimates for the proportion of throughput consumed by line
330 heaters as process gas (Groebner, 2020), and a generic EF for CH₄ emissions from industrial,
331 commercial, and residential natural gas consumption (ECCC, 2025). To our knowledge, this EF

332 is an industry standard EF and is very similar to the EF used by the local gas utility—which they
333 adjust based on gas composition analysis—to estimate incomplete combustion emissions from
334 line heaters in their inventory. The gas utility’s approach differs slightly from ours in that the
335 utility combines estimated gas consumption by line heaters annually at the asset-level with their
336 EF to estimate incomplete combustion emissions. Differences between the approaches are small,
337 and we surmise that when downscaled, the utility’s estimates would be similar to those we
338 derived from modeling but less representative of shorter time scales. We followed Eq. (2) to
339 estimate line heater incomplete combustion CH₄ emissions:

$$341 \quad E_{lh} = \frac{((Q * (1 + \varepsilon)) * P_{lh}) * EF}{24} \quad (2)$$

342
343 where E_{lh} is the line heater exhaust CH₄ emissions rate in kg/h, Q is daily station throughput
344 drawn by the model given a user input date, ε is approximated throughput measurement error
345 drawn from an error distribution centered on zero and assuming error of $\pm 3\%$ (upper limit
346 provided by the gas utility), P_{lh} is the estimated proportion of station throughput consumed by
347 line heaters as process gas (Groebner, 2020), and EF is the incomplete combustion CH₄ EF of
348 3.7×10^{-5} kg CH₄/m³ of natural gas consumed (ECCC, 2025). Other major sources of incomplete
349 combustion CH₄ at the stations were not present (see Table 1 and S1). The process was repeated
350 10,000 times.

351 The resulting distributions of potential fugitive, vent, catalytic heater exhaust, and line
352 heater exhaust CH₄ emissions were summed to generate a modeled estimate of hourly CH₄
353 emissions from a station, $E_{station}$, on a given day, following Eq. (3):

$$355 \quad E_{station} = E_{fug} + E_{vent} + E_{cat} + E_{lh} \quad (3)$$

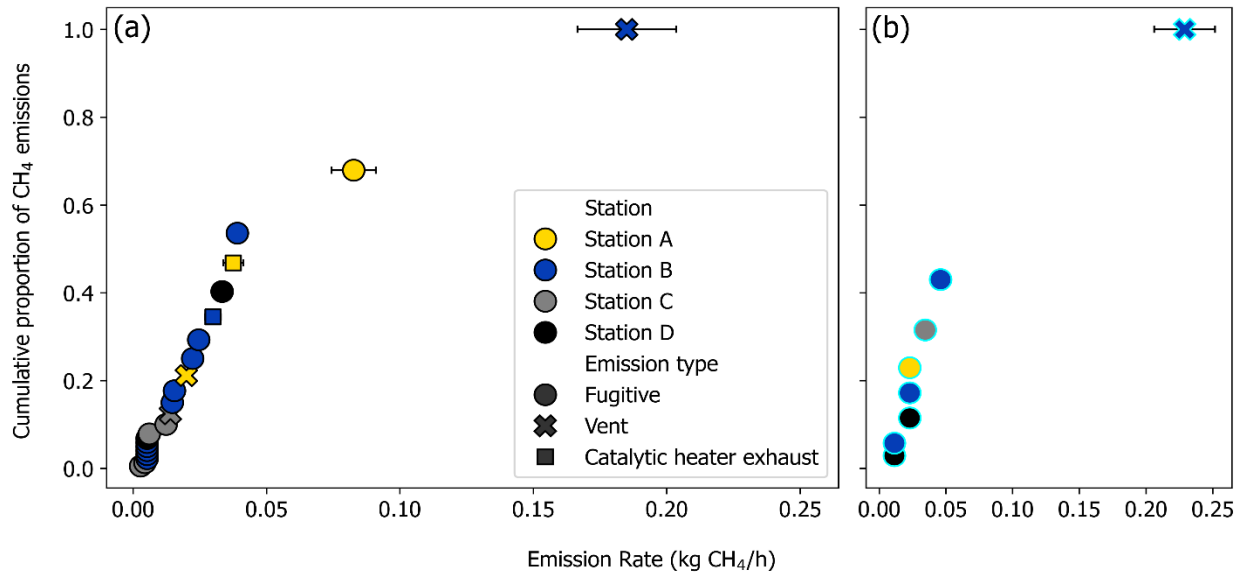
356
357 Only relevant sources were simulated for each station, as not all sources were present at all
358 stations. This model provided a reasonable blend of empirical and operational elements.

360 **3. Results and discussion**

361 *3.1. Component-level surveys*

362 In general, we did not find many sources of CH₄ emissions in the component-level surveys and
363 the rates quantified were low compared to other sources and rates in the oil and gas supply chain.
364 Figure 3a shows the rates of different types of emissions detected and quantified in the
365 component-level surveys as a proportion of total emissions quantified across all stations. We
366 averaged the rates for continuous or persistent sources that were measured more than once to
367 include in Figure 3.

368



369
 370 **Figure 3.** (a) CH₄ rates quantified in the component-level surveys by station and emission type
 371 as a cumulative proportion of total emissions quantified across all three surveys at the stations
 372 (circle markers with black outline). (b) Rates quantified in historic leak detection surveys at the
 373 stations between 2020 and 2023 (circle markers with bright blue outline). Mean rates are shown
 374 for sources measured in > 1 survey in (a) and (b). Error bars represent the rated accuracy ($\pm 10\%$)
 375 of the hi-flow sampler applied to rate estimates.

376
 377
 378 The largest source identified in the component-level surveys was a continuous gas
 379 chromatograph vent at Station B (Figure 3a). This instrument measures gas composition for
 380 custody transfer and billing as natural gas moves from transmission to distribution. We
 381 quantified emissions from the vent at 0.16–0.23 kg CH₄/h (mean: 0.19 kg CH₄/h, Figure 3a).
 382 Historic leak detection data similarly reported emissions of 0.16–0.32 kg CH₄/h (mean: 0.23 kg
 383 CH₄/h, Figure 3b) from the same vent, which was quantified with a hi-flow sampler four times
 384 over five surveys conducted between 2020 and 2023 (Figure 3b). The chromatograph vent
 385 accounted for 32% of total component-level CH₄ emissions measured in this study and 57% of
 386 emissions in the historic leak detection dataset. The higher contribution in the historic data set
 387 likely reflects the fact that the component-level surveys in this study captured emissions from a
 388 broader set of sources across all stations (e.g., transmission pipeline pneumatic valve vents and
 389 catalytic heater exhaust), increasing the denominator of total measured emissions and thereby
 390 reducing the relative contribution of the chromatograph vent.

391 For context, emissions from the chromatograph vent are comparable to the 75th percentile
 392 of fugitive emission rates reported in the Clearstone distribution for on-site sources at Alberta oil
 393 and gas production facilities (Clearstone Engineering, 2019). However, the vent emits at a rate
 394 nearly 13 times lower than the mean rate (2.4 kg CH₄/h) from individual sources reported for two

395 city-gate stations in Montreal (Williams et al., 2022). If emissions persist at the mean observed
396 rate, the chromatograph vent alone would emit approximately 2 t CH₄/yr.

397 No other stations had a chromatograph vent. Stations A and C had pneumatic valves on
398 transmission pipeline segments that vented—the quantified rates were an order of magnitude
399 lower than the chromatograph vent at Station B (Figure 3a). No other vent sources were present
400 at the stations. A previous study identified odorizer vents emitting CH₄ at distribution stations in
401 the U.S. (Lamb et al., 2015). The natural gas distributed in Calgary is odorized upstream of
402 distribution stations in the city.

403 Stations A and B had active catalytic heaters, which are used in combination with process
404 buildings to ensure process equipment is warm, reducing potential for liquids formation or
405 malfunction in cold temperatures. Catalytic heaters can emit through both their exhaust hoods
406 and catalyst beds where heat is generated, both of which are known to emit incompletely
407 combusted CH₄ (Festa-Bianchet et al., 2024). Catalytic heaters are generally turned off during
408 warmer summer months. Mean rates at Station A and B were 0.03 kg CH₄/h and 0.04 kg CH₄/h,
409 respectively. These are an order of magnitude lower than the mean rate (0.28 kg CH₄/h ± 0.04 kg
410 CH₄/h) of 38 catalytic heater exhaust measurements at oil and gas production sites in British
411 Columbia (Festa-Bianchet et al., 2024). Possible reasons for the difference between our results
412 and Festa-Bianchet et al. (2024)'s are sample size, the measurement methods used, smaller
413 heaters in the distribution segment, and differences in fuel gas composition that could affect
414 hydrocarbon destruction efficiency, assuming the heaters are similar models. We measured the
415 largest rates from the catalytic heater exhausts during the winter survey (Figure 2) at these
416 stations. This could suggest emissions vary temporally with temperature, in addition to varying
417 seasonally when “on” or “off” at different times of the year. We also observed CH₄ emissions
418 from the catalyst beds (or emissions that escaped capture by the fume hood) on the units with
419 OGI but could not quantify these due to their temperature and inability to fully capture the
420 emissions with the hi-flow. Similar to oil and gas production sites (Festa-Bianchet et al., 2024),
421 catalytic heaters may be a unique source to distribution stations in cold climate regions.

422 We detected and quantified several fugitive emissions across the stations. Figure 3a
423 shows that the largest was responsible for 14.3% of total emissions measured across the stations.
424 Station A's catalytic heater pressure relief valve (PRV) was emitting, indicating that the supply
425 gas pressure was too high. During the survey, a station operator attempted a repair and shut the
426 supply gas off to the unit. We also detected a fugitive emission that resulted from two failed
427 mechanical valves on a small separator attached to the line heater at Station D. This caused CH₄
428 to emit from the end of a plugged line outside the northernmost building at the station (Figure
429 1d). A station operator made a temporary repair at a later date and replaced the valves after our
430 last survey at Station D.

431 On average, we detected a higher number of sources in the component-level surveys
432 (Station A: 2; Station B: 6.7; Station C: 2.3; Station D: 0.7) at the stations than reported in the
433 historic leak detection data (Station A: 1; Station B: 1.4; Station C: 1; Station D: 2). We attribute
434 this primarily to measuring catalytic heater exhaust and all vents for CH₄ emissions, which may

435 have been outside of the scope of field technicians' work as these sources are not typically
436 considered an actionable leak, and supplementing OGI with olfactory methods and soapy water
437 for leak detection. The emergence of new leaks may also partly explain the differences in the
438 number of sources detected in the component-level surveys in this study and the historic leak
439 detection data.

440 The number of fugitives shown in Figure 3a included many sources from the last survey
441 at Station B (Figure 2). We detected two leaks from threaded connections on gauges attached to
442 the line heaters with OGI that persisted from the November survey. The operator inspected these
443 leaks in November but they were not repaired immediately because of safety reasons related to
444 the cold temperature and risk of equipment damage. This prompted us to inspect all gauges on
445 the line heaters using olfactory methods and snoop in the subsequent survey in March (Figure 2),
446 revealing an additional 6 small leaks. These were below the quantifiable limit of the hi-flow and
447 thus were assigned the instrument's lower limit as a rate (Figure 3a). The operator repaired 7 out
448 of the 8 leaks immediately, leaving one for repair during future maintenance. The quantity of
449 leaks indicates that line heaters may be prone to many small leaks from threaded connections on
450 gauges. Frequent temperature changes as gas enters and exits the heaters—causing metal to
451 expand and contract—could explain this finding.

452 Working collaboratively with the natural gas utility enabled abatement of fugitive CH₄
453 emissions as an extension of the research. We used the measured fugitive rates, assumptions on
454 emissions duration, and repair dates to calculate that the component-level surveys avoided 0.9 t
455 CH₄ from being emitted into the atmosphere (see S4 for details on the calculations).

456 Overall, the stations had relatively few CH₄ emissions. Mean aggregated component-
457 level rates for the stations were 4.3×10^{-2} kg CH₄/h (Station A), 0.3 kg CH₄/h (Station B), $3.6 \times$
458 10^{-2} kg CH₄/h (Station C), and 1.3×10^{-2} kg CH₄/h (Station D). Operators visit them regularly and
459 some process buildings have lower explosive limit (LEL) alarms which trigger operator call outs.
460 The urban nature of the stations, where some are located adjacent to pathways and buildings,
461 may also result in call-ins to the utility if passersby smell CH₃SH. These factors could limit the
462 emissions from the stations. Despite the low rates, the mitigated emissions from threaded
463 connections, leaking valves, and a PRV on a catalytic heater highlight that opportunities to
464 reduce fugitive CH₄ at these stations exist. Much larger rates have been measured at city gate
465 stations in Montreal (Williams et al., 2022), suggesting that urban natural gas distribution sites
466 are not ubiquitously low-emitting.

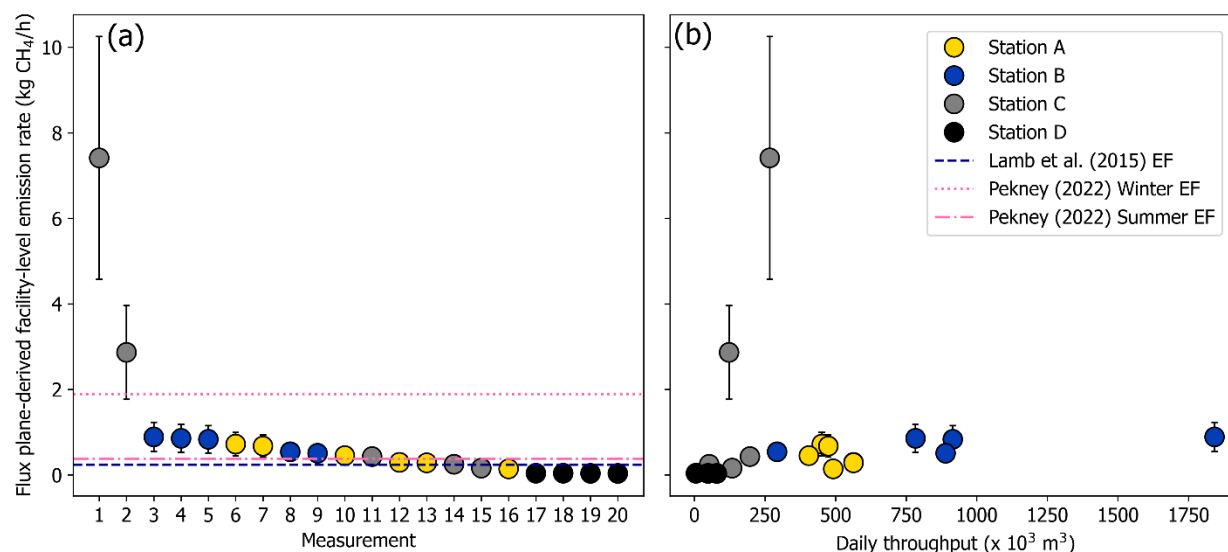
467 468 *3.2. Facility-level measurements*

469 The novel application of the human-portable flux plane method in this study to measure facility-
470 level emissions enabled capture of CH₄ emissions from all sources at the stations emitting at the
471 time of the measurements. This included incomplete combustion emissions from line heaters
472 owing to the vertical capabilities of the flux plane method, which were not measured in the
473 component-level surveys because of the height at which plumes are emitted and their
474 temperature. The method allowed for targeting of atmospheric conditions for measurements that

475 limited vertical plume rise from the stations due to its user-friendliness and practicality (Vollrath
476 et al., 2026). Applying the method addressed an important knowledge gap in the existing
477 research literature related to the sources and rates of emissions at distribution stations where
478 large reductions in gas pressure occur such as those in Calgary. Here we report the quantified
479 rates and explore the most likely sources of CH₄ emissions measured with facility-level
480 measurements.

481 Figure 4a shows the facility-level flux plane-derived CH₄ emission rate estimates by
482 station over the study period. The rates ranged between 3.4×10^{-2} kg CH₄/h to 0.9 kg CH₄/h,
483 except two measurements at Station C that resulted in substantially higher rate estimates of 2.9
484 kg CH₄/h and 7.4 kg CH₄/h. Station D emitted at the lowest rates (mean: 3.6×10^{-2} kg CH₄/h;
485 standard deviation: 2.3×10^{-3} kg CH₄/h), while Station B emitted at higher rates (mean: 0.7 kg
486 CH₄/h; standard deviation: 0.15 kg CH₄/h) more consistently than the other stations. This was
487 unsurprising given that Station D is the smallest, has fewer components and pieces of equipment
488 with potential to emit CH₄, and pushes more natural gas through the distribution system during
489 periods of high demand. Station B is the largest, has sources such as a gas chromatograph vent
490 and catalytic heater (see Table 1 and S1 for more details on the stations), and handles a high
491 volume of throughput.

492



493 **Figure 4.** (a) Flux plane-derived facility-level CH₄ emissions rate estimates. Measurements 6
494 and 7 and 17 and 18 were repeat measurements on the same day, spaced approximately one hour
495 apart. Horizontal lines show CH₄ emissions factors (EFs) derived from measurements at “city
496 gate” stations in the U.S. from Lamb et al. (2015) and Pekney (2022) for comparison. (b) The
497 facility-scale rates plotted against daily natural gas throughput at the stations. Throughput data
498 were provided by the gas utility. Error bars represent the average uncertainty of pole-based flux
499 plane measurements as determined in controlled release testing (Vollrath et al., 2026).

501

502

503 With the exception of the two elevated emission rate estimates at Station C, the CH₄ emissions
504 rates at Stations A and C were generally similar but slightly higher at Station A (A—mean: 0.4 kg
505 CH₄/h; standard deviation: 0.2 kg CH₄/h, B—mean: 0.3 kg CH₄/h; standard deviation: 0.1 kg
506 CH₄/h). These stations are similar in design, equipment, and operating processes and therefore
507 have largely comparable sets of potential CH₄ sources. One key difference is that Station A has
508 an active catalytic heater, whereas the catalytic unit at Station C was unpowered and inactive
509 during the measurement period. In addition, similar to Station D, Station C pushes more gas
510 through the distribution system during periods of higher demand, meaning its throughput can be
511 low or zero at times during the year. In contrast, Station A has higher throughput and receives
512 and distributes gas all year. These operational differences likely explain the slightly higher
513 emissions rates at Station A than Station C.

514 Mean facility-level emissions rates were 2.5 to 61.7 times larger than the mean of
515 aggregated component-level rates from each survey depending on the station (Station B: 61.7
516 times, Station A: 9.9 times, Station D: 2.8 times, and Station B: 2.5 times). Despite the large
517 discrepancy, there is little basis to directly comparing component- and facility-level rates further
518 because not all sources were measured in the component-level surveys and measurements at each
519 scale were performed asynchronously. However, the multi-scale measurements and observations
520 of emissions and equipment configurations provide important context for exploring the most
521 likely sources of CH₄ emissions measured in facility-level measurements.

522 We attribute the vast majority of the flux plane-derived CH₄ emissions rates to
523 incomplete combustion from the line heaters for several reasons. First, with the flux plane
524 method, CH₄ mixing ratios were measured and monitored in near-real time downwind of the
525 stations close to their fencelines using the LI-7810. Based on the mixing ratios, wind direction,
526 and location of equipment, the thermal electric generators (TEGs)—which power the sites and
527 were not quantified on-site—were interpreted to be substantially smaller emitters. Second, other
528 sources that could explain the additional emissions at similar magnitudes were lacking in the on-
529 site surveys. Some fugitive CH₄—which was also not quantified on-site—may have been
530 escaping catalytic heater fume hoods inside buildings at Stations A and B and emitted to the
531 atmosphere through passive building vents. However, based on other measured fugitive CH₄
532 rates, we hypothesize that these emissions were insufficient in magnitude to explain most of the
533 additional emissions. Third, the highest CH₄ mixing ratios—or stations' plume centerlines—
534 measured with the pole-based flux plane method were located directly downwind of the line
535 heaters and at similar heights to their exhaust stacks (~5 m a.g.l.). Figure S2 shows CH₄ mixing
536 ratio by height for two facility-scale measurements. Plumes were sometimes closer to the
537 ground, but we surmise this was due to differences in the pole operator's elevation relative to the
538 stations during the measurements and atmospheric conditions rather than another source. For
539 example, OGI video taken at Station D on 3 January 2025 showed approximately 1 m downwash
540 of the line heater's plume over tens of seconds (see supplemental video). Fourth, the gas utility
541 indicated that incomplete combustion emissions from line heaters is also the largest source of
542 CH₄ emissions in aggregate in their inventory. These examples support attributing the majority of

543 facility-level CH₄ emissions that could not be measured in the component-level surveys to
544 incomplete combustion from line heaters.

545 Repeat pole-based flux plane measurements conducted ~1 hour apart at Stations A and D
546 yielded nearly identical emission rates (Figure 4a), indicating limited variability on hourly
547 timescales and demonstrating good repeatability of the flux-plane method. In contrast, emissions
548 varied substantially over longer timescales. For Stations A, B, and C, most facility-level emission
549 rates were correlated with throughput (Figure 4b), consistent with emissions driven by line heater
550 operation. This confirms the importance of incomplete combustion emissions from the line
551 heaters to total facility-level CH₄ emissions. These stations use vacuum-style heaters that
552 consume ~0.15% of throughput, whereas Station D uses a bath-style heater (~0.23% of
553 throughput), and its emissions were nearly constant and uncorrelated with throughput (Groebner,
554 2020). This suggests fundamentally different heater operating characteristics, with emissions at
555 Station D effectively switching “on” or “off” seasonally as the station’s operations change.

556 Seasonal operation further implies that emissions are likely lower in summer, when both
557 catalytic and line heaters are turned down or off depending on the station due to reduced heating
558 requirements for equipment and lower or no gas throughput. Consistent with this, summer
559 measurements at some of the same Calgary stations reported substantially lower CH₄ emission
560 rates (Hugenholtz et al., 2021), and similar seasonal contrasts have been observed elsewhere,
561 with winter emissions several times higher than summer emissions at city-gate stations in Ohio
562 (Pekney, 2022, pink lines Figure 4a). These findings highlight challenges in annual scaling and
563 suggest that inventories relying on non-winter measurements—such as the U.S. Environmental
564 Protection Agency’s (EPA’s) Greenhouse Gas Inventory (GHGI) EF of 0.24 kg CH₄/h/station
565 derived from component-level surveys (Lamb et al., 2015, blue line Figure 4a)—may
566 underestimate emissions if cold-period operation is not captured.

567 Notably, throughput alone cannot explain the two largest emission rates observed at
568 Station C (2.9 and 7.4 kg CH₄/h), which occurred during the coldest (-15.7 °C) and windiest (7.7
569 m/s) conditions of the study. These events, combined with strong downwind odor and otherwise
570 low component-level emissions, suggest abnormal line heater operation, potentially leading to
571 incomplete combustion and venting of CH₄ through exhaust stacks. To our knowledge, the line
572 heater stacks at the stations in this study operate by natural draft: hot exhaust gases rise through
573 and exit stacks, while outside air required for combustion is drawn in. The exact root causes of
574 the high emissions rates are unclear, but very cold conditions can reduce stack air intake by
575 condensing and freezing exhaust gases, while very windy conditions can also disrupt air intake
576 and line heater burner flames, thereby affecting combustion (Marlett, 1997). Measurements were
577 performed at other stations under similar conditions at times during the study period (e.g., very
578 cold conditions on 3 January 2025—see Figure 2), which yielded substantially smaller rate
579 estimates. This suggests that other underlying mechanisms may have contributed to the high
580 emissions rates at Station C, and that very cold and windy conditions alone would not likely
581 elicit this type of response in line heater emissions more broadly. The remaining measurements at
582 Station C were an order of magnitude lower, reinforcing the episodic nature of these events.

583 Similar, high emission rates from stations with line heaters have been reported elsewhere
584 (Pekney, 2022), which disproportionately influence emissions. Given the magnitude of the rates,
585 the frequency and duration of these events should be better understood to improve estimates of
586 total CH₄ emitted over time.

587 The magnitude of the emissions rates we measured and attributed to the line heaters at
588 Station C may not be unique to the distribution segment. Tyner et al. (2021) reported rates for
589 line heaters of 1.3 kg CH₄/h and 4.8 kg CH₄/h (approximated based on Figure 6 in Tyner et al.
590 (2021)) at oil and gas production sites in British Columbia (B.C.) measured with aircraft. The
591 type of emission (e.g., fugitive or incomplete combustion) was not reported in the study and the
592 conditions at the time of the measurements are unknown, but the rates are similar to the rates we
593 quantified from stations in Calgary. CH₄ emissions rates of this magnitude from line heaters
594 could thus be a more widespread and frequent phenomena requiring mitigation efforts. More
595 work is needed to diagnose root cause and confirm whether the emissions are abnormal and due
596 to process upsets or within the envelope of routine but variable emissions. Maintenance of line
597 heaters is required to mitigate combustion issues (Groebner, 2020).

598 Overall, facility-level emission rates measured in this study span and often exceed EFs
599 derived from existing studies, reflecting differences in measurement methods, station
600 configurations, and capture of incomplete combustion emissions from line heaters in
601 measurements. The variability observed across stations, seasons, and operating conditions
602 underscores the need for multi-temporal, facility-level measurements to develop representative
603 EFs and improve urban CH₄ inventories. Finally, the measurements and attribution of emissions
604 in this and other studies highlight line heaters as a critical and under-characterized source
605 requiring targeted mitigation.

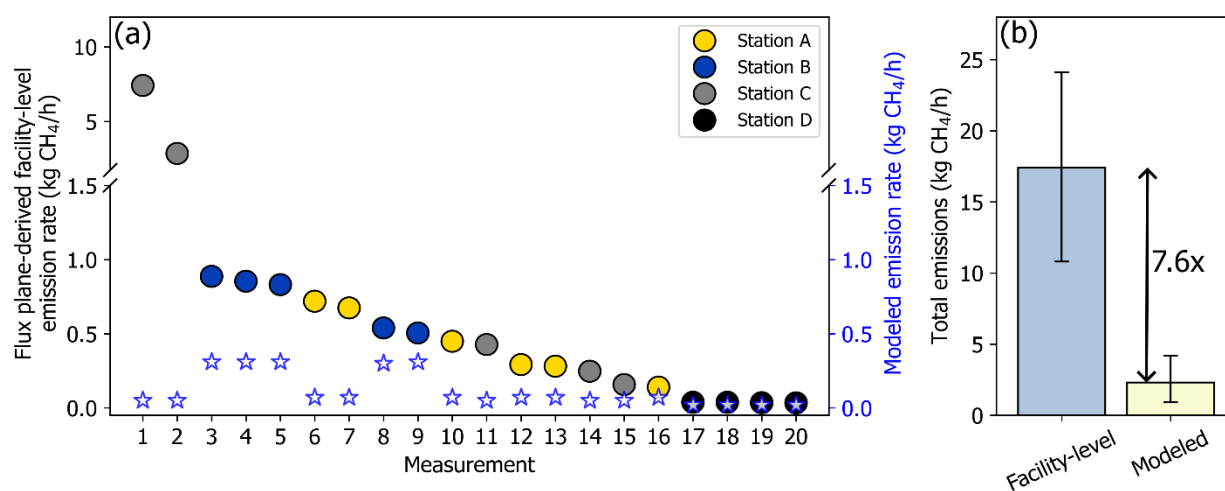
606

607 *3.3. Comparison of modeled and flux plane-derived CH₄ emission estimates*

608 Comparing measurements of CH₄ emissions to estimates derived from conventional approaches
609 such as inventories can help provide insight into whether estimates—which inform climate
610 reporting and mitigation—are representative of real-world emissions. We developed a Monte
611 Carlo-based modeling framework integrating component-level measurements, historic leak
612 detection data, gas throughput, source specific EFs, and understanding of station sources and
613 processes to enable a temporally resolved comparison of snapshot measurements with estimates.
614 The model generated an emission rate estimate for a station in kg CH₄/h on a given day based on
615 four source categories observed at the stations: fugitives (leaks), vents, catalytic heater exhaust,
616 and line heater exhaust.

617 Figure 5a compares modeled to flux plane-derived estimates for the days on which
618 facility-level measurements were performed at the stations. On average, the flux plane estimates
619 were 13.9 times larger than the modeled estimates (standard deviation: 33.9). Results are skewed
620 by the two large flux plane estimates (2.9 and 7.4 kg CH₄/h), which were 57.3 and 148.3 times
621 larger than modeled estimates, respectively. All flux plane-derived estimates were between 1.6
622 and 148.3 times greater than modeled estimates for stations. Given the skewed distribution, the

623 median ratio between facility-level and modeled estimates was 2.8, which was lower than the
 624 mean ratio. In decreasing order, the largest discrepancies between facility-level and modeled
 625 estimates for stations expressed as ratios were Station C (mean = 44.4, standard deviation =
 626 62.2), Station A (mean = 6.1, standard deviation = 3.3), Station B (mean = 2.3, standard deviation
 627 = 0.6), and Station D (mean = 1.8, standard deviation = 0.1). The very large gaps between a
 628 number of facility-level measurements and modeled estimates, such as those observed for Station
 629 C, underscore the difficulty of representing large but infrequent emissions using traditional
 630 modeling approaches that scale EFs with activity factors (AFs). Much larger measured than
 631 modeled emissions at Station C could reflect broader combustion or operational issues with its
 632 line heater requiring mitigation. Further investigation is required.
 633



634 **Figure 5.** (a) Comparison of individual facility-level flux plane emission rate estimates with
 635 temporally-resolved estimates derived from the model developed in this study. Note the broken
 636 y-axis. Error bars for individual measurements and modeled estimates are not shown for clarity.
 637 (b) Comparison of total CH₄ emissions quantified across all facility-level flux plane
 638 measurements with total emissions estimated with the model. The error bar on the facility-level
 639 total represents the range of likely estimates based on the average uncertainty of pole-based flux
 640 plane measurements as determined in controlled release testing (Vollrath et al., 2026). The error
 641 bar on the modeled total represents a 95% confidence interval (CI), calculated by propagating
 642 errors through the model for each estimate (§2.2.4).
 643

644
 645
 646 Figure 5b shows that measured emissions rates at the facility-level totaled 17.4 kg CH₄/h (10.8
 647 kg CH₄/h to 24.1 kg CH₄/h based on the average uncertainty of the flux plane method) across all
 648 measurements during the study period, whereas modeled estimates totaled 2.3 kg CH₄/h (95%
 649 CI, 0.9 kg CH₄/h to 4.2 kg CH₄/h), or 7.6 times less than the sum of facility-level measurements.
 650 We attributed the vast majority of facility-level emissions that could not be measured in
 651 component-level surveys to line heater incomplete combustion (§3.2). Provided that our

652 attribution is correct, after accounting for emissions measured at the component-level we
653 estimate that the incomplete combustion of process gas by line heaters was responsible for a total
654 of 15.5 kg CH₄/h (89.1%) out of the 17.4 kg CH₄/h of facility-level measurements. The two large
655 rates quantified at Station C contributed 10.2 kg CH₄/h or 66% to facility-level emissions
656 attributed to line heaters and 58.6% to all emissions. In contrast, line heater incomplete
657 combustion was only a small fraction of total modeled CH₄ emissions (0.02 kg CH₄/h or <1%),
658 which is 775 times lower than our estimate for these emissions derived from facility-level
659 measurements and attribution. Catalytic heater exhaust was estimated to emit a total of 0.36 kg
660 CH₄/h with the model, with leaks and vents—primarily the chromatograph vent at Station B—
661 estimated to emit the remainder of total modeled emissions (1.9 kg CH₄/h).

662 There is reasonable agreement between total measured (1.9 kg CH₄/h) and modeled (2.3
663 kg CH₄/h) emissions attributed to leaks, vents, and catalytic heater exhaust. Slightly higher
664 modeled emissions for these sources are likely due to the inclusion of historic leak detection data
665 in the model, which included a larger rate for the chromatograph vent at Station B than we
666 measured on site. Attribution of facility-level rates did not involve the historic leak detection data
667 and relied on our on-site measurements and other observations only. Furthermore, modeling of
668 Station B's fugitive emissions, which was the largest station with the highest potential to emit
669 CH₄, may have been biased toward higher leak counts, slightly increasing emissions. The
670 distribution of leak counts from the component-level surveys and historic leak detection data that
671 informed the modeling of this station's fugitive emissions was strongly right skewed.

672 Compared to the other sources modeled, estimates of incomplete combustion CH₄
673 emissions from line heaters are at odds with estimates derived from facility-level measurements
674 and attribution. We explore several possibilities. First, we used a generic EF of 3.7×10^{-5} kg
675 CH₄/m³ of natural gas consumed to estimate incomplete combustion emissions from line heaters
676 in the model. The EF is very similar to the EF used by the gas utility in their inventory and to our
677 knowledge is used widely to estimate CH₄ emissions from different end uses of natural gas. It is
678 listed as an EF by Environment and Climate Change Canada (ECCC) and is included in the
679 Canadian Energy Partnership for Environmental Innovation (CEPEI) Emissions Estimation
680 Manual, which provides emissions factors and methodological guidance to gas distributors, other
681 companies, and consultants in Canada for estimating emissions (ECCC, 2025; CGA, n.d.). This
682 EF could be too small. Second, line heaters, as well as catalytic heaters, are used on oil and gas
683 production sites (Festa-Bianchet et al., 2024) and natural gas distribution sites. Equipment are the
684 same but EFs listed by ECCC to estimate CH₄ emissions from natural gas end use differ by two
685 orders of magnitude depending on sector/consumer classification (8.2×10^{-3} kg CH₄/m³ natural
686 gas consumed for oil and gas producers in Alberta vs. 3.7×10^{-5} kg CH₄/m³ natural gas consumed
687 for industrial, commercial, residential, and most other end users, ECCC, 2025). These EFs could
688 differ due to differences in gas composition in production and distribution settings; however, the
689 EF used in this study and more broadly by gas utilities may not represent real emissions from
690 equipment that combusts gas if EF selection is based on consumer classification or segment of
691 the natural gas supply chain only. Further study is required. Third, line heaters could consume

692 much more gas than estimated, but to our knowledge consumption rates used to model emissions
693 in this study were based on metered consumption at a distribution station in the U.S. (Groebner,
694 2020). Fourth, combustion efficiencies and thus emissions rates could be highly variable, which
695 would not be captured with traditional EF x AF approaches. Fifth, despite our efforts to resolve
696 modeled estimates temporally with facility-level measurements, conventional EF x AF
697 approaches typically fail to capture larger but infrequent emissions such as those observed at
698 Station C. Overall, some combination of these possibilities probably explains the differences
699 between estimates.

700 The results shown here apply to the timing of the facility-level measurements and
701 modeled estimates, and caution should be taken in scaling the findings from this study up
702 temporally. Measurements and modeled estimates, as well as discrepancies between the two,
703 only represent snapshots in time. However, results do suggest that distribution stations are
704 emitting more CH₄ than estimated using conventional approaches and that line heater incomplete
705 combustion emissions are substantially underrepresented.

706 The modeling framework developed in this study is an improvement over conventional
707 inventory approaches in that it integrates source counts, component-level measurements,
708 operational data (throughput), and process-based understanding to generate time resolved
709 estimates of CH₄ emissions. This noted, we do not attempt to reconcile modeled estimates with
710 rates derived from facility-level measurements because underestimated line heater incomplete
711 combustion emissions in the model could be due to a number of factors, which should be
712 revisited by researchers and workers at gas utilities. Additionally, revising the EF used in
713 modeling would still underestimate total incomplete combustion CH₄ emitted by line heaters at
714 distribution stations; conventional EF x AF approaches cannot capture the heavier tail of rates
715 that occur less frequently, such as those measured from line heaters in this and other studies
716 (Tyner et al., 2021; Pekney, 2022), which can disproportionately affect emissions. This
717 underscores the need to compliment modeling with facility-level measurements, to identify
718 emissions that escape conventional estimates for reporting and mitigation.

719 Our results have broader implications. Given the potential issues we highlighted with the
720 incomplete combustion EF, CH₄ emissions from natural gas end use could also be substantially
721 underestimated in other cases where it or similar EFs are used to estimate and track emissions.
722 Notably, recent city- and neighborhood-level atmospheric studies in New York, NY (Zhao et al.,
723 2026) and Calgary, AB (Xing et al., 2026) have indicated that emissions from natural gas end use
724 dominate the CH₄ signal across seasons in these urban areas. Incomplete combustion emissions
725 were also identified as a large source of urban CH₄ emissions in aggregate in a reanalysis of data
726 from several city-level studies by Vollrath et al. (2025), demonstrating an area where mitigation
727 is needed. We resolved line heaters as a pathway for these incomplete combustion emissions and
728 a mitigation target. While some emissions are expected as combustion is never fully complete,
729 strategies to ensure high efficiency combustion should be developed and implemented for line
730 heaters. Finally, large rates that disproportionately affect emissions should also be better

731 understood to eliminate their occurrence through improved maintenance or other methods,
732 yielding material reductions of urban CH₄ emissions and climate benefit.

733

734 **4. Conclusion and outlook**

735 This study combined component- and facility-level measurements and modeling to characterize
736 and advance understanding of CH₄ emissions from four natural gas distribution stations in
737 Calgary, Alberta, addressing key gaps in understanding station-level contributions to urban CH₄
738 budgets and mitigation.

739 On-site surveys showed that fugitive emissions were generally low and readily abatable,
740 confirming that periodic component-level inspections remain valuable for identifying degraded
741 equipment and reducing climate and safety risks. However, these methods only captured 1.6–
742 40.1% of total emissions depending on the station, as they could not quantify incompletely
743 combusted CH₄ emitted in line heater exhaust due to the height at which plumes are emitted and
744 their temperature.

745 The novel application of the human-portable flux plane method enabled quantification of
746 total station emissions, including emissions from line heaters—which combust process gas prior
747 to pressure regulation and are generally outside of the capabilities of component-level methods—
748 in a user-friendly and practical manner. Facility-level flux-plane measurements revealed
749 substantially higher emission rates, ranging from 3.4×10^{-2} to 7.4 kg CH₄/h, with most emissions
750 attributable to the incomplete combustion of process gas by the line heaters. Two extreme
751 emission events, measured at the same station under very cold and windy conditions, were likely
752 caused by line heater operating issues, underscoring the importance of facility-level
753 measurements for detecting episodic events that contribute disproportionately to total emissions.
754 Measured rates were similar in magnitude to rates quantified from line heaters at oil and gas
755 production sites in B.C. using aircraft (Tyner et al., 2021), suggesting that larger emissions from
756 line heaters may be a more widespread phenomenon across the oil and gas supply chain in
757 production regions and cities. There is a need to investigate these larger rates further and
758 determine their root cause for mitigation.

759 Emissions were stable on hourly timescales but varied over weeks and seasons at most
760 stations. Facility-level, flux plane-derived CH₄ emission rates were generally correlated with
761 daily throughput, consistent with incomplete combustion dominating emissions and line heaters
762 operating more intensively during periods of high demand. Situating the rate estimates from this
763 work in the context of other studies of CH₄ emissions from distribution stations indicated that
764 seasonal operating practices, including heater turndown or shutdown in summer, can further
765 contribute to temporal variability of emissions, highlighting the need for inventories to account
766 for seasonal effects.

767 The Monte Carlo-based modeling framework developed in this study generated
768 temporally resolved estimates of CH₄ emissions, addressing issues with comparing snapshot
769 measurements with estimates typically derived from annualized inventories and downscaled.
770 Measured facility-level rates exceeded modeled rates by factors of 1.6–148.3, totaling 17.4 kg

771 CH₄/h (10.8 kg CH₄/h to 24.1 kg CH₄/h based on method uncertainty) across all measurements
772 compared with 2.3 kg CH₄/h (95% CI, 0.9 kg CH₄/h to 4.2 kg CH₄/h) from the model. Emissions
773 attributed to leaks, vents, and catalytic heater exhaust in measurements and modeling were
774 similar (1.9 kg CH₄/h vs. 2.3 kg CH₄/h); emissions attributed to incomplete combustion from line
775 heaters in facility-level measurements were 775 times greater than modeled estimates, indicating
776 that stations may be emitting more CH₄ than previously recognized due to conventional
777 estimates underrepresenting line heater emissions. Further investigation of incomplete
778 combustion CH₄ emissions from line heaters, underlying EFs, and other modeling assumptions is
779 required to improve estimates of total emissions from stations generally.

780 Overall, the results show that line heaters are the dominant and most variable CH₄ source
781 at the distribution stations studied, facility-level measurements capturing all CH₄ emissions offer
782 a complementary perspective needed to identify episodic high-emission events that fall outside
783 of the scope of component-level surveys, and that conventional approaches are underestimating
784 CH₄ emissions from distribution stations because emissions from the incomplete combustion of
785 process gas by line heaters are underrepresented. Consistent with results from city-level
786 measurement and source attribution studies in Canada, the U.S., and other locations, this study
787 identifies the incomplete combustion of natural gas as an important source of urban CH₄
788 emissions and line heaters as a specific and under-characterized pathway for those emissions
789 with potential mitigations.

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1 **Supplemental material to “Multi-scale measurements and temporally resolved modeling of**
2 **methane emissions at natural gas distribution stations”**

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9

10 **S1. Descriptions of the stations**

11 In Figure 1 in the main text, Stations A, B, and C are all large with similar infrastructure on site.
12 In general, these stations each have line heaters which heat the gas prior to its pressure
13 regulation, a large “main run” building where the high-pressure gas is regulated, and several
14 segments of above-ground pipe with connectors and mechanical valves. Stations A and C have
15 additional segments of transmission pipeline above-ground where the direction and flow of gas
16 through the transmission system can be adjusted using a remotely operated manifold that
17 controls three gas-driven pneumatic valves. To maintain gas flow, the valves on these pipelines
18 continuously vent gas.

19 Stations B and C each have a separator to remove additional impurities in received gas.
20 The separator at Station B is several times larger than the separator at Station C, possibly
21 reflecting much higher throughput. Both separators have pressure relief valves. Stations A, B,
22 and C each have one catalytic heater, which are a known source of CH₄ emissions in the
23 Canadian upstream oil and gas industry (Festa-Bianchet et al., 2024), to heat process buildings
24 and associated equipment. The catalytic heater at Station C was not operational because this
25 station did not have direct current (DC) electricity to power the unit. These three stations
26 generated their own electricity using thermal electric generators (TEGs) or other generators, but
27 the TEGs (two units) at Station C were smaller and did not produce DC power. Furthermore,
28 these three stations had standalone buildings to house electronics and wiring related to
29 Supervisory Control and Data Acquisition (SCADA) systems. Station B was the largest of all
30 stations and had a gas chromatograph—which continuously vented—connected at the point
31 where the gas transfers custody from transmission to distribution within the facility to determine
32 its composition.

33 Station D was unique from the other stations in that its spatial footprint was smaller and it
34 had fewer equipment with potential to emit CH₄. No pneumatic valves or catalytic heaters were
35 present on site. This station had a bath-style line heater with a single exhaust stack (main text
36 Figure 1d), where process gas is used to heat a liquid bath at atmospheric pressure, which in turn
37 heats the gas that flows through the station. In contrast, the other stations had one or two
38 vacuum-style line heater units with multiple exhaust stacks (Station A: one unit, six stacks;
39 Station B: two units, four stacks/unit for eight stacks total; Station C: one unit, four stacks) where

40 the liquid bath is under vacuum to reduce the energy required to raise the bath's temperature, and
41 the gas is heated indirectly with steam (Groebner, 2022). A y-strainer separator was attached to
42 the line heater at Station D to filter impurities from the received gas and had a series of
43 mechanical valves attached to it.

44 Stations A and B operate continuously throughout the year, whereas Stations C and D are
45 currently seasonal operations, pushing more gas through the system when temperatures drop and
46 demand increases. The line heaters at Stations C and D are turned down or off in summer due to
47 little or no station throughput and thus lack of a need to heat the gas. New residential
48 development is underway around Station C—it is unclear if this station will remain a seasonal
49 station or not with urban growth. Ultrasonic flow meters measured throughput at all stations.

50

51 **S2. Flux plane quality assurance**

52 We quality-assured (QA'd) the flux plane measurements following the protocol developed by
53 Vollrath et al. (2026) to ensure that the majority of stations' plumes were captured by the pole in
54 the vertical dimension, as there is a fixed limit to the height of the measurements. The QA
55 protocol attempts to understand the vertical geometry of the experiments using the height and
56 characteristics of the emissions source, the height of the receptor, atmospheric conditions, and
57 the downwind distance of the measurements. We refer readers to Vollrath et al. (2026) for further
58 details. We also used OGI to confirm the behavior and dispersion of the line heater plumes prior
59 to performing the pole-based measurements.

60 A total of three measurements were flagged by the QA protocol based on geometry (i.e.,
61 potentially insufficient measurement height). We examined the time series of CH₄ mixing ratios
62 for these measurements in more detail found that all captured the majority of plumes vertically,
63 as indicated by decreasing CH₄ with height and the shape of plumes in the vertical dimension, as
64 observed in the data (Vollrath et al., 2026). This confirms that most measurements were valid.

65 One measurement at Station D on 13 November 2024 had very high and variable
66 background CH₄ mixing ratios (2.4 ppm to 2.7 ppm). These fluctuations were larger in
67 magnitude than the CH₄ enhancement from the station. As such, we were unable to disambiguate
68 between target and non-target emissions in this measurement and discarded it. We noted a potent
69 smell consistent with the combustion of organic matter upwind, which could explain the
70 substantially elevated background emissions. On this date, the wind was blowing from the south.
71 The CH₄ emissions could have been coming from a large, closed landfill, wastewater treatment
72 plant, or a small cattle operation hundreds of meters to kilometers upwind of the target source.

73 Overall, data processing and quantification were performed on 20 out of the 21 of the
74 facility-level flux plane measurements after quality-assuring the data.

75

76 **S3. Additional details on wind measurements and vertical profile estimations**

77 On 11 November 2024 wind data were not recorded with the TriSonica Mini (TSM) at Stations B
78 and C due to a wiring error. On 3 January 2025, we experienced temperature-related reliability
79 issues with the TSM at Stations B, C, and D and wind data were not recorded. The temperature

80 during the facility-scale measurements on 3 January 2025 was -19 degrees Celsius, which is near
81 the lower limit for the TSM's operating temperature. We collected wind data at the stations with
82 an RM Young 81000 after 3 January 2025. We also collected data with both anemometers on 21
83 February 2025 to compare measured wind speeds (Figure S1).

84 We used wind data from a Calgary Regional Airshed Zone (CRAZ) air quality monitoring
85 station located at 50.955120, -113.969787 to fill in wind data gaps. We selected this station due
86 to its proximity in between Stations B, C, and D in south Calgary. The alternative was the
87 Environment and Climate Change Canada (ECCC) weather station at the Calgary International
88 Airport which is in the northeast of the city. Wind speed and direction are measured at a height of
89 10m at the CRAZ station, while trace gases and particulate matter are measured at lower heights.

90 Wind speed and direction were measured at 2.2m with the RM Young 81000. The pole-
91 based flux plane method requires estimating a vertical wind profile, for which we used a power
92 law (Vollrath et al., 2026). For the coefficient in the power law, we used 0.17 (Heier, 2014) and
93 0.24 depending on the location of the station in Calgary and the surrounding land use (more rural
94 vs. urban). The coefficient of 0.24 chosen to represent vertical wind shear at urban locations is
95 similar to 0.25 recommended by the U.S. Environmental Protection Agency (EPA, 2000) for
96 urban environments under D atmospheric stability classes (similar to almost all of our
97 measurements). The power law was used with these coefficients to extrapolate wind speed
98 estimates at the various heights to the heights of the grid cell centers in the flux plane (see
99 Vollrath et al., 2026 for more details).

100 Temperature and atmospheric pressure were taken from the Environment and Climate
101 Change Canada (ECCC) weather station at the Calgary International Airport (WMO ID: 71877)
102 to use in converting CH₄ concentration in ppm to mass concentration in quantifying the
103 emissions with the flux plane method (Vollrath et al., 2026).

104

105 **S4. Tracking CH₄ emissions avoided through on-site detection and abatement**

106 To calculate the CH₄ emissions avoided, we assumed that detected and repaired fugitive sources
107 would have continued emitting for one-half a year if they had not been identified as part of the
108 research. Some fugitives were not immediately repaired. We tracked these repair dates and
109 subtracted the CH₄ emitted from the date that the fugitive emission was detected until it was
110 repaired by operators from the total potential avoided emissions. Following this approach, we
111 estimate that the quantity of fugitive emissions avoided by the on-site research at the stations
112 totaled 0.9 t CH₄/yr over the duration of the study.

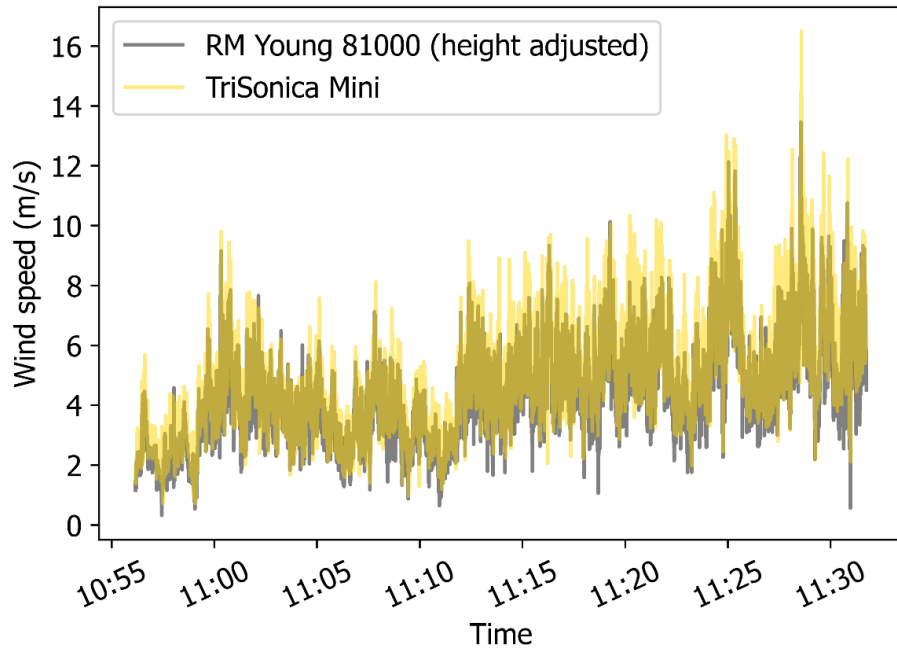
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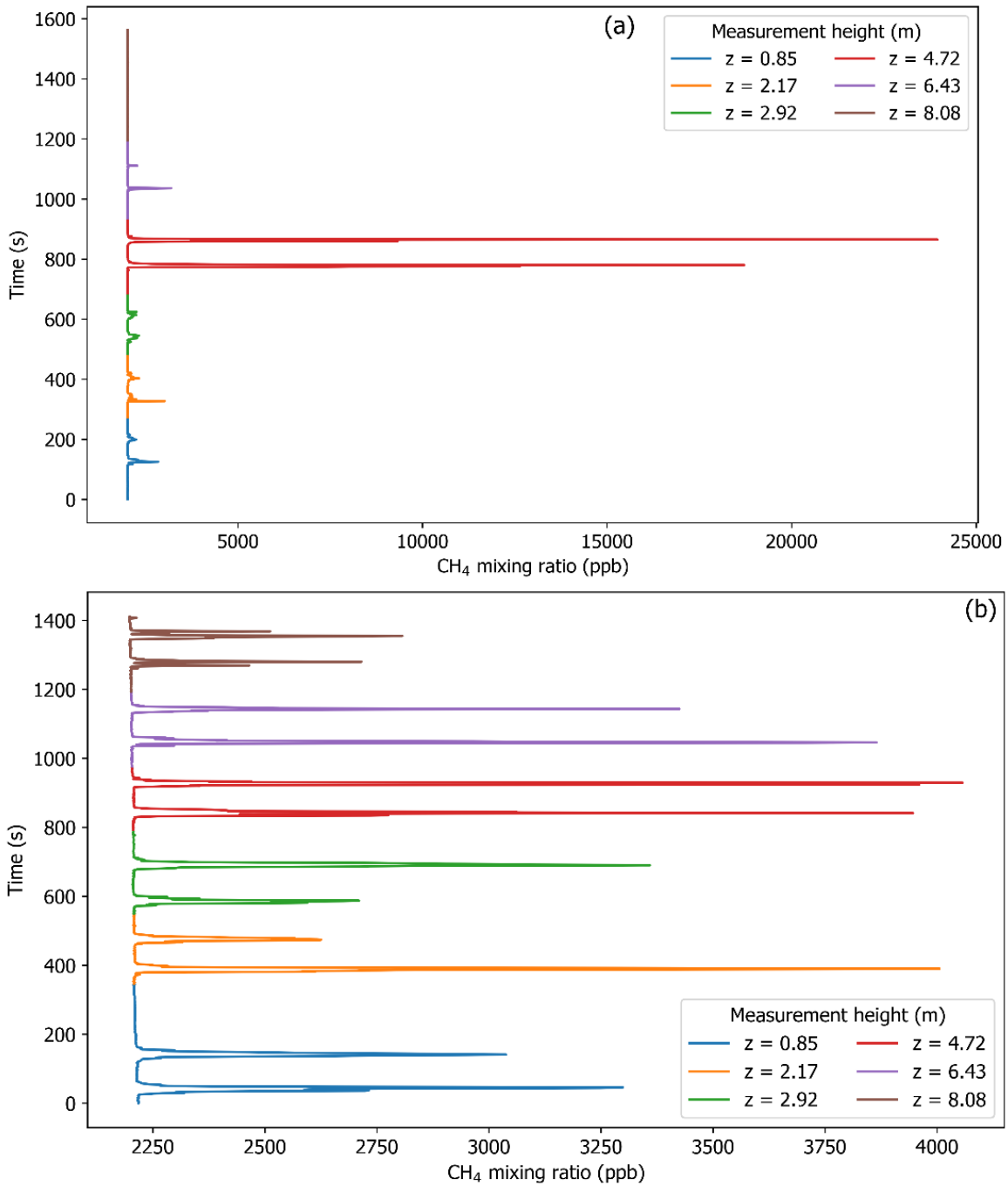
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Figure S1. Comparison of wind speed measurements with the TriSonica Mini (TSM) and RM Young (RMY) 81000 anemometers on 21 February 2025. Mean wind speeds were 5.0 m/s (standard deviation = 1.8 m/s) and 4.4 m/s (standard deviation = 1.7 m/s) for the TSM and RMY, respectively. RMY measured wind speeds in the figure were adjusted for height using the method in S3 to match the height at which wind was measured with the TSM (1.9 m) for comparison.



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 126 **Figure S2.** Pole-based measurements of CH₄ mixing ratios by measurement height relative to the
 127 surface performed outside of stations' fencelines (see Vollrath et al., 2026 for more details on the
 128 flux plane pole method). (a) Station C on 24 October 2024 and (b) Station B on 3 January 2025.
 129 The heights at which the highest mixing ratios were measured were generally consistent with the
 130 heights of line heater exhaust stacks and their incomplete combustion CH₄ plumes.

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