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a potential positive feedback loop**

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Floating algal beds and methane dynamics: a potential positive feedback loop

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Abstract

Eutrophic shallow freshwater ecosystems often develop floating filamentous microalgae on their surface during spring and summer, known as floating algal beds (FLAB). In recent years, FLAB has become more frequent and pronounced due to rising temperatures and drier conditions, sometimes even covering the entire surface of water bodies. New evidence suggests that phytoplankton can produce methane (CH₄) and it has also been reported that algal-derived carbon can enhance CH₄ production in the sediments, raising the possibility that FLAB may increase CH₄ emissions. However, FLAB may also reduce CH₄ emissions by decreasing CH₄ diffusion at the air-water interface and/or trapping CH₄ bubbles below the mat, thereby increasing the opportunity for microbial CH₄ oxidation before release to the atmosphere. Consequently, the net impact of FLAB on carbon emissions from freshwater ecosystems remains unclear. To address this knowledge gap, a field experiment consisting of a treatment covered with FLAB and a control (no FLAB) was carried out in a eutrophic shallow ditch. Diffusive and ebullitive CH₄ emissions increased by 12-fold and 5-fold, respectively, in the presence of FLAB, resulting in a 5-fold increase in CO₂-equivalent emissions. This increase appears to be linked to enhanced CH₄ production in the sediments fuelled by FLAB derived organic carbon, which was mostly relevant when anoxia developed beneath the mat. Overall, these findings indicate that FLAB blooms can substantially amplify carbon emissions from shallow aquatic ecosystems, with effects driven not only by FLAB biomass but also by mat-induced changes in water column dynamics and by intrinsic sediment properties.

Key words

Carbon emissions, ditches, ebullition, diffusion, sediment, freshwater ecosystems, eutrophication, oxidation, greenhouse gas

Highlights

- FLAB affected CH₄ and CO₂ fluxes from the ditch
- Total CO₂ equivalents were fivefold higher in the presence of FLAB
- FLAB effects depend on water column dynamics and sediment conditions

Introduction

Some species of filamentous freshwater algae can form floating clusters in wind-sheltered habitats (Hillebrand 1983). These clusters are often referred as metaphyton, pseudoplankton, pond scum or floating algal beds (FLAB) (Hillebrand 1983; Pikosz 2015; further used here). The initial development of these algae generally occurs at the sediment surface, where they survive through winter. After a period of submerged growth, they form tangled filamentous colonies that trap oxygen bubbles, which enables the colonies to rise to the surface where they continue to grow (Pikosz and Messyas 2015; Mendoza-lera and others 2016; Pikosz and others 2017; Gladyshev and Gubelit 2019). This event typically occurs in spring to early summer, when increasing water temperatures, longer days, and higher radiation create key environmental conditions that promote floating algae development (Pikosz and Messyas 2015; Gladyshev and Gubelit 2019). The rapid growth of FLAB is often followed by an equally rapid decay and decomposition phase when temperature and radiation decrease, where senescent masses sink or are washed ashore sometimes generating huge ecological and economic impacts (Gladyshev and Gubelit 2019). Floating mats can accumulate harmful concentrations of *Escherichia coli* (Whitman and others 2003) and disrupt ecosystem food webs (Page and others 2022), leading to negative consequences in the ecosystem. These effects taken together, alongside their wide distribution, contamination tolerance, occurrence in eutrophic habitats, and ease of identification, have led to the use of FLAB as indicators of deteriorating water quality (Whitton 1984; Philips 1990; Commission 2014; Gladyshev and Gubelit 2019). In addition, these dense floating algal mats shade the water column and may cause anoxia, inducing the death of deeper FLAB layers and of other organisms, ultimately reducing species diversity (Gladyshev and Gubelit 2019). They can also impact biogeochemical cycles through their impact on light availability, oxygen dynamics, organic matter accumulation, and nutrient cycling (Green and Fong 2016). While these ecological and biogeochemical impacts are considerably well documented, their consequences for the production, consumption, and emission of the major greenhouse gases methane (CH₄) and carbon dioxide (CO₂) remain poorly understood. As a result, the net effect of FLAB on aquatic greenhouse gas budgets is currently difficult to predict and therefore to include into ecological models.

Laboratory studies applying algal material directly onto sediment cores show that algae markedly increase CH₄ production (Uz and others 2007; Schwarz and others 2008; West and others 2012; Liang and others 2016), likely because algal carbon is more readily decomposed by methanogens than terrestrial carbon (West and others 2012; Grasset and others 2018). However, these experiments were all laboratory based, whereas in natural systems FLAB blooms develop at the water surface. As they age, deeper layers can decay, remain suspended, or accumulate in sediments, potentially influencing CH₄ dynamics throughout the whole water column. FLAB mats can affect

O₂ concentrations below the floating mat, which is a key driver of both CH₄ production and oxidation (Conrad 1999; Borrel and others 2011). They might also be able of producing CH₄, as shown for some phytoplankton taxa (Bižić and others 2020; Klintzsch and others 2020, 2023; Baliña and others 2025), suggesting that FLAB could be an overlooked source of CH₄. FLAB may also exert a physical effect by trapping CH₄ bubbles beneath the mat - as has been described for other types of floating vegetation (Attermeyer and others 2016; Kosten and others 2016) - diminishing ebullition and reducing the water-atmosphere gas exchange, thereby increasing CH₄ residence time and providing greater opportunity for microbial CH₄ oxidation before release to the atmosphere (Kosten and others 2016). At the same time, FLAB may also act as a strong daytime CO₂ sink, although this effect could be reversed at night (Peixoto and others 2016). Taken together, the net effect of FLAB on ecosystem carbon fluxes remains difficult to predict.

FLAB is usually favoured to grow in eutrophic and shallow systems with stagnant waters, limited wave and wind action (Pikosz and Messyasz 2015; Gladyshev and Gubelit 2019), such as drainage ditches. In the Netherlands, FLAB occurrence and proliferation in ditches during spring and summer - driven by inputs from agricultural wastewater and manure from surrounding pastures - were already reported more than forty years ago (Hillebrand 1983; Simons and Beem 1990; Simons 1994). Since then, continued eutrophication, higher irradiation in spring, rising temperatures, and increasingly dry, drought-prone conditions that promote stagnant water (KNMI 2026) have likely further intensified FLAB development, where they can sometimes even cover the entire surface of the ditch (Fig. S1). These climatic conditions are expected to promote even more frequent FLAB blooms in the future, yet their *in-situ* effects on CH₄ and CO₂ dynamics remain poorly understood, leading to an important knowledge gap in terms of total GHG emissions from eutrophic ditches. In this study, our main goals are: I) evaluate the effect of FLAB on the total GHG carbon emissions of a eutrophic ditch, by measuring CO₂ and CH₄ emissions in the presence and absence of FLAB; and II) identify the potential mechanisms driving changes in CH₄ emissions in the presence of FLAB. We hypothesize that: 1) both diffusive and ebullitive CH₄ emissions will increase in the presence of FLAB, whereas CO₂ emissions will decrease, changing the total ecosystem C-emissions; and 2) increased CH₄ emissions will be primarily driven by an extra input of algal organic matter in combination with anoxic conditions below the floating mat. To address these hypotheses, we carried out a five-day field experiment in a eutrophic Dutch ditch using eight open-bottom/open-top cylinders, four covered with FLAB and four left uncovered as controls. We directly measured or indirectly estimated all the CH₄-related processes: CH₄ diffusive and CH₄ ebullitive emissions, dissolved CH₄ concentrations and CO₂ diffusive emissions, were measured *in-situ* on a daily basis; incubations were carried out to estimate methane oxidation (MOX) rates, FLAB-related CH₄

production, and sediment CH₄ production. Emission measurements were used to evaluate potential changes in the total ecosystem C-emissions, whereas CH₄ mass balances were conducted for each replicate to investigate the potential drivers underlying FLAB effects on CH₄ dynamics.

Methods

1. Study site

Field experiments were carried out in a eutrophic drained ditch (51°55'18" N, 5°48'10" E) in the Netherlands, between 23rd and 30th August 2024. This region is used for intense agriculture with substantial agricultural runoff (RIVM 2024). The local climate is temperate marine, with temperatures ranges of 3 – 7°C in winter and 17 – 25°C in summer. The month August in the year 2024 was warm, with a mean temperature of 19.3°C (KNMI, 2024). The ditch was selected based on observed FLAB occurrences in previous years.

2. Field experiments

Experiments consisted of deploying eight enclosures made of transparent polycarbonate of 1mm thickness, with a size of 1m in height and 0.5m in diameter (maximum volume of 196 L and a surface area of 0.2 m²) (Fig. S2). The lower 0.3 m of each enclosure was fitted with a stainless-steel rim to improve sediment grip and enhance overall stability (Fig. S2a, b). The surface and bottom of the enclosures were open to include all the relevant production and consumption CH₄ pathways associated with both sediment and water column processes, whereas lateral transport was inhibited by the walls. Four enclosures were covered with 4000g wet weight (WW; ~7 cm of height) of freshly collected FLAB (Fig. S2e) and four remained as a control, without FLAB. As no FLAB developed in the study ditch on August 2024, FLAB was collected from a nearby location (51°52'17.6" N, 5°51'04.9" E).

Inside all the enclosures an inverted plastic funnel attached to a glass bottle was placed, to collect gas bubbles. Also, in two treatment and two control replicates (randomly selected), and in the ditch (downstream the enclosures) oxygen and temperature high frequency sensors (MiniDOT, PME®) were placed 0.5m below the water surface (Fig. S2c), to posteriorly derive ecosystem metabolism rates. The enclosures were placed in the ditch on 23rd of August and left for 72hs to stabilize. Prior to installing the enclosures, sediment was inspected and any submerged macrophytes were removed. After placement, a fish net was used to ensure that the enclosures were fishless. On the 26th of August, FLAB was added, together with bubble traps and MiniDOTs. The measurements lasted until the 30th of August. To account for potential effects of the enclosures on CH₄ and CO₂

emissions, a set of four automatic chambers was also deployed directly in the ditch, downstream of the enclosures, from 26th to 30th August (Fig. S2d).

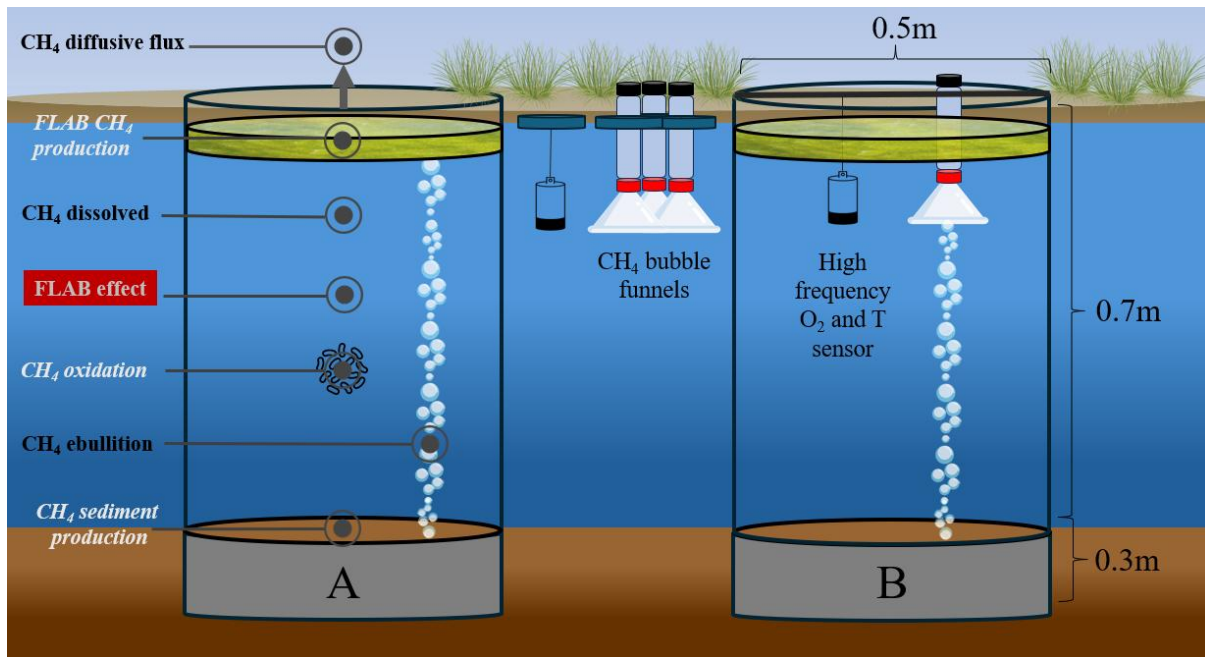


Figure 1. Schematic representation of the experimental design. A) Includes all the CH₄ related processes that were either directly measured (black and bold) or indirectly estimated (white and italics); B) includes dimensions of the enclosures, as well as the general setup, including the high frequency O₂ and T sensors (MiniDOT, PME®) and the bubble funnel; C) One MiniDOT and four bubble funnels were also placed in the ditch, attached to floating devices.

3. Limnological characterization

Remaining FLAB at the end of the experiment was collected from the surface of each replicate, its wet weight (WW) was recorded, and samples were dried at 70°C (Universal oven, Memmert, Germany) until constant weight, at which point the dry weight (DW) was determined. The WW:DW ratio obtained at the end of the experiment was applied to the initial WW to estimate the initial DW.

In addition to the high frequency sensors (MiniDOT, PME®), oxygen (O₂) and temperature (T) profiles were measured at 10 cm intervals (from just below the water surface until sediment) in each replicate and in two locations in the ditch (upstream and downstream of the enclosures), once per day every day. With the same frequency, subsurface (within the first 5cm) pH and conductivity were recorded for each enclosure and the ditch. All these measurements were taken using a portable multiparameter meter (HQ Series, Hach Company, Loveland, CO, USA) equipped with corresponding sensors (Hach, USA). On the 29th of August an irradiance profile was also carried out in one FLAB replicate, two control replicates and in the ditch. Photosynthetically active radiation (PAR, 400 – 700 nm) was measured using a LI-COR LI-250 Light Meter (LI-COR Biosciences, Lincoln, NE,

USA) coupled to a submersible quantum sensor US-SQS/L (WALZ Mess- und Regeltechnik, Effeltrich, Germany). Measurements were taken every 10cm from subsurface up to 50cm. The vertical light attenuation coefficient ($K_d \text{ PAR}$) was estimated by fitting a linear regression between depth (m) and the natural logarithm of downwelling PAR irradiance ($\mu\text{mol photons m}^{-2} \text{ s}^{-1}$), where the regression slope corresponds to $K_d \text{ PAR}$ ($\ln I = K_d \text{ PAR} \times \text{depth} + b$) (Kirk 2011). The euphotic depth, defined as the depth receiving 1% of surface PAR, was calculated by inserting $\ln (0.01 \times \text{surface irradiance})$ into this regression and solving for depth (Kirk 2011).

On the first and last day of the experiment subsurface water samples (within the first 10cm) were collected from each replicate and the ditch to carry out the following analyses: a) phosphate (PO_4^{3-}), nitrate (NO_3^-) and ammonium (NH_4^+) concentration (from 15ml of water preserved at -20°C), on a SEAL AA3 HR AutoAnalyzer (SEAL Analytical) using standard methods; b) total organic carbon (TOC) from unfiltered water and dissolved organic carbon (DOC) from water filtered through GF/F glass microfiber filters (1.2 μm pore size, 47 mm diameter; Cytiva Whatman, Maidstone, UK). In both cases, 10 ml samples were preserved with 0.1 ml 2M HCl solution at 4°C upon analysis, on a Analytik Jena multi-N/C 3100 analyzer; c) Chlorophyll a (Chla-a) from a known volume of water filtered through glass GF/C microfiber filters (1.2 μm pore size, 47 mm diameter; Cytiva Whatman, Maidstone, UK), posteriorly stored at -20°C . Upon analysis, Chl-a was extracted using 10ml of 95% cold ethanol and left overnight at 4°C and under dark conditions. After 24hs, the absorption in the wavelengths of 665 and 750 was measured before and after acidification with 0.12N HCl solution (ISO 10260, 1992).

4. Ecosystem metabolism

Ecosystem gross primary production (GPP), respiration (R) and net ecosystem production (NEP) rates were estimated by means of high-frequency oxygen and temperature data (miniDO₂T, Precision Measurement Engineering, Inc.®), following Soued and Prairie (2021). Ecosystem metabolism rates were calculated based on a diurnal open system O₂ model (Odum, 1956), where changes in O₂ concentration are a function of GPP, ER, and O₂ exchange at the water-air interface (K_{O₂}), following equation 1.

$$\frac{dO_2}{dt} = \frac{GPP}{Z_{epi}} + \frac{ER}{Z_{epi}} + K_{O_2}(O_{2 \text{ sat}} - O_2) \quad \text{equation 1}$$

Where Z_{epi} is the epilimnion depth, which in our case is the mean depth of each enclosure or the ditch, respectively, for the entire duration of the deployment. $O_{2 \text{ sat}}$ is the theoretical concentration of O₂ at saturation, considering the in-situ temperature and atmospheric pressure. O_2 is an empirically measured oxygen concentration in the water. Detailed equations of the model can be found in Hall & Hotchkiss (2017).

Daily estimates of GPP and ER were obtained through maximum likelihood using equation 1 and the R package Stream Metabolizer (Appling and others 2018). Net daily primary production (NPP) was then calculated as GPP

- ER. A final mean value $\pm$ standard deviation of GPP, ER, and NPP was obtained for each replicate and the ditch for the entire duration of the experiment.

5. Greenhouse gas dynamics

5.1 CH₄ dissolved in the water

The concentration of CH₄ dissolved in the water was obtained by means of the headspace technique (Magen and others 2014). Approximately 6ml of water was injected into 12ml pre-vacuumed exetainers (Labco exetainer®) containing 0.1ml of H₂SO₄ 1M as fixing solution and afterwards stored at room temperature. Upon analysis, the samples were flushed with pure N₂ to equilibrate pressures, vigorously shaken for 2 minutes to ensure mixing between the air and water phases, and posteriorly 100 μ l (by triplicate) analysed in a methane GC-FID (Shimadzu, Nexis, CG-2030) associated to an autosampler (Shimadzu, AOC-6000 Plus). Before every batch run, a calibration curve was made. CH₄ concentration in the sample was calculated according to Henry's law for the given temperature and salinity (Sander 2015).

In each of the eight replicates and in the two sites from the ditch (upstream and downstream of the enclosures), samples of dissolved CH₄ were taken once a day on the 26th (afternoon) and the 30th of August (morning), and twice a day (in the morning and afternoon) between the 27th and 29th, obtaining a total of eight samples for each enclosure as well as for the two points in the ditch. Each measurement had a methodological duplicate.

5.2 CH₄ and CO₂ fluxes

5.2.1. Air: water interface CH₄ and CO₂ fluxes from enclosures

CH₄ and CO₂ diffusive emissions (mg m⁻² d⁻¹) from the enclosures were obtained by placing a lid on top of the enclosures, which was connected to an ultra-portable greenhouse gas analyzer (GGA, Los Gatos Research, ABB Inc., San Jose, CA, USA), creating a closed loop. The lid was made from transparent polycarbonate (0.6cm thick), had an extra sealing rim covering the external borders of the internal face to improve the sealing (1cm width), and a surface of 0.2m² (Fig. S3). Each measurement lasted three minutes and, since measurements were monitored in real time, any abrupt increase in CH₄ emissions during the three-minute deployment was considered as a CH₄ bubble intrusion, and the diffusive flux measurement was discarded and repeated. The height of the headspace of each enclosure was measured every day, to account for any potential differences water level. The diffusive fluxes were calculated based on robust linear models using the gasfluxes package (Fuss 2024) in R (R Core Team 2025), following equation 2, 3 and 4 (Zhao and others 2018).

$$F = \frac{10VP_0 \left(1 - \frac{W_0}{1000}\right) f_0}{RS (T_0 + 273.15)} \quad \text{equation 2}$$

where V (cm^3) is the chamber volume, P_0 (kPa) is the initial air pressure, W_0 (mmol mol^{-1}) is the initial water vapor mole fraction, f_0 is the initial rate of change in water-corrected CO_2 or CH_4 mole fraction ($\mu\text{mol mol}^{-1}$) inside the chamber, R is the gas constant ($8.314 \text{ Pa m}^3 \text{ K}^{-1} \text{ mol}^{-1}$) and T_0 ($^\circ\text{C}$) is the initial air temperature. To estimate f_0 a linear regression algorithm was used, using the least squared method to fit a straight line (equation 3)

$$C = a_0 + a_1 t \quad \text{equation 3}$$

Where a_0 and a_1 are the intercept and slope of the regression line, respectively, and t is the time. Considering this, f_0 can be calculated as

$$f_0 = \frac{\partial C}{\partial t} \int_{t=t_0}^{\cdot} = a_1 \quad \text{equation 4}$$

Average wind (m s^{-1}), atmospheric pressure (hPa) and atmospheric temperature ($^\circ\text{C}$) were recorded in situ during diffusive flux measurements, using a hand-anemometer (Kestrel 3000 Pocket Weather Meter, Nielsen-Kellerman Co., Boothwyn, PA, USA). These diffusive fluxes were measured in total eight times in each enclosure, twice a day (in the morning and afternoon) between the 26th and 29th of August, and only in the morning on the 30th of August. Diffusive flux measurements were coupled to CH_4 dissolved sample retrieving, and they were all done during daytime.

5.2.2 Air: water interface CH_4 and CO_2 diffusive fluxes from the ditch

Downstream the enclosures, four floating, transparent, and automated cylinder-shaped chambers (height = 51 cm, inner diameter = 39 cm) were deployed (Fig. S2d). Each chamber was placed on top of a floating collar to ensure buoyancy and tied to both sides of the ditch to avoid drifting. Chambers had a transparent flat lid associated to a stepper motor, which was connected to a multiplexer with an integrated pump (2.5 L min^{-1}) (Nijman and others 2024). The multiplexer ensured that one chamber was closed at a time and facilitated gas circulation between the chambers and an ultra-portable greenhouse gas analyzer (GGA, Los Gatos Research, ABB Inc., San Jose, CA, USA). The CO_2 and CH_4 flux inside each chamber were measured for 3-min and followed by 30 seconds flushing time in between closures. A temperature logger (HOBO Pendant MX Temp, Onset Computer Corporation, Bourne, MA, USA) was placed inside each chamber, to continuously record air temperature. Total fluxes ($\text{mg m}^{-2} \text{ d}^{-1}$) were calculated as described in section 5.2.1, following equations 2, 3 and 4. This automatic setup was powered by batteries, since there was no access to the electrical grid. This method of powering the system introduced problems that led to occasional interruptions in data logging.

Since CO_2 and CH_4 fluxes were recorded semi-continuously, these measurements include total fluxes: diffusive CH_4 emissions but potentially CH_4 ebullitive emissions too. Given that the latter were accounted for with bubble

funnels, these were not obtained from the semicontinuous data. All 628 measured fluxes were individually inspected for CH₄ bubble intromission and to assure linearity. From the whole data set, 32% had to be removed because it had either CH₄ bubble intromissions, not a linear CH₄ increase or started with a very high CH₄ baseline, the remaining 68% fulfilled the requirements needed to be compared with the diffusive fluxes from the enclosures.

5.2.3 CH₄ ebullitive emissions

CH₄ ebullitive emissions (mg m⁻² d⁻¹) was estimated in each enclosure and in the ditch, by placing funnels with an area of 0.03 m² attached to inverted 350 ml glass bottles filled with water. One funnel was placed in each replicate (Fig. S4a), and four funnels attached to floaters were placed in the ditch (Fig. S4b), upstream the enclosures. When enough volume was accumulated, 3ml samples of the bubbles were retrieved using a needle connected to a 3ml syringe through their rubber stopper, placed in 3ml pre-vacuumed exetainers (Labco exetainer ®) and stored in room temperature until analysis. Upon analysis, 50µl of the sample (by triplicate) was injected in a GC-FID (model 5890A, Hewlett-Packard, Palo Alto, CA, USA) First, the concentration of CH₄ (mg CH₄ L⁻¹) in the sample was obtained, considering the volume of sample injected (50µl), the slope of the calibration curve (area standard * nmol CH₄ standard⁻¹) and the molar mas of CH₄ (16.04 g mol⁻¹). CH₄ ebullitive flux was obtained using equation 5.

$$CH_4 \text{ ebullitive flux} = \frac{CH_4 \text{ concentration} * \text{Total volume collected}}{\text{Funnel area} * \text{Deployment time}} \quad \text{equation 5}$$

Where CH₄ ebullitive flux (mg m⁻² d⁻¹) is obtained considering the concentration of CH₄ in the gas sample (mg L⁻¹), the total volume of sample collected (L) in the bubble trap, the area of the funnel (m²) and the total deployment time (days).

5.2.4 Sediment: water interface CH₄ diffusive emissions

The diffusive CH₄ emissions from sediment cores (mg m⁻² d⁻¹) were obtained by taking a core from the ditch using a 1.2m height and 0.6m diameter acrylic liner. After extraction, part of the water column was gently removed, the headspace height was measured, and the core was set to rest for approximately an hour. Upon measurement, a lid with two connectors was placed on top of the core and connected to the GGA, creating a closed loop. Cores were taken from the ditch, downstream and upstream of the enclosures, on the 23rd and 29th of August. This procedure was repeated on the 18th and 24th of October, to assess potential temporal variability. All the cores were taken within approximately 3 meters of total distance and close to the experimental setup area. No cores were extracted from the enclosures, to avoid resuspension of sediments and, therefore, affecting the treatments. The diffusive sediment CH₄ fluxes were calculated as described for the enclosures, following equation 2, 3 and 4 (Zhao and others 2018).

5.3. CH₄ standardize gas exchange velocity (K_{600} CH₄)

CH₄ dissolved concentrations and CH₄ diffusive emissions in the air: water interface from the ditch and the treatments, alongside the wind measurements, were used to calculate the standardized exchange velocity for each case and each day (K_{600} CH₄). A detailed description of this calculation can be found in Suppl. Inf. 1.

5.4 Total GHG emissions (as CO₂ equivalents)

Total GHG emissions were estimated by summing CH₄ diffusive and ebullitive emissions (converted to CO₂ equivalents) and CO₂ diffusive emissions. We used a global potential warming (GPW) of 27 in a 100-year horizon for CH₄ (Forster and others 2021).

Because CO₂ diffusive fluxes were measured only during daytime, a correction was applied to account for higher nighttime emissions. Based on published studies comparing daytime and nighttime CO₂ fluxes in open water (Liu and others 2016; Attermeyer and others 2021; Gómez-Gener and others 2021) and floating macrophyte stands (Peixoto and others 2016), mean correction factors of 0.45 ± 0.22 and 0.43 ± 0.13 were derived, respectively. Nighttime fluxes were estimated by multiplying the measured daytime fluxes by the appropriate correction factor, assuming that systems acting as daytime CO₂ sinks became nighttime sources. Mean daily CO₂ fluxes were then calculated from the combined daytime and estimated nighttime values.

For CH₄ ebullitive emissions, two adjustments were applied to calculate CO₂-equivalent emissions. First, the sampling frequency differed between the ditch and the treatment: bubble funnels in the ditch accumulated enough bubbles for sampling on three separate days, whereas those in the control and FLAB treatments were sampled twice. Although individual fluxes were standardized to deployment duration, the unequal number of samples could still bias comparisons. To minimize this bias, we calculated CO₂-equivalent emissions based on the total mass of CH₄ emitted during the experimental time, rather than on individual flux measurements. For each replicate, the mass of CH₄ collected in all ebullition samples was summed and normalized by area (mg m^{-2}). This represents the total CH₄ mass released over the entire monitoring period. We then divided this total mass by the total deployment time (in days) for that replicate - whether from the ditch or from the treatments. The resulting rate ($\text{mg CH}_4 \text{ m}^{-2} \text{ d}^{-1}$) was then converted into CO₂ equivalents. This approach provides a more consistent and comparable estimate because it accounts for differences in sampling frequency between replicates and the ditch. Second, ebullitive CH₄ emissions measured in the FLAB treatment represent bubbles captured beneath the floating algal mat, but not necessarily the amount that reached the atmosphere. Floating mats can trap bubbles, reducing the fraction that escapes. To account for this potential retention, we applied a correction factor derived from Kosten et al. (2016), who quantified bubble retention under various types and densities of floating vegetation. Although

their vegetation types differed from the FLAB mats used in this study, they offer the best available analogue in literature. They reported bubble retention between 10% and 40%, with higher retention associated with greater biomass. We therefore applied 10% and 40% retention factors to the median CO₂ equivalents derived from CH₄ ebullition from the FLAB system, to estimate the corresponding lower- and upper-bound potential emission scenarios.

6. Methane oxidation rates (MOX) in the water

To estimate methane oxidation rates (MOX) in the water, water from the ditch itself was taken on the 27th of August and incubated in a total of eight 120ml glass bottles. In each bottle, 20ml of ditch water was placed, leaving a headspace of 100ml, 1 ml of pure CH₄ was added (1% of the headspace's volume) and bottles were sealed with rubber stoppers and aluminium crimp caps using a manual crimper, to ensure airtight conditions (Nijman and others 2022). Water was incubated under complete dark or complete light conditions, and there were four replicates per treatment. The incubation bottles were placed on an orbital shaker (GIO Gyrotory® Shaker, New Brunswick Scientific Co., Inc., Edison, NJ, USA), at 150 r.p.m, to ensure continuous mixing of the water and headspace phases, in a room at 21°C. The concentration of CH₄ in the headspace of the bottles was measured every day for 5 days, by injecting a 100µl sample (by triplicate) of the headspace of each bottle in a GC-FID (model 5890A, Hewlett-Packard, Palo Alto, CA, USA). The µmol of CH₄ in the headspace were calculated considering the area of the peak, the slope of the calibration curve and the volume (ml) of the headspace in the bottle. Afterwards, the nmol of CH₄ dissolved in the water phase were obtained following equation 6.

$$CH_4dissolved = \frac{CH_4headspace * CH_4solubility}{\frac{water\ volume}{headspace\ volume}} \quad \text{equation 6}$$

Where CH₄ dissolved (nmol) corresponds to the CH₄ dissolved in the water, CH₄ in the headspace (nmol) is the mass of CH₄ in the headspace phase, CH₄ solubility is obtained as $CH_4solubility = Kh * RT$, where Kh for 293K and 1atm pressure is 0.0015 M/atm, and water volume (ml) divided by headspace volume (ml) corresponds to the ratio between the headspace and water phases. The final concentration of CH₄ in µmol L⁻¹ was obtained by relativizing for the water volume (L) in each incubation bottle, and by converting nmol to µmol. From these incubations, a regression between CH₄ dissolved (µmol L⁻¹) and time (days) was obtained, where the slope corresponds to the CH₄ oxidation (MOX) rate (µmol L⁻¹ day⁻¹).

7. FLAB-related CH₄ production

To evaluate the potential for FLAB- related CH₄ production, 120ml glass bottles containing either only 20ml of ditch water (control) or 20ml of ditch water + 0.5gr of FLAB wet weight (treatment), in both cases leaving a 100ml headspace, were incubated under different temperature and CH₄ concentration conditions: 1) light and no

extra CH₄ addition; 2) light and 1ml of CH₄ added; 3) dark and no extra CH₄ addition; 4) dark and 1ml of CH₄ added. Bottles were sealed with rubber stoppers and aluminium crimp caps, to ensure airtight conditions. Incubation bottles were placed in a room with a controlled temperature of 21°C and on an orbital shaker (GIO Gyrotory® Shaker, New Brunswick Scientific Co., Inc., Edison, NJ, USA), at 150 r.p.m. The concentration of CH₄ in the headspace of the bottles was measured every day for 5 days, by injecting a 100µl sample of the headspace of each bottle in a GC-FID (model 5890A, Hewlett-Packard, Palo Alto, CA, USA) with manual injection. Alongside the samples, a calibration curve was also run. The µmol of CH₄ in the headspace were calculated considering the area of the peak, the slope of the calibration curve and the volume (ml) of the headspace in the bottle. Afterwards, the nmol of CH₄ dissolved in the water phase were obtained following equation 6. The final concentration of CH₄ in µmol L⁻¹ was obtained by relativizing for the water volume (L) in each incubation bottle. To ensure the incubation bottles did not become anoxic, O₂ concentrations in all the bottles were measured at the end of the incubation period using a Microx TX3 oxygen microsensor (flat-broken needle tip, Presens, Germany).

8. Sediment incubations to assess sediment CH₄ production and oxidation.

On the final day of the experiment (30th of August), three different 120cm core liners were used to extract one core from the ditch, one core from one of the control replicates and one from the FLAB replicates, the last two randomly selected. Back in the laboratory, each core was sliced to prepare incubations to estimate sediment CH₄ production (PROD) and CH₄ oxidation (MOX) rates. From each core, the first 2cm were incubated to estimate MOX rates, whereas the second following 4cm were incubated to estimate PROD rates, following Nijman and others 2022 and Struik and others 2024. For MOX rates, approximately 5g of wet sediment weight were placed in 120ml glass bottles with 15ml of water coming from that same system, and five replicates per core were created. Each bottle was sealed with rubber septa and aluminium crimp caps using a manual crimper to ensure airtight conditions. After sealing, a volume corresponding 10% of the headspace of the bottle (1ml) of pure CH₄ was injected to each bottle. Methane concentration in the headspace of each bottle was measured twice a day for five days. For PROD rates, approximately 25g of wet sediment wet weight was placed in a 120ml glass bottle with 15ml of water coming from that same system (previously flushed with pure N₂ to remove O₂), also creating five replicates per core. The preparation of PROD incubations was done in an anoxic chamber to ensure anoxic conditions. Methane concentration in the headspace of each bottle was measured once a day for five days. All MOX and PROD bottles were placed in an orbital shaker (GIO Gyrotory® Shaker, New Brunswick Scientific Co., Inc., Edison, NJ, USA), at 150 r.p.m, in a room with controlled temperature of 21°C and under complete dark conditions. The concentration of CH₄ in the headspace of each bottle was measured using a GC-FID (model

5890A, Hewlett-Packard, Palo Alto, CA, USA) with manual injection. The nmol of CH₄ in the headspace were calculated considering the area of the peak, the slope of the calibration curve and the volume (ml) of the headspace in the bottle. Afterwards, the nmol of CH₄ dissolved in the water phase were obtained following equation 6. Once the incubations were over, all the incubation bottles were opened and placed in a 70°C drying oven (Binder GmbH, Tuttlingen, Germany) until constant weight. Sediment dry weight was recorded for each replicate and finally rates of CH₄ production as nmol day⁻¹ g dry or wet weight⁻¹ were obtained.

9. CH₄ mass balance in the enclosures

To assess the effect of FLAB on ditch CH₄ dynamics, CH₄ mass balances were carried out for each replicate. Because the side walls of the enclosures substantially reduced lateral transport (Suppl. Inf. 2), lateral inputs were considered negligible and were therefore excluded from the mass balance. Also, since this ecosystem is very shallow (less than one meter depth), CH₄ bubble dissolution in the water column was considered as negligible (Joyce and Jewell 2003; McGinnis et al. 2006). Consequently, the change in CH₄ dissolved in the enclosures (ΔCH_4) would be the result of the sum up of sediment flux (*Sed*) plus the effect of FLAB (*FLAB*, below explained in detail), minus CH₄ oxidation in the water column (*MOX*), and CH₄ diffusion to the atmosphere (*DIF*), following equation 7.

$$\Delta CH_4 = Sed + FLAB - (MOX + DIF) \quad \text{equation 7}$$

The effect of FLAB accounts for different potential processes: CH₄ production directly by FLAB, changes in MOX rates below the floating mat due to changes in CH₄ and O₂ concentration, enhancement of CH₄ production in the sediments due to FLAB decomposition (leading either to higher CH₄ diffusive emissions, but also potentially enhancing CH₄ bubble formation and, due to the presence of the FLAB mat, potentially bubble accumulation below the mat) in combinations with decreased O₂ concentration below the FLAB mat, that might furthermore favour CH₄ production. A schematic description of all effects can be found in Fig. S5.

Some of the components of the mass balance (equation 7) were measured directly *in situ* (such as ΔCH_4 and *DIF*, explained in sections 5.1 and 5.2.1, respectively) whereas others were estimated indirectly (*Sed*, *FLAB*, and *MOX*). Below, a description of how each one of these indirect processes were estimated is explained. In Table 1 the parameters used for each one of the estimations are detailed.

9.1. *Sed*: modelling sediment CH₄ production

Sediment CH₄ production rates (*Sed*) were measured through flux measurements from extracted cores (section 5.2.4) and by sediment incubations (section 8). Two different methods were used to have a more reliable and accurate estimation of the potential sediment CH₄ production rates. For the mass balance, a set of three potential

sediment production rates were used, and the best fit was selected. Also, *Sed* was corrected for the temperature in the sediments (which was measured *in situ* every day, in each enclosure) following equation 8 (Segers 1998).

$$P_{sedT} = P_{sed} * Q_{10\ sed}^{\frac{(T_{sed}-T_{ref})}{10}} \quad \text{equation 8}$$

Where P_{sedT} refers to the production of CH₄ in the sediments corrected by the temperature normalized by the area of the enclosure (μmol day⁻¹), P_{sed} is the non-corrected CH₄ production in the sediments (μmol day⁻¹), $Q_{10\ sed}$ was considered 3 (Table 1), T_{sed} is the temperature in the sediments (°C) and T_{ref} was considered 20°C (Table 1).

9.2. MOX: modelling methane oxidation (MOX) rates in the water

The methane oxidation rate (MOX, μmol L⁻¹ day⁻¹) was obtained as described in section 6. To estimate the mass of CH₄ oxidized at each time point, MOX was corrected for the temperature in the water following equation 9 (Segers 1998; Thottathil and others 2019).

$$MOX_T = MOX * Q_{10\ mox}^{\frac{(T_{water}-T_{ref})}{10}} \quad \text{equation 9}$$

Where MOX_T is the temperature corrected MOX rate (μmol L⁻¹ day⁻¹), MOX is the MOX rate obtained from the incubations (μmol L⁻¹ day⁻¹), $Q_{10\ mox}$ was considered 2 (Table 1), T_{water} is the subsurface water temperature in the enclosures (°C) and T_{ref} is the reference temperature (20°C) (Table 1).

Because aerobic MOX depends on the availability of both O₂ and CH₄, either substrate may become limiting. Therefore, the MOX rate was additionally corrected using a dual-substrate Monod formulation, following equation 10 (Segers 1998; Martinez-Cruz and others 2015).

$$MOX_{corr} = MOX_T * \frac{(CH_4)}{(KCH_4 + CH_4)} * \frac{(O_2)}{(KO_2 + O_2)} \quad \text{equation 10}$$

Where MOX_{corr} is the MOX rate corrected by O₂ concentration, CH₄ concentration and temperature (μmol L⁻¹ day⁻¹), MOX_T is the temperature corrected instantaneous MOX rate (day⁻¹) obtained from equation 9, CH_4 is the concentration (μmol L⁻¹) at each time point, KCH_4 is the half saturation constant of CH₄ for MOX (μmol L⁻¹, Table 1), O_2 is the subsurface O₂ concentration in the enclosure at each time point (mg L⁻¹) and KO_2 is the half saturation constant of O₂ for MOX (mg L⁻¹, Table 1).

9.3 FLAB: modelling FLAB effect as CH₄ production from a pool of decayed organic matter

The potential for CH₄ production induced by FLAB was estimated through laboratory incubations, and the indirect effect that the floating may exert on MOX rates by changing O₂ and CH₄ concentrations below the mat are also considered within the MOX corrections explained in section 9.2. Therefore, in the mass-balance model the FLAB component was considered as an additional source of CH₄ production in the sediments due to decomposition of

the organic carbon (OC) in the decayed pool of FLAB. The consumption of OC was modelled following equation 11 (Westrich and Berner 1984; Adair and others 2010; Forney and Rothman 2012).

$$\frac{dOC}{dt} = I - k * OC(t) \quad \text{equation 11}$$

Where $\frac{dOC}{dt}$ is the change in the organic carbon (OC) pool in time, I is the input rate of OC (gr day⁻¹), k is the decay constant for OC decomposition coming from phytoplankton (day⁻¹) and $OC(t)$ is the organic carbon (g) at a certain time point.

This equation can be derived, and the solution is equation 12.

$$OC(t) = \frac{I}{k} (1 - e^{-kt}) \quad \text{equation 12}$$

The input rate of OC (I , gr day⁻¹) refers to the amount of organic carbon transferred to the sediments per unit of time. To calculate this rate, we first determined the total dry-weight loss of FLAB over the experimental period by subtracting the final dry weight from the initial dry weight. The corresponding organic carbon (OC) content was then estimated as 44.8% of the total dry-weight loss, following Grasset et al. (2018). This total OC loss (g) was divided by 48 hours (the period during which FLAB production peaks) to obtain the input rate expressed in g day⁻¹.

After this, the OC obtained from equation 12 was converted to CH₄ production, following equation 13 (Segers 1998).

$$CH_4 \text{ rate } (t) = f * k * OC(t) \quad \text{equation 13}$$

Where $CH_4 \text{ rate } (t)$ is the CH₄ production rate due to OC decomposition at a certain time point (gr day⁻¹), f is the fraction of OC that is converted to CH₄ (unitless), k is the decay constant of OC coming from phytoplankton (day⁻¹) and $OC(t)$ is the modelled OC (gr) at a certain time point, obtained from equation 12.

Table 1. Parameters used to model each one of the indirectly derived components of the mass balance.

Mass balance considerations		
Component	Parameter	Reference
<i>Sed</i>	Q _{10 SED} = 3 T _{ref} (°C) = 20	Segers 1998; Liikanen and others 2002; Duc and others 2010
<i>FLAB</i>	OC content in phytoplankton = 44.8 % k (day ⁻¹) = 0.034 f (unitless) = 0.01 – 0.04	Grasset and others 2018 Grasset and others 2018 Segers 1998
<i>MOX</i>	Q _{10 MOX} = 2 K _{O2} (mg L ⁻¹) = 0.25 K _{CH4} (μmol L ⁻¹) = 3	Segers 1998; Thottathil and others 2019 Guérin and others 2007 Segers 1998

The final mass balance used to model CH₄ concentrations in each replicate is detailed in equation 14.

$$CH_t = CH_{4\ t-1} + dt * (Sed + FLAB - (MOX + DIF)) \quad \text{equation 14}$$

Where $CH_{4_{new}}$ (μmol) is the modelled mass of CH_4 concentration at each time point, $CH_{4_{t-1}}$ (μmol) is the CH_4 mass at the previous time (the model was initiated with the CH_4 mass in each replicate at the onset of the experiment), dt is de delta time within each sampling point (day^{-1}), Sed is the corrected and surface scaled sediment CH_4 production rate ($\mu\text{mol day}^{-1}$), $FLAB$ is the volume scaled CH_4 production rate coming from FLAB decomposition ($\mu\text{mol day}^{-1}$), MOX is the corrected and volume scaled CH_4 oxidation rate ($\mu\text{mol day}^{-1}$) and DIF is the surface scaled CH_4 diffusive flux ($\mu\text{mol day}^{-1}$). It is important to notice that the Sed and DIF are surface related processes, whereas MOX and $FLAB$ are volumetric related processes, so each one of these rates were scaled to the area and volume, respectively, of each replicate at each time point. The surface of each replicate did not change throughout the experimental period, but the total volume inside each replicate had small changes that were considered in the calculations. Once the mass balance is done, the obtained $CH_{4_{new}}$ mass at each time point can be converted to concentration by scaling it to the volume of each replicate at each time point, and this is depicted in Fig. 6 and Fig. S15. This modelled CH_4 concentration can be compared to the observed dissolved CH_4 concentration in each replicate at each time point, to check if the predictive concentration fits the observed one.

10. Statistical analysis

All statistical analyses were performed in R (version 4.4.1; R Core Team 2025). Dissolved CH_4 concentrations were modelled using a generalized linear mixed-effects model (GLMM) with a Gamma distribution and a log link function, implemented in the glmmTMB package (Brooks and others 2017). Replicate ID was included as a random effect to account for repeated measurements over time. Given the large differences in variance among treatments, the model included a variance structure dependent on Treatment ($\text{dispformula} = \sim \text{Treatment}$) to improve model fit. Model diagnostics were evaluated using simulated residuals from the DHARMA package (Hartig 2023), including checks for uniformity and overdispersion, which indicated that the model adequately captured the data. Post-hoc pairwise comparisons of treatments within each sampling day were performed using estimated marginal means from the emmeans package (Lenth 2023), with Sidak adjustment for multiple comparisons, and compact letter displays were generated to summarize significant differences among treatments for each day.

Results

1. Limnological parameters

When including data for the whole experimental period, pH, conductivity, phosphate and ammonium were similar among the ditch, the control and FLAB replicates (Table 2). Parameters related to water turbidity, such as secchi depth, $K_d \text{ PAR}$, ash free dry weight (AFDW), dissolved organic carbon (DOC) and total organic carbon (TOC) were

similar between the ditch and the control treatment, but they were considerably higher in the FLAB treatment (Table 2). Similarly, CH₄ subsurface dissolved concentrations were higher in FLAB treatment, but similar between the ditch and the control treatment. Nitrate was similar between the control and FLAB treatment, but it was considerably higher in the ditch. The ecosystem metabolism based on diel O₂ fluctuations indicated an overall autotrophic metabolism for the ditch, a near-neutral metabolism for the control treatment and heterotrophic metabolism for the FLAB treatment. Note that we may miss autotrophic activity in the FLAB treatment as FLAB produced O₂ may have been emitted directly to the atmosphere and is not detected by the O₂ probes. When differentiating between beginning and end of the experimental period, the biogeochemistry in the ditch and control treatments changed little over time. In contrast, the FLAB treatment exhibited a clear shift, with higher dissolved CH₄ and elevated DOC concentrations at the end (Fig. S6).

The day-time temperature profiles for the ditch and the enclosures (Fig. S7) showed a consistent pattern across all treatments, with a well-mixed water column and similar temperature ranges. In contrast, day-time dissolved O₂ profiles (Fig. S8) exhibited treatment-specific dynamics. All systems began the experiment with similarly high O₂ subsurface concentrations, which declined over time but following different patterns. In the ditch, dissolved subsurface O₂ decreased from 13.3 ± 0.0 mg L⁻¹ to 3.0 ± 0.1 mg L⁻¹ by the end of the experiment. The control treatment showed a smaller decline, from 16.4 ± 0.9 mg L⁻¹ to 9.8 ± 0.3 mg L⁻¹. In the FLAB treatment, enclosures started at 15.3 ± 1.5 mg L⁻¹, but three (#1, #5, and #6) became nearly anoxic by the end (0.8 ± 0.4 mg L⁻¹), whereas #8 still had a concentration of 7.2 ± 0.1 mg L⁻¹ on the final day.

Table 2. Limnological parameters for the ditch, the enclosures control and the enclosures with FLAB. Values represent the mean for the experimental period $\pm$ standard deviation.

Parameter	Ditch	Control	FLAB
Secchi depth (m)	0.6 ± 0.1	0.6 ± 0.0	-
K _d PAR (m ⁻¹)	$5.0 \pm \text{NA}$	6.9 ± 5.3	$35.4 \pm \text{NA}$
Euphotic depth (m)	$0.9 \pm \text{NA}$	1.7 ± 1.3	$0.2 \pm \text{NA}$
Water T (°C)	20.3 ± 0.1	20.6 ± 0.1	21.1 ± 0.3
pH	7.6 ± 0.0	7.9 ± 0.1	7.9 ± 0.2
Conductivity ($\mu\text{S cm}^{-1}$)	585.8 ± 0.8	532.8 ± 4.1	532.9 ± 14.0
Dissolved O ₂ (mg L ⁻¹)	6.9 ± 0.1	11.7 ± 0.7	10.1 ± 1.5
Dissolved CH ₄ ($\mu\text{mol L}^{-1}$)	1.5 ± 0.3	0.8 ± 0.5	11.0 ± 14.0
AFDW (mg L ⁻¹)	7.7 ± 1.9	9.4 ± 2.7	18.7 ± 6.6
DOC (mg L ⁻¹)	4.7 ± 1.3	4.5 ± 0.7	9.6 ± 3.5
TOC (mg L ⁻¹)	3.9 ± 1.1	5.7 ± 1.0	20.6 ± 14.9
PO ₄ ³⁻ ($\mu\text{mol L}^{-1}$)	0.1 ± 0.0	0.3 ± 0.8	0.2 ± 0.2
NO ₃ ⁻ ($\mu\text{mol L}^{-1}$)	9.3 ± 5.9	1.7 ± 3.0	3.3 ± 3.7
NH ₄ ⁺ ($\mu\text{mol L}^{-1}$)	2.5 ± 0.8	1.9 ± 0.6	2.1 ± 0.6
Chla ($\mu\text{g L}^{-1}$)	42.5 ± 17.0	20.7 ± 3.4	45.5 ± 30.2
GPP (g O ₂ m ⁻² d ⁻¹)	20.7 ± 3.3	1.7 ± 0.1	4.5 ± 1.2
RE (g O ₂ m ⁻² d ⁻¹)	-18.0 ± 2.9	-2.0 ± 0.1	-5.9 ± 1.0
NEP (g O ₂ m ⁻² d ⁻¹)	2.7 ± 0.6	-0.3 ± 0.0	-1.4 ± 0.2

K_d (attenuation coefficient for photosynthetically active radiation); AFDW (ash free dry weight); DOC (dissolved organic carbon); TOC (total organic carbon); PO_4^{3-} (phosphate); NO_3^- (nitrate), NH_4^+ (ammonium); Chla (Chlorophyll a). All measurements correspond to subsurface samples (within the first 10cm of the water column).

2. Greenhouse gas (CH_4 and CO_2) dynamics

The pattern of dissolved CH_4 concentrations was similar between the ditch and the control treatment but differed for the FLAB treatment. From 28th of August onward, CH_4 concentrations in the FLAB treatment increased markedly and continued to rise until the end of the experiment, reaching a final mean value of $28.9 \pm 16.6 \mu M$, considerably higher than the final concentration in the ditch ($1.4 \pm 0.4 \mu M$) and in the control treatment ($1.7 \pm 0.3 \mu M$). The large standard deviation in CH_4 concentrations within the FLAB treatment reflects substantial variability among replicates, driven primarily by one of them (enclosure #8), which consistently exhibited lower CH_4 concentrations than the other FLAB replicates, but that remained higher than those in the control treatment and the ditch.

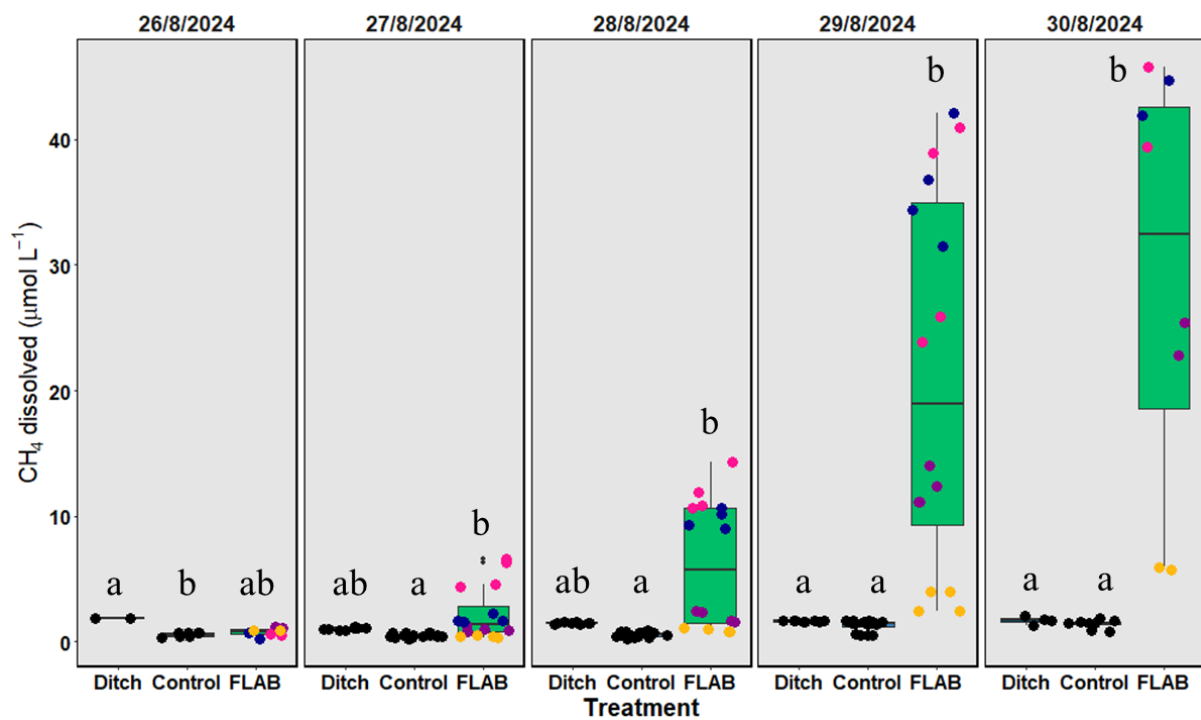


Figure 2. Methane (CH_4) dissolved concentration ($\mu mol L^{-1}$) in the ditch, the control treatment and the FLAB treatment. Panels indicate the sampling dates throughout the experimental period. Each point corresponds to the dissolved CH_4 concentration *per* sample and two samples were taken *per* replicate and *per* day, which was accounted for in the statistical analysis. All measurements were done during daytime. Different letters indicate statistically significant differences between treatments from the same date. Colours in the FLAB treatment indicate individual replicates: #1 (purple), #5 (pink), #6 (blue), and #8 (yellow).

Diffusive CH₄ emissions (Fig. 3) followed a similar pattern as CH₄ dissolved concentrations. For the ditch, data was collected on the 26th, 27th and 29th of August, with mean overall value for the whole experimental period of $0.1 \pm 0.2 \text{ mg m}^{-2} \text{ d}^{-1}$ (Fig. S9). The control treatment had higher CH₄ diffusive emissions than the ditch, ranging between 0.8 ± 0.3 and $4.1 \pm 1.5 \text{ mg m}^{-2} \text{ d}^{-1}$ at the beginning and the end of the experiment, respectively. The FLAB treatment exhibited a strong increase in CH₄ diffusive emissions through the experiment, with emissions starting at 3.5 ± 3.3 and ending at $78.4 \pm 44.5 \text{ mg m}^{-2} \text{ d}^{-1}$. The large standard deviation in the flux at the end of the experimental period reflects substantial variability among FLAB replicates, again driven primarily by replicate #8, which exhibited very low diffusive flux ($2.9 \pm 0.1 \text{ mg m}^{-2} \text{ d}^{-1}$) in comparison with the rest of the FLAB replicates ($97.3 \pm 14.1 \text{ mg m}^{-2} \text{ d}^{-1}$). The control and FLAB treatments exhibited daily K₆₀₀ CH₄ within the same range (Fig. S10), indicating that the differences in diffusive emissions are related to the treatment itself and not to differences in physical conditions. The lower CH₄ diffusive flux for the ditch in comparison to the control treatment despite their similar CH₄ dissolved concentrations (Fig. 2) could be related to lower K₆₀₀ CH₄ in the automatic chambers measurements (Fig. S10) as a result of lower turbulence due to their height and floating holders.

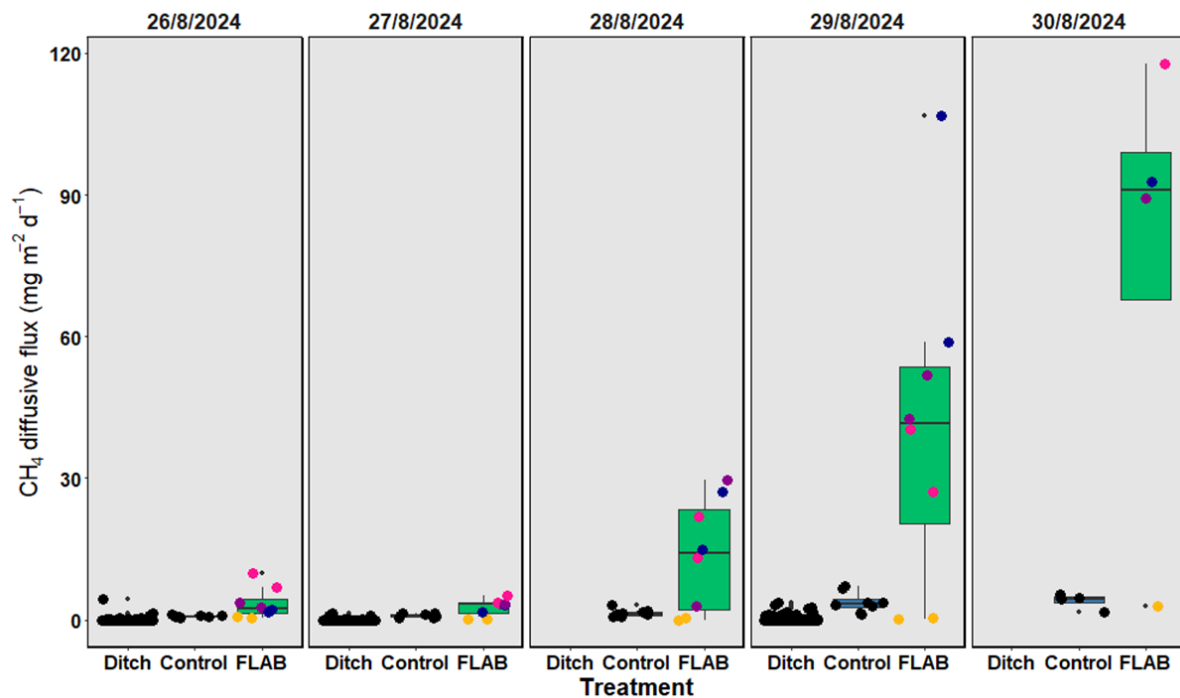


Figure 3. Methane (CH₄) diffusive flux ($\text{mg m}^{-2} \text{ d}^{-1}$) from the ditch, the control treatment and the treatment with FLAB. Panels indicate the sampling dates throughout the experimental period. Each data point from the control and FLAB treatment corresponds to a flux measured: between the 26th and the 29th two measurements were done *per day* and *per replicate* (morning and afternoon), whereas on the 30th one measurement was done *per replicate* (morning). All measurements were done during daytime. Each data point for the ditch corresponds to the

automatically measured diffusive fluxes in the morning and/or afternoon of that day. Colours in the FLAB treatment indicate individual replicates: #1 (purple), #5 (pink), #6 (blue), and #8 (yellow).

Carbon dioxide (CO₂) diffusive flux (Fig. S11) had a very different pattern depending on the treatment. The ditch had similar fluxes during the three dates that data could be collected, and the mean overall value indicates that it was almost in equilibrium with the atmosphere, or a slight source ($0.8 \pm 0.7 \text{ mg m}^{-2} \text{ d}^{-1}$) (Fig. S12). The control treatment started acting as a sink of CO₂ on the first day of the experimental period ($-83 \pm 76.6 \text{ mg m}^{-2} \text{ d}^{-1}$) but then shifted towards being a net source of CO₂, with a mean flux of $306.0 \pm 52.2 \text{ mg m}^{-2} \text{ d}^{-1}$ on the last day of the experiment. The FLAB treatment acted always as a substantial sink of CO₂, with an overall mean value of $-1358.1 \pm 417.5 \text{ mg m}^{-2} \text{ d}^{-1}$. It is important to highlight that all these measurements were carried out during daytime, but these patterns will change and might even be reversed during nighttime.

Ebullitive CH₄ emissions had also a different pattern depending on the treatment and the moment of the experimental period (Fig. 4). In the ditch, there was enough trapped gas volume to retrieve samples at three different time points (28th, 29th and 30th of August) and from all four bubble funnels each time. Both the control and FLAB treatments produced enough bubble volume to allow sampling on two dates (28th and 30th August). Nearly all control and FLAB funnels yielded sufficient volume for both collections, except for replicate #8 from FLAB treatment, which accumulated enough bubbles only by the final sampling date (30th August) and this single sample corresponded to the lowest CH₄ ebullitive emission observed in the FLAB treatment ($3.3 \text{ mg m}^{-2} \text{ d}^{-1}$). Ebullitive emissions from the ditch (45.5 ± 32.3 ; 120.7 ± 83.8 and $82.8 \pm 32.9 \text{ mg m}^{-2} \text{ d}^{-1}$ for the 28th, 29th and 30th, respectively) were of the same order of magnitude as those in the control treatment (33.8 ± 20.2 and $121.0 \pm 148.8 \text{ mg m}^{-2} \text{ d}^{-1}$ for the 28th and 30th, respectively) and as those from the FLAB treatment on the 28th August sample retrieval ($52.0 \pm 41.4 \text{ mg m}^{-2} \text{ d}^{-1}$) but emissions were higher for the FLAB treatment on the 30th August sample retrieval ($539.1 \pm 550.8 \text{ mg m}^{-2} \text{ d}^{-1}$). The first bubble collection in the FLAB treatment reflects emissions produced within the first 48hs of experiment (from 26th to 28th August) and it was comparable in magnitude to the ditch and control treatment. The last bubble collection represents emissions produced in the last 48hs (29th and 30th of August), which were an order of magnitude higher and exhibited substantial variation among replicates, mainly driven by the low ebullitive emissions from replicate #8, following the same pattern observed for CH₄ dissolved concentrations (Fig. 2) and CH₄ diffusive emissions (Fig. 3).

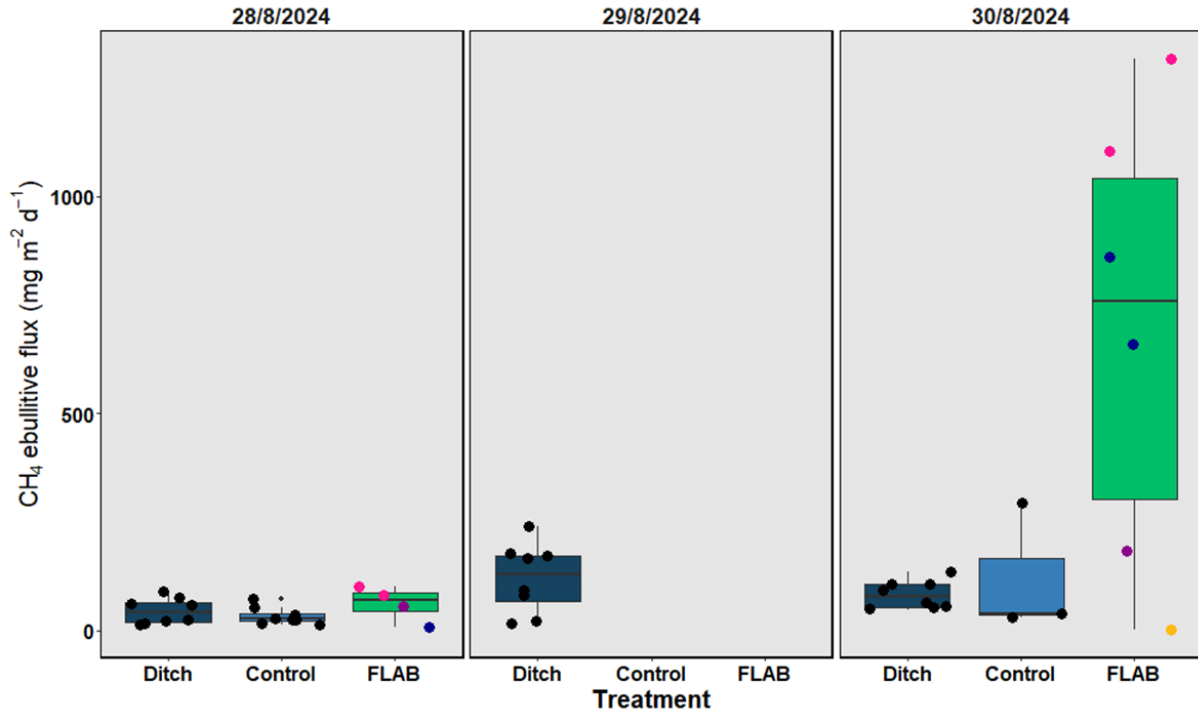


Figure 4. Methane (CH_4) ebullitive emissions ($\text{mg m}^{-2} \text{d}^{-1}$) from the ditch (dark blue), the control treatment (light blue) and the treatment with FLAB (green). Panels indicate the dates where there was enough gas collected to retrieve samples. In the ditch, samples could be retrieved from the four bubble funnels in three different time points (28th, 29th and 30th August), whereas in the control and FLAB treatments there was enough gas accumulated to retrieve samples in two different time points (28th and 30th August). On the 28th samples could be retrieved from three of the four FLAB replicates (not enough sample in replicate #8), but from all four control replicates. On the 30th samples could be collected from the four FLAB replicates, but from three of the four control replicates (not enough sample in replicate #2). Colours in the FLAB treatment indicate individual replicates: #1 (purple), #5 (pink), #6 (blue), and #8 (yellow).

CH_4 and CO_2 diffusive emissions alongside CH_4 ebullitive emissions were converted to CO_2 equivalents for the ditch, the control and the FLAB treatment, separately, following the considerations indicated in section 5.4 (Fig. 5). In all cases, the systems acted as net sources and the highest share corresponded to CH_4 ebullitive emissions. The ditch ($2.0 \pm 1.0 \text{ g CO}_{2\text{eq}} \text{ m}^{-2} \text{ d}^{-1}$) and the control treatment ($1.8 \pm 1.8 \text{ g CO}_{2\text{eq}} \text{ m}^{-2} \text{ d}^{-1}$) yielded overall similar mean CO_2 equivalent emissions. In contrast, the treatment with FLAB yielded considerably higher and much more variable mean CO_2 equivalent emissions ($8.2 \pm 8.0 \text{ g CO}_{2\text{eq}} \text{ m}^{-2} \text{ d}^{-1}$). This high variation is related to the variability among FLAB replicates, driven mostly by one of the four replicates (#8). Only for the CH_4 ebullitive pathway from the FLAB treatment a consideration of potential CH_4 bubble retention between 10% and 40% below the FLAB mat was applied, obtaining a new median value in each case (Fig. 5). If there was no bubble retention at all, the median value would be $6.7 \text{ g CO}_{2\text{eq}} \text{ m}^{-2} \text{ d}^{-1}$ (black line), whereas with a 40% retention (more probable at the beginning of the experimental time) the new median would be $4.2 \text{ g CO}_{2\text{eq}} \text{ m}^{-2} \text{ d}^{-1}$ (red dashed line) and with

a 10% retention (more probable at the end of the experimental time) the median would be $6.3 \text{ g CO}_{2\text{eq}} \text{ m}^{-2} \text{ d}^{-1}$ (yellow dashed line).

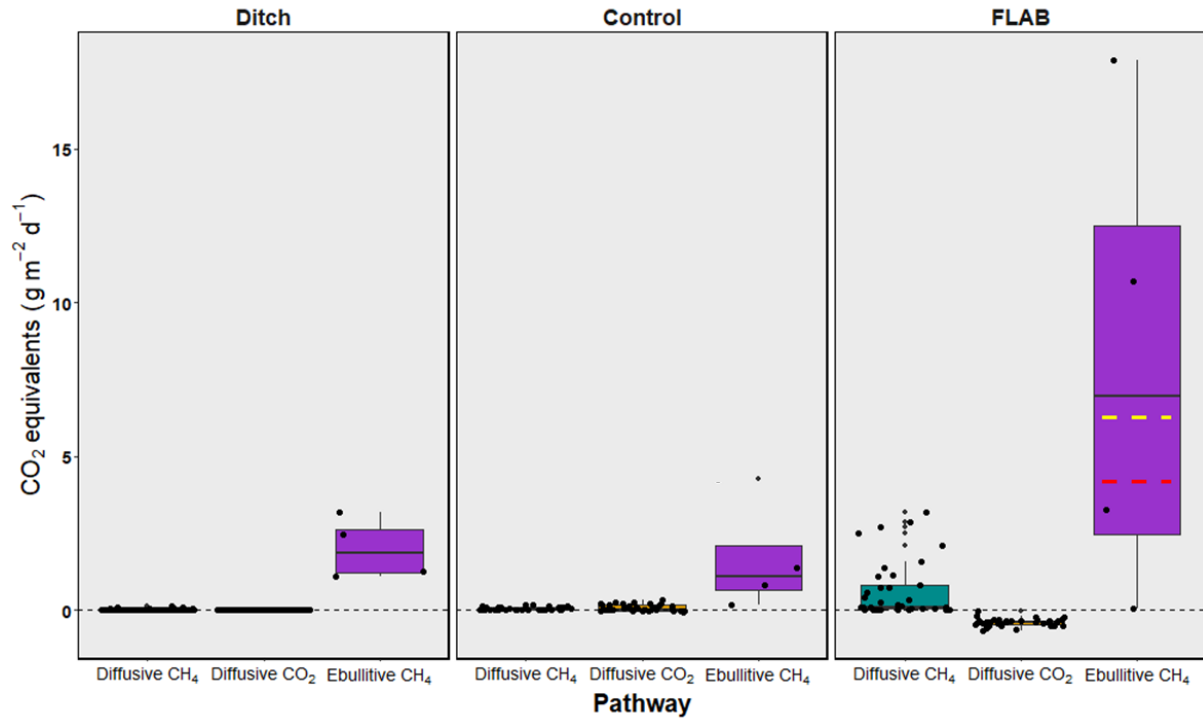


Figure 5. CO₂ equivalent emissions (g CO_{2eq} m⁻² d⁻¹). Each panel corresponds to a different treatment (ditch, Control or FLAB treatment) and the different boxes relate to the different emissions pathways: CH₄ and CO₂ diffusive fluxes and CH₄ ebullitive emissions. In the FLAB panel, the red and yellow lines depicted on top of the ebullitive pathway boxplot correspond to the median associated with a 10% or 40% retention of ebullitive flux, correspondingly, due to the potential effect of FLAB on bubble retention.

3. Modelling CH₄ concentrations in the enclosures

Below, the results obtained for each component of the mass balance (equation 14) and the overall results are addressed separately.

3.1. *Sed*: sediment CH₄ production

Sediment CH₄ fluxes obtained from sediment cores averaged $0.5 \pm 0.4 \text{ nmol CH}_4 \text{ g wet weight sediment}^{-1} \text{ h}^{-1}$ (range: 0.04 ± 0.00 to $1.4 \pm 0.0 \text{ nmol CH}_4 \text{ g wet weight sediment}^{-1} \text{ h}^{-1}$; Table S2) and were comparable between August ($0.4 \pm 0.2 \text{ nmol CH}_4 \text{ g wet weight sediment}^{-1} \text{ h}^{-1}$) and October ($0.5 \pm 0.5 \text{ nmol CH}_4 \text{ g wet weight sediment}^{-1} \text{ h}^{-1}$); therefore, all measurements were pooled to model sediment CH₄ production.

The mean sediment CH₄ production rates were of 0.64 ± 0.11 ; 0.47 ± 0.03 and $0.57 \pm 0.04 \text{ nmol CH}_4 \text{ gr wet weight sediment}^{-1} \text{ h}^{-1}$ for the ditch, the control and the FLAB treatment, respectively, indicating no clear differences among them. Conversely, the mean sediment CH₄ oxidation rates were of 1.96 ± 0.00 , 1.88 ± 0.00 and $0.86 \pm 0.02 \text{ nmol CH}_4 \text{ gr wet weight sediment}^{-1} \text{ h}^{-1}$ for the ditch, the control and the FLAB treatment, respectively, where the

ditch and control treatment had a similar pattern whereas the FLAB treatment had a lower sediment CH₄ oxidation rate.

The mean sediment CH₄ production rates obtained from the two methods were consistent, indicating that both approaches are suitable. However, the laboratory incubations may overestimate CH₄ production and oxidation rates because the controlled conditions are optimized to favour each process. In contrast, the sediment core measurements capture a broader (and likely more realistic) range of potential *in-situ* CH₄ production. For this reason, we selected the mean, minimum, and maximum values derived from the August and October core measurements and used them as three potential scenarios of sediment CH₄ production in the model.

3.2. *MOX*: methane oxidation rates in the water

Up to 60h of incubation, both light and dark treatments had a similar pattern and no significant changes in dissolved CH₄ were detected. After this threshold, CH₄ concentration decreased in both treatments, fastest in the dark treatment (Fig. S13). This time frame after 60h was used to estimate the *MOX* rate of each treatment, as the slope from the regression between the dissolved CH₄ ($\mu\text{mol L}^{-1}$) and time (day), obtaining a rate of $-1.3 \mu\text{mol L}^{-1} \text{d}^{-1}$ and $-5.3 \mu\text{mol L}^{-1} \text{d}^{-1}$ for the light and dark treatment, respectively. Given that these rates represent either a scenario with constant light or with constant darkness, a third scenario that would include both situations was obtained as the mean rate of these two ($-3.3 \mu\text{mol L}^{-1} \text{d}^{-1}$). These three rates were used as three different potential scenarios for *MOX* in the mass balance.

3.3. *FLAB*: floating algae bed effects on dissolved CH₄

We did not observe substantial CH₄ production in the FLAB treatments, evidenced by a similar pattern of CH₄ dissolved concentrations between FLAB and control (Fig. S14). Although from these results it cannot be concluded that FLAB is not producing CH₄ (the rate of production could be low, and therefore not captured in the resolution of this incubation experiment), for the particular modelling exercise of this manuscript it is considered that direct production of CH₄ by FLAB is negligible.

The indirect effect of FLAB on *MOX* rates was considered by correcting the water *MOX* rates (section 9.2) for the O₂ and CH₄ concentrations below the mat, at each time point. Therefore, if the algae mat affected the concentration of O₂ and CH₄, this is reflected in the model with the corresponding changes in *MOX* rate.

The FLAB effect was further modelled, therefore, as an extra sediment CH₄ production due to labile organic carbon input to the sediments. For this, the input rate of OC (I , g day^{-1}) of each replicate from the FLAB treatment was obtained as the difference between the final and initial FLAB dry carbon weight (44.8% of dry weight) divided by the last 48h of experiment, which is when the CH₄ emissions spiked (Fig. 2, 3 and 4). Values of I ranged

between 26 and 45 g day⁻¹ (Table S3). The rest of the parameters used to model FLAB decomposition are specified in Table 1 and Table S3.

3.4. Model selection

The normalized root mean square error (NRMSE) of the final model for the FLAB treatment ranged from 26% to 45%, indicating a moderate prediction error relative to the mean observed values and suggesting that the model captured the main patterns in the data reasonably well. For the control treatment, NRMSE values ranged from 27% to 67%, reflecting a larger relative prediction error. However, this higher error was expected given the low CH₄ concentrations in the controls, where small absolute deviations translate into large relative errors. Nevertheless, predicted values ($\pm$ error) remained within the range of observed concentrations.

The parameters setting resulting in the best model fits depended on the treatment and on the replicate, indicating a considerable spatial variability. The model that best described the increase in water column CH₄ concentrations in the FLAB enclosures #5 and #6 was based on the mean sediment production scenario and the mean MOX scenario; for FLAB enclosures #1 and #8 it was based on the low sediment production scenario combined with the mean and low MOX scenarios, respectively.

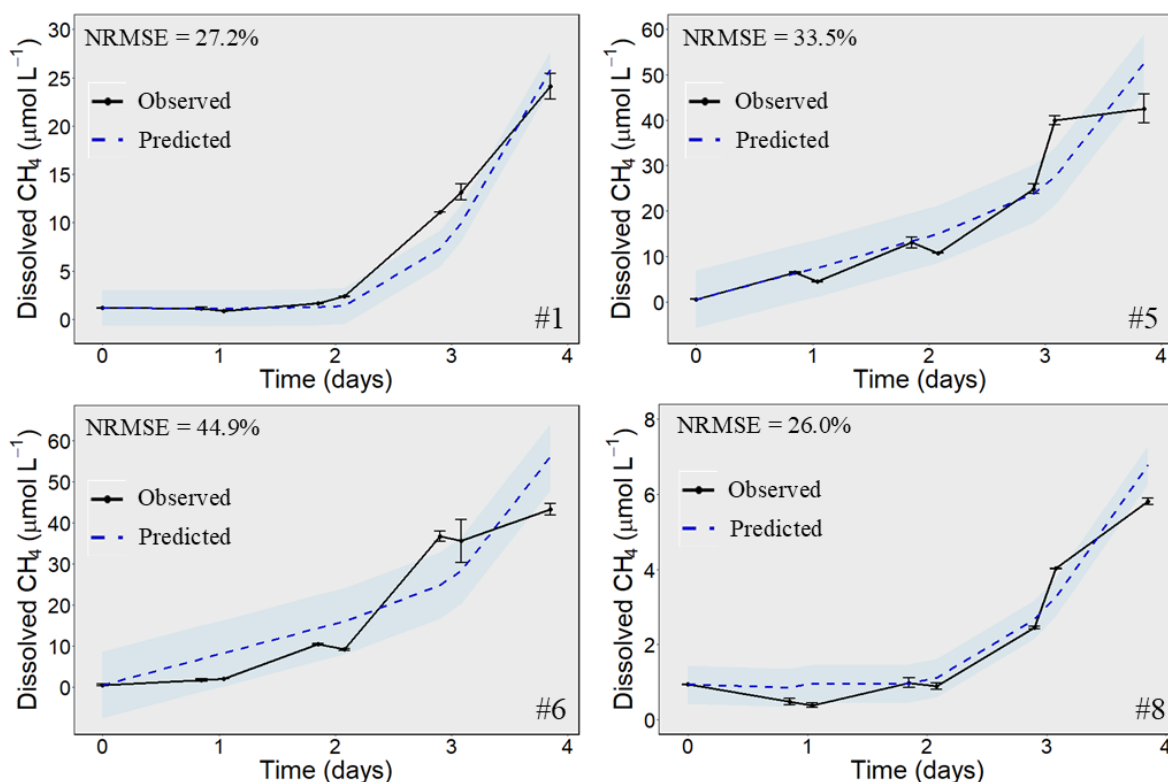


Figure 6. Modelled (blue) versus observed (black) CH₄ concentrations in each one of the four replicates of the FLAB treatment. The shaded area around the blue curve corresponds to the standard deviation of the residuals from the model. The points and error bars of the black curve correspond to the measured time points and their standard error bars.

Discussion

FLAB had a strong indirect effect on CH₄ dynamics, evidenced by higher dissolved CH₄ concentrations and substantially increased diffusive and ebullitive CH₄ emissions in the presence of floating algae, consistent with previous studies (Liang and others 2016; Grasset and others 2018). On average, CH₄ diffusive emissions were 12-fold higher and CH₄ ebullitive emissions were on average 5-fold higher in the presence of FLAB than in the control despite considerable variability among FLAB replicates. In contrast, FLAB acted as a strong daytime sink for CO₂ due to high photosynthetic activity. Although nighttime CO₂ fluxes were not measured directly, available evidence indicates that CO₂ uptake by floating primary producers during the day is often offset by nighttime respiration (Peixoto et al. 2016). Accounting for this effect did not alter the overall conclusion that FLAB substantially increased the carbon GHG total emissions of the system. The combined effects of enhanced CH₄ emissions and altered CO₂ dynamics resulted in a marked increase in CO₂-equivalent emissions in the presence of FLAB, with the overall GHG emissions being on average 4.5 times higher than that of the control, highlighting that FLAB blooms - likely to increase with nutrient enrichment and warming – play a major role in regulating carbon greenhouse gas emissions from freshwater ecosystems.

The magnitude of FLAB-induced increases in CH₄ diffusive and ebullitive emissions varied substantially among replicates, reflecting fine-scale spatial heterogeneity in sediment and water column conditions. Such variability is common in shallow freshwater systems, where differences in sediment organic matter content, redox status, and microbial activity can strongly influence baseline CH₄ production potential and the degree to which FLAB modifies local biogeochemical processes. In our experiment, replicates that developed anoxic conditions beneath the FLAB mat exhibited the largest increases in diffusive and ebullitive CH₄ emissions, consistent with the reported enhancement of methanogenesis under oxygen-depleted conditions beneath floating vegetation mats (King 1990; Kosten and others 2016). Conversely, the replicate that remained comparatively oxygenated throughout the experiment showed markedly lower dissolved CH₄ concentrations and weaker FLAB effects on both CH₄ diffusive and ebullitive fluxes. Given that all replicates received similar amount and type of FLAB, these patterns suggest that FLAB impacts on CH₄ dynamics are mediated not only by the biomass or coverage of the floating mat but also by differences in sediment properties and associated metabolic activity. Because the replicates were separated by only ~10 m in total, the observed variability underscores how small-scale heterogeneity in sediment characteristics and water–sediment interactions can modulate the strength of FLAB-driven alterations to ecosystem metabolism and GHG emissions.

The presence of FLAB also altered key physical, chemical, and biological characteristics of the ecosystem, particularly by increasing organic matter availability and reducing light and oxygen in the water column. Ash-free dry weight, DOC, TOC and turbidity in the water column were all higher in the presence of FLAB compared with both the control treatment and the ditch, consistent with previous observations of increased DOC following algal amendments (Liang and others 2016). These patterns likely arise because FLAB mats persist at the water surface while fragments remain suspended or settle, allowing them to influence the entire water column. Concomitantly, dissolved O₂ concentrations and PAR decreased under the FLAB mat, in line with findings by Pikosz and others 2017, resulting in a shift in the water column metabolism toward more heterotrophic conditions underneath the FLAB. This metabolic change is driven by shading and reduced O₂ availability beneath the floating mat, which diminishes autotrophic production, as also reported by other studies (Blindow and others 2006; Page and others 2022).

The thickness and density of the FLAB layer are key determinants of their ecological impact, with higher biomass generally associated with stronger negative effects on ecosystem functioning (Green and Fong 2016). At the start of the experiment, the wet floating biomass of FLAB averaged 20.6 ± 0.5 kg WW m⁻², decreasing to 4.5 ± 1.1 kg WW m⁻² by the end of the experiment. Because the mesocosms were laterally enclosed, the biomass lost from the floating mat remained within the system, either accumulating in the water column or settling to the sediments, where it contributed to organic matter decomposition. The thickness and biomass of FLAB used in this study is comparable to that used in previous studies (Green and Fong 2016; Liang and others 2016), and resemble a natural FLAB bloom transitioning from a bloom into its decay phase, with metabolically active surface layers overlying decomposing biomass. Indeed, despite the observed decline in the mat biomass over time, all FLAB treatments remained daytime CO₂ sinks throughout the experiment (Fig. S11), indicating that active photosynthetic uptake and decomposition processes occurred simultaneously throughout the experiment.

To identify the potential mechanisms driving changes in CH₄ emissions in the presence of FLAB, a multiple approach effect was considered, including 1) potential CH₄ production directly by FLAB; 2) indirect effects on MOX rates through changes in O₂ and CH₄ dissolved below the mat; and 3) potential CH₄ production through FLAB decomposition in the sediments. There was no evidence of CH₄ production by FLAB from the laboratory incubations. Previous studies have shown that phytoplankton can produce CH₄ and rates are typically low (Klitzsch and others 2019; Bižić and others 2020; Balaña and others 2025). If FLAB were producing CH₄ at rates comparable to those reported in the studies cited above ($\sim 0.01\text{--}0.2$ μmol CH₄ g⁻¹ Chl-a h⁻¹) this would translate into diffusive CH₄ fluxes around $1.8 \cdot 10^{-4}$ and $3.5 \cdot 10^{-3}$ mg m⁻² d⁻¹ (considering the mean Chla concentration in the

FLAB treatment: $45.5 \pm 30.2 \mu\text{g L}^{-1}$, the mean enclosure volume and surface area). These rates represent less than 5% of the mean diffusive CH_4 emissions measured in the FLAB treatment, so they would not have contributed substantially to measured emissions. Regarding the indirect effect of FLAB on MOX, overall floating mats increased CH_4 and decreased O_2 concentrations beneath the mat. These changes were incorporated into the MOX calculations using a dual-substrate Monod model (Segers 1998; Guérin and Abril 2007; Martinez-Cruz and others 2015), which assumes that MOX increases with the availability of both CH_4 and O_2 . Because CH_4 and O_2 were inversely related below the algae mats in our experiment, this approach may have underestimated MOX rates. Previous studies suggest that while Monod kinetics adequately describe CH_4 dependence, MOX dependence on O_2 is more complex (Rudd and others 1974; Rudd 1976) and may instead peak at high CH_4 and low O_2 concentrations (approximately 0.5 mg L^{-1}) (Thottathil and others 2019). If this relationship also applies to our system, MOX rates during the final 48 h of the experiment may have been underestimated, resulting in a conservative estimate of the indirect effect of FLAB on CH_4 dynamics. Consequently, the actual impact of FLAB on CH_4 cycling may have been greater than indicated by our MOX-corrected estimates. Nevertheless, we consider our approach appropriate because it avoids overestimating MOX activity under low-oxygen conditions.

Finally, the potential increase in CH_4 production associated with the decomposition of algal-derived organic carbon was estimated by combining parameters from our experiments and values from literature. Although such estimates are inherently uncertain, the close agreement between observed and modelled CH_4 concentrations supports the conclusion that sediment CH_4 production increased in the FLAB treatment because of enhanced decomposition of algal-derived organic matter. It is important to note that CH_4 buildup beneath FLAB likely reflects a combination of increased diffusive and ebullitive inputs (where the latter would lead to CH_4 bubble dissolution beneath the mat) which cannot be disentangled with the current dataset. Resolving these contributions would require measurements of bubble retention beneath FLAB and how trapping efficiency varies with mat thickness, as both processes are likely to play a key role in regulating FLAB-induced CH_4 emissions.

In nature, FLAB may occur as scattered patches coexisting or not with submerged macrophytes, or as dense surface blooms (Pikosz and Messyasz 2015), and these spatial differences are likely to have different effects on the total carbon emissions of the ecosystem. We emphasize that the magnitude and direction of FLAB effects depend on their spatial distribution, biomass, and interactions within the FLAB–water column–sediment continuum, which together determine the ecological conditions that develop beneath the mat. As reflected by the variability among our replicates, the effects of well-developed FLAB blooms on CH_4 dynamics can vary considerably. We attribute this variability to the extent to which the mat alters O_2 availability, as well as on intrinsic

sediment characteristics and broader climatic and limnological conditions. Consequently, the influence of FLAB on CH₄ cycling is complex, spatially heterogeneous, and temporally variable. Nonetheless, our results indicate that dense FLAB mats can substantially alter the ecological functioning and biogeochemical properties of shallow freshwater ecosystems. Our findings further support the use of FLAB as indicators of deteriorating water quality (Whitton 1984; Philips 1990; European Commission 2014; Gladyshev and Gubelit 2019), as their presence may also increase ecosystem-scale greenhouse gas emissions. As climate change is expected to promote warmer and drier conditions that favour FLAB development, positive feedback between FLAB proliferation and CH₄ emissions may emerge. This highlights the need for a better understanding of the environmental factors controlling FLAB development and persistence in freshwater systems.

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Supplementary information for:

Floating algal beds and methane dynamics: a potential positive feedback loop

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- Figure S15: Modelled (blue) versus observed (black) CH₄ concentrations in each one of the four replicates of the control treatment.



Figure S1. FLAB in Dutch drainage ditches in spring and summer in a) the province of Gelderland and b) of North Brabant, in the Netherlands.

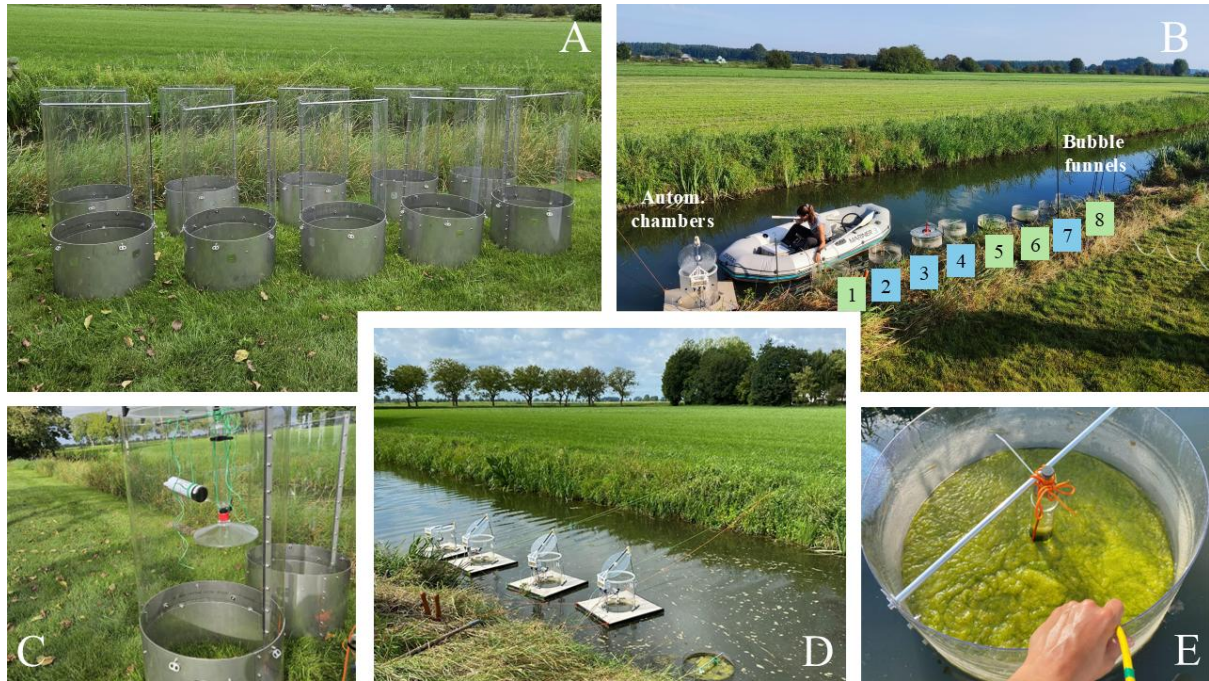


Figure S2. Set-up of field experiments. A) Enclosures just before deployment, made of transparent polycarbonate and including a stainless-steel rim in the bottom; B) General set-up of the field experiments. From upstream (i.e. upper part of the picture) to downstream: four bubble traps, the eight enclosures and the four automatic chambers. The numbers denote the eight replicates, numbers in green correspond to FLAB treatment whereas number in blue correspond to the control; C) Representation of how the high frequency sensor (miniDOT[®]) and the bubble trap were placed inside of the enclosures (NOTE: the miniDOT was not placed in every enclosure, it was placed in two treatment and two control enclosures randomly selected, and another one was placed in the ditch, between the automatic chambers and the first enclosure); D) Set-up of automatic chambers, downstream the enclosures. It can be noted in the picture that one of the chambers is closed (meaning that the total CH₄ and CO₂ flux from that chamber is being measured), while the rest of the chambers are open; E) Example of an enclosure with FLAB (treatment).

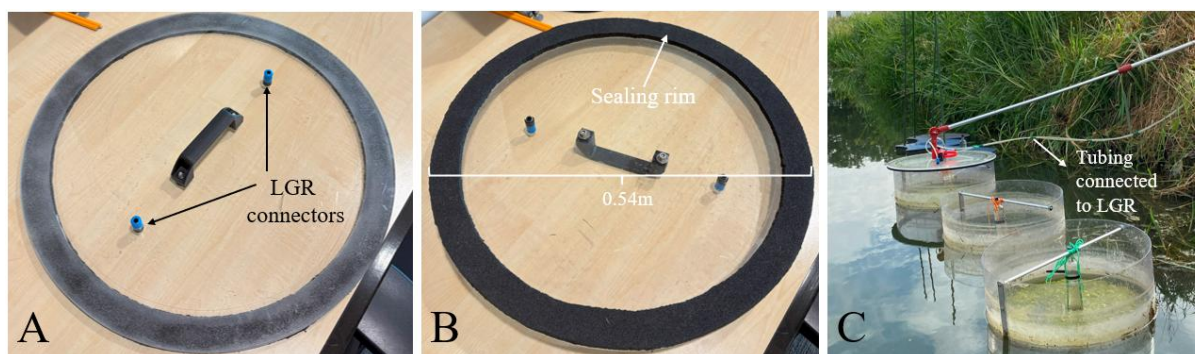


Figure S3. Lid placed on top of the enclosures to measure CH_4 and CO_2 diffusive emissions. A) Front view of the lid. LGR connectors are indicated, the tubing was connected to these ends and then to the LGR, creating a closed loop; B) Back view of the lid, where the sealing rim is in the outer section; C) Picture depicting how the lid was placed on top of the enclosures in the field.

Supplementary Information 1: Gas exchange velocity calculations

Gas exchange velocities (K) were calculated based on the obtained gas fluxes and the corresponding CH₄ concentrations in the water following equation S1 (Prairie and del Giorgio 2013; DelSontro and others 2016)

$$K = \frac{Flux\ gas}{Kh * \Delta p_{Gas}} \quad \text{equation S1}$$

Where Flux gas is the diffusive flux for CH₄ (mmol m⁻² d⁻¹), Kh is the Henry's constant correspondent corrected for atmospheric pressure and water temperature, and Δp_{Gas} is the difference between the partial pressure of the gas in the water (P_w) and the partial pressure of the gas in equilibrium with the atmosphere (P_{eq}), i.e. Δp_{Gas} (ppmv) = P_w - P_{eq}.

The obtained values of K were standardized to a Schmidt number of 600 (equation S2), obtaining the standardized K₆₀₀.

$$K_{600} = \frac{K_{CH_4}}{(SC_{CH_4}/600)^{-n}} \quad \text{equation S2}$$

Where Sc is the Schmidt number of a given gas at a given temperature (Wanninkhof 1992), and n is a value that depends on wind speed. A value of n = 2/3 was used for ambient wind speeds <3.7 m s⁻¹ and of n = 1/2 for ambient wind speeds >3.7 m s⁻¹ (Guérin and others 2007). Wind speeds were measured using a wind anemometer (Kestrel ®).

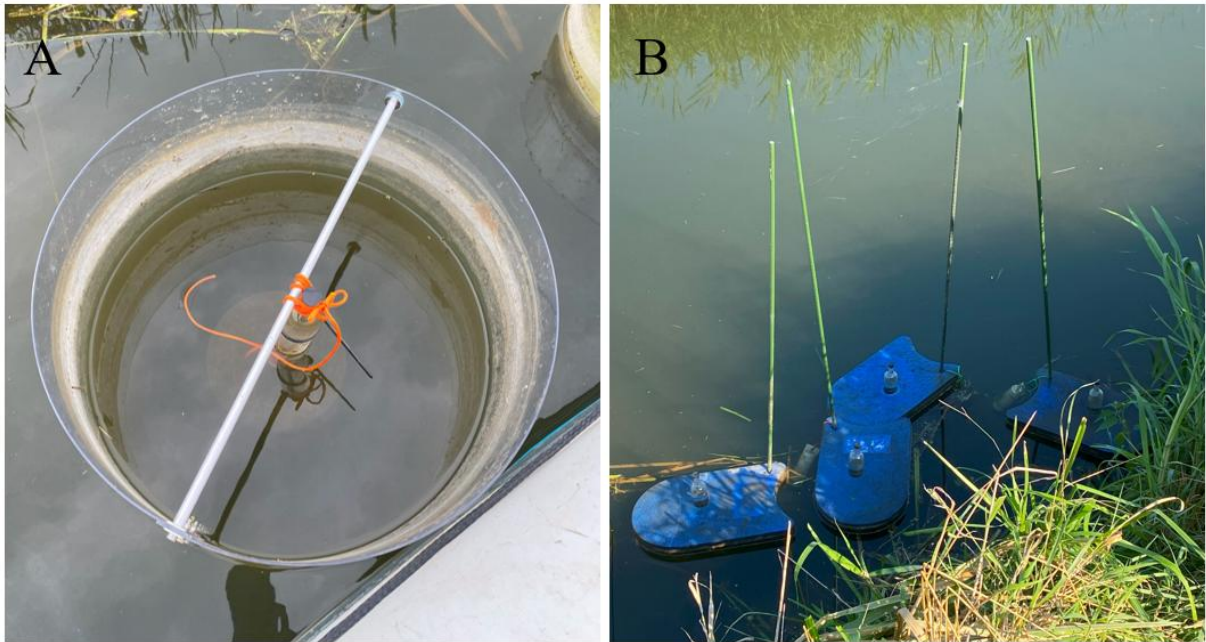


Figure S4. Pictures depicting A) how the CH₄ bubble funnels were placed in the enclosures and B) how the CH₄ bubble funnels were placed in the ditch, these last ones located upstream the enclosures.

Supplementary information 2: Assessment of water level change in the enclosures

Daily measurements of headspace height (cm) were used to calculate the change in headspace between consecutive days for each replicate. An increase in headspace indicated a loss of water from the enclosure to the ditch, whereas a decrease indicated water intrusion from the ditch into the enclosure. Using the daily headspace change (m) and the enclosure surface area (0.2 m²), the corresponding volume change (L) was calculated and expressed as a percentage of the total enclosure volume (196.3 L). The mean absolute daily volume change across all enclosures was $4.0 \pm 3.5\%$, ranging from 0.8% to 12.8%. Lateral water exchange was considered negligible and therefore not included in the mass balance.

Table S1. Percentage (%) of water either lost (negative) or gained (positive) in the enclosures, between consecutive days from the experimental period. There is no data from 26/8/24 to 27/8/24 because no changes were registered between these days.

<i>Treatment</i>	<i>Replicate</i>	<i>Dates</i>	<i>% of volume water either lost (negative) or gained (positive) in each replicate</i>
FLAB	#1	27/8/24 to 28/8/24	-11.3
		28/8/24 to 29/8/24	3.5
		29/8/24 to 30/8/24	2.0
	#5	27/8/24 to 28/8/24	-4
		28/8/24 to 29/8/24	-1.1
		29/8/24 to 30/8/24	-1.0
	#6	27/8/24 to 28/8/24	-4.6
		28/8/24 to 29/8/24	-2.2
		29/8/24 to 30/8/24	-1.0
	#8	27/8/24 to 28/8/24	5.3
		28/8/24 to 29/8/24	3.5
		29/8/24 to 30/8/24	-0.5
CONTROL	#2	27/8/24 to 28/8/24	-12.1
		28/8/24 to 29/8/24	3.5
		29/8/24 to 30/8/24	1.8
	#3	27/8/24 to 28/8/24	-12.8
		28/8/24 to 29/8/24	3.3
		29/8/24 to 30/8/24	2.4
	#4	27/8/24 to 28/8/24	-7.9
		28/8/24 to 29/8/24	-1.7
		29/8/24 to 30/8/24	1.5
	#7	27/8/24 to 28/8/24	-4.6
		28/8/24 to 29/8/24	-2.2
		29/8/24 to 30/8/24	-1.0

The tones of green correspond to replicates from the FLAB treatment, whereas the tones of blue correspond to the control treatment. The different tones in each case just provide clarity to easily identify the replicates, they do not imply any difference between them.

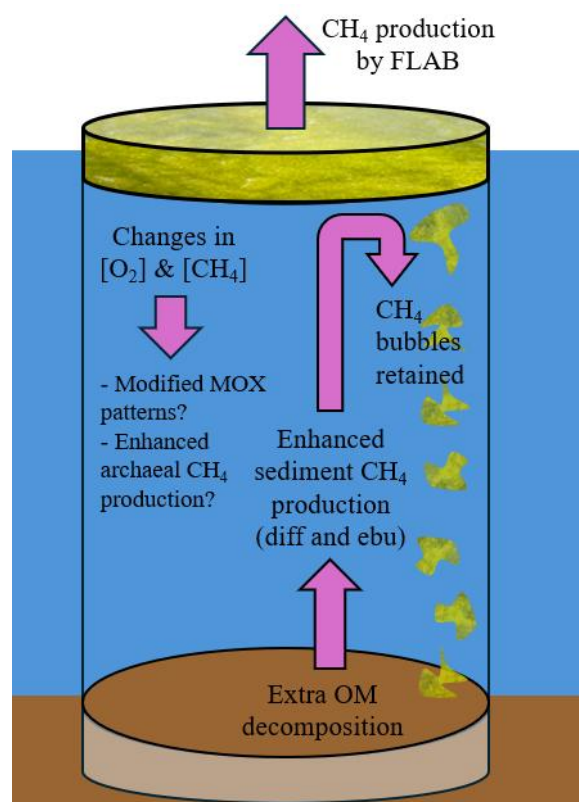


Figure S5. Schematic figure indicating the potential effects of FLAB on methane (CH₄) dynamics: FLAB could produce CH₄ directly; FLAB that sinks to the bottom can fuel extra organic matter (OM) decomposition, enhancing sediment CH₄ production, both by diffusion and/or ebullition; part of the CH₄ bubbles produced can be retained below the algae mat, increasing CH₄ dissolved concentrations below the FLAB; the algae mat can change (oxygen) O₂ and CH₄ concentration below the mat, modifying methane oxidation (MOX) patterns and/or enhancing CH₄ production by a reduction of O₂ concentrations.

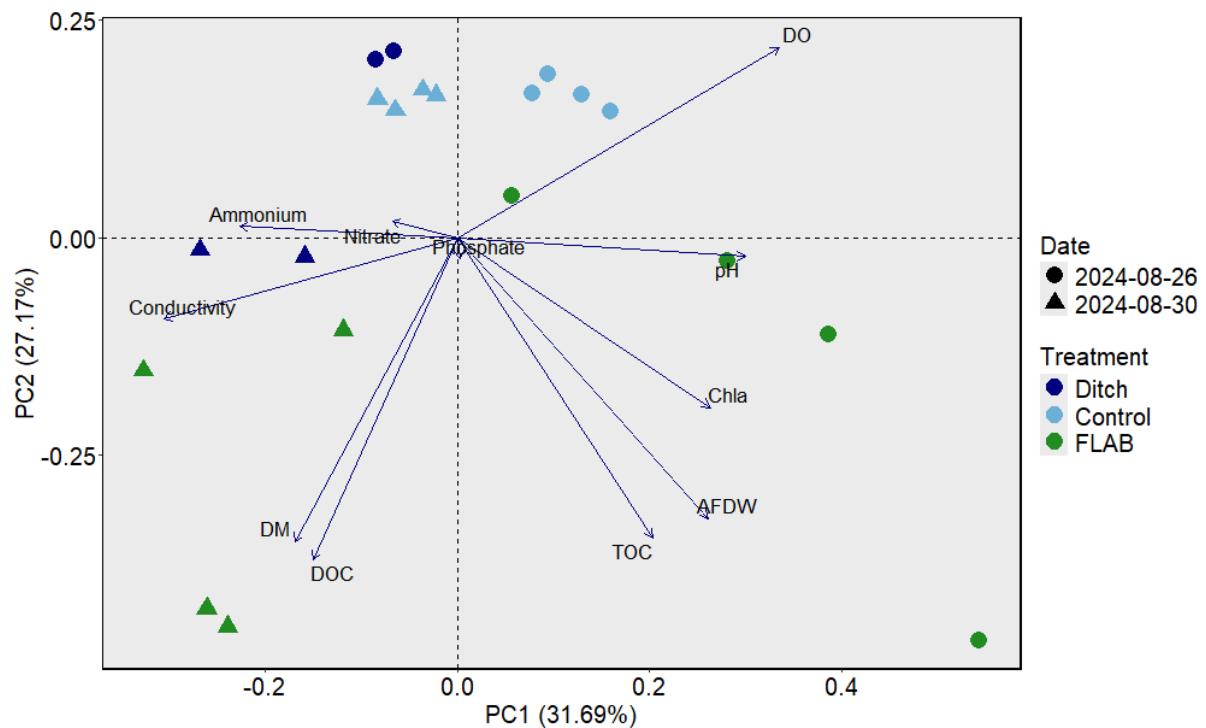


Figure S6. Biplot of principal component analysis (PCA) including data from the ditch (dark blue), from the control (light blue) and from the FLAB (green) replicates, for the onset (circles) and end (triangles) of the experimental period. The environmental variables are pH, conductivity, dissolved oxygen (DO), ammonium, phosphate, nitrate, chlorophyll a (Chla), dissolved methane (DM), dissolved organic carbon (DOC), total organic carbon (TOC), ash free dry weight (AFDW). The first principal component axis (PC1) explained 31.7% of the variation and the main variables were DO (loading = 0.44) and conductivity (loading = -0.40), which were particularly high at the onset and end of the experiment, respectively. The second principal component axis (PC2) explained 27.2% of the variation and the main variables were DOC (loading = -0.49), DM (loading = -0.46), TOC (loading = -0.45) and AFDW (loading = -0.42), all of them higher in the FLAB treatment at the end of the experiment.

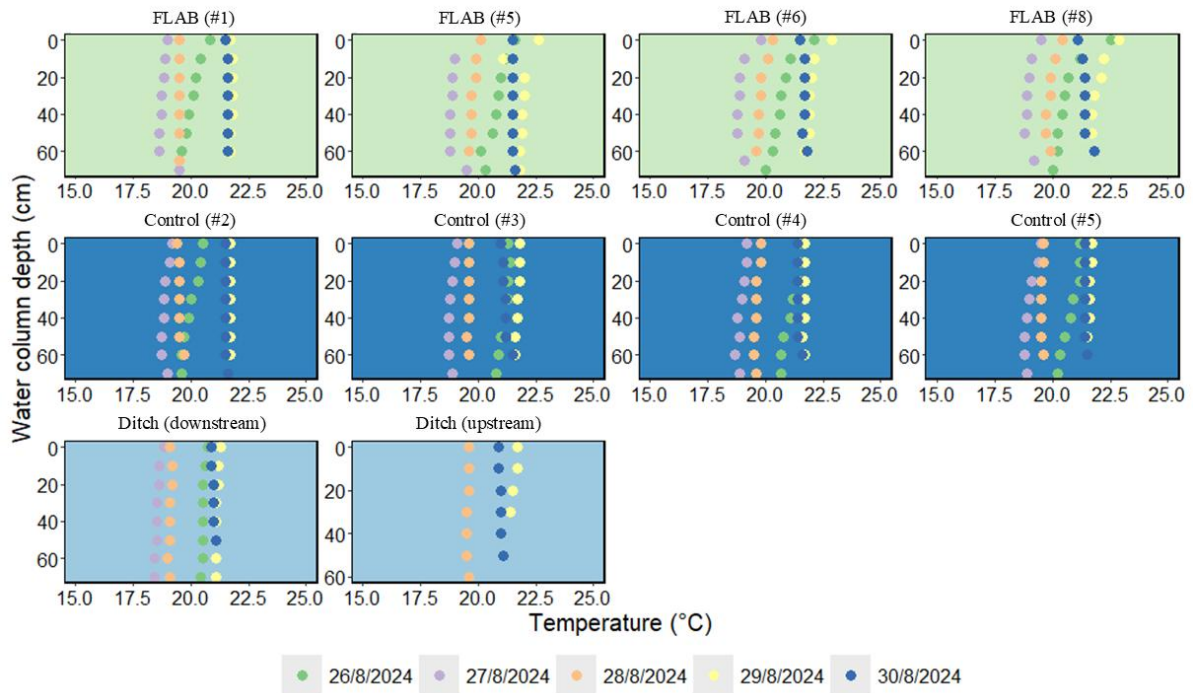


Figure S7. Daily temperature ($^{\circ}\text{C}$) profiles carried out in the ditch (light blue), the enclosures control (dark blue) and the enclosures with FLAB (green). Each day is represented by dots with different colours. The daily profiles were carried out always in the morning, between 9am and 12hs.

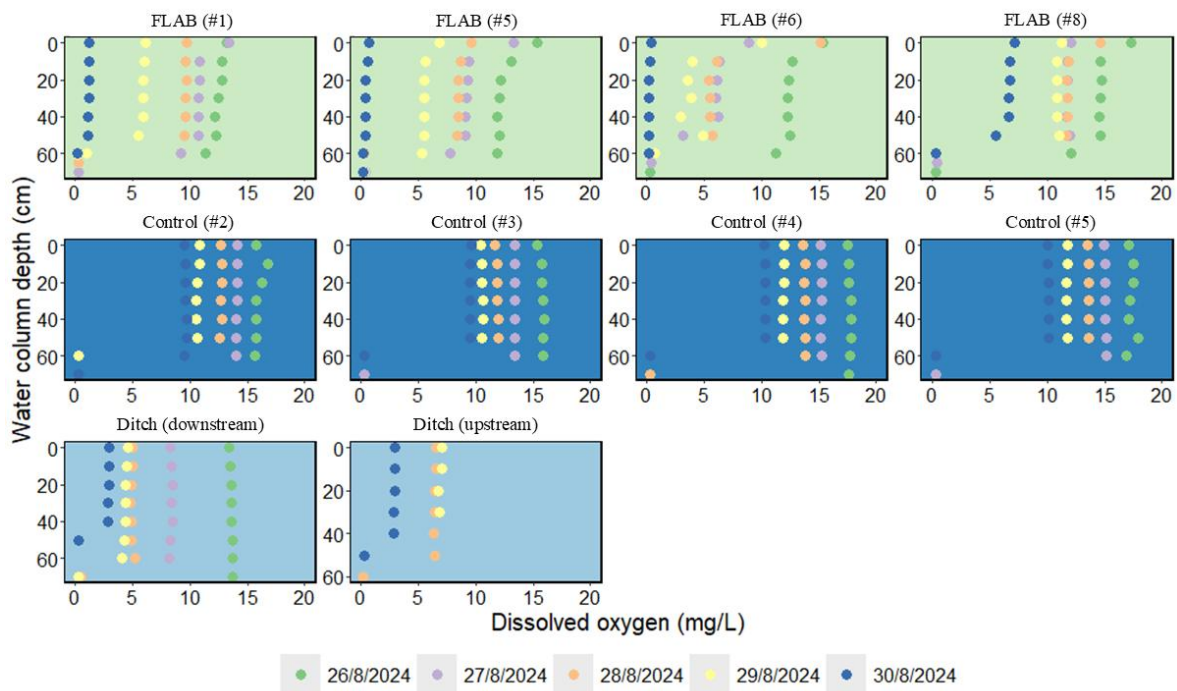


Figure S8. Daily dissolved oxygen (mg L^{-1}) profiles carried out in the ditch (light blue), the enclosures control (dark blue) and the enclosures with FLAB (green). Each day is represented by dots with different colours. The daily profiles were carried out between 9am and 12hs.

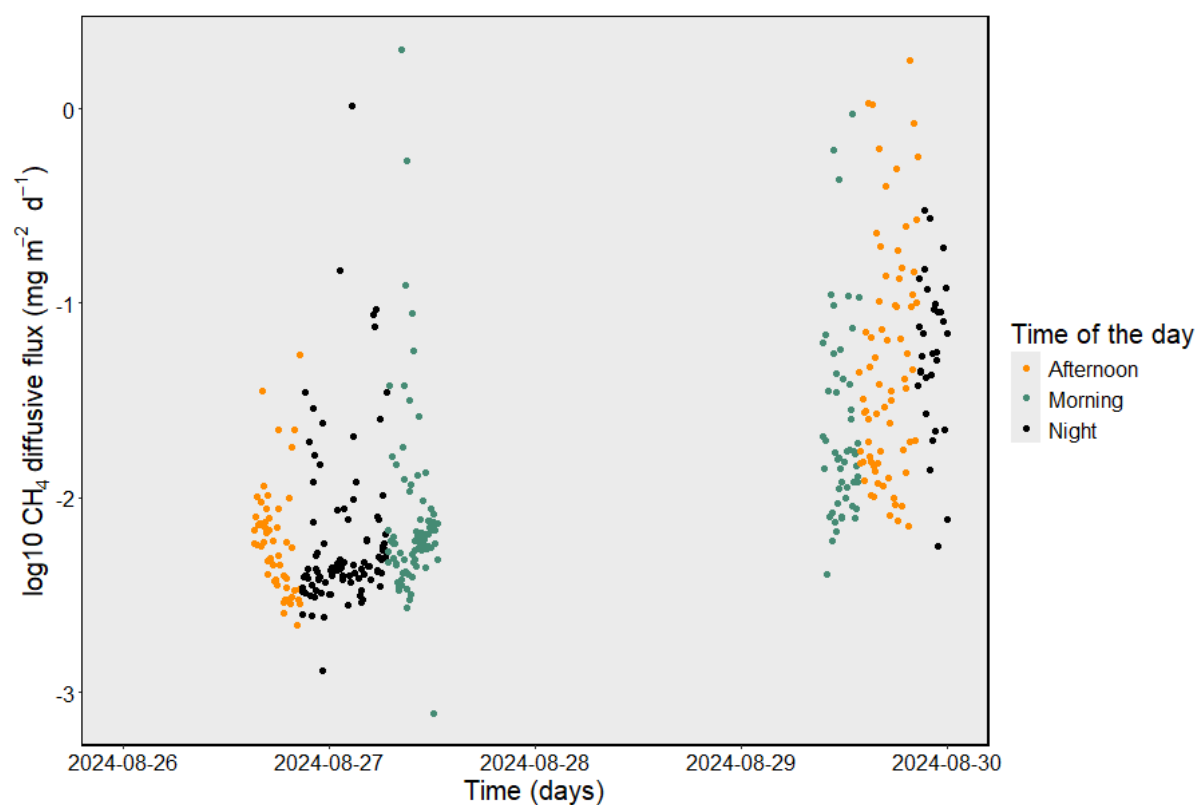


Figure S9. Log10 CH₄ diffusive emissions from the ditch, obtained with the automatic chambers. The different colours represent the moment of the day: afternoon (yellow), morning (green) or night (black). Data could be collected for the afternoon and night of the 26th of August, morning of 27th August, and also morning, afternoon and night of the 29th of August 2024.

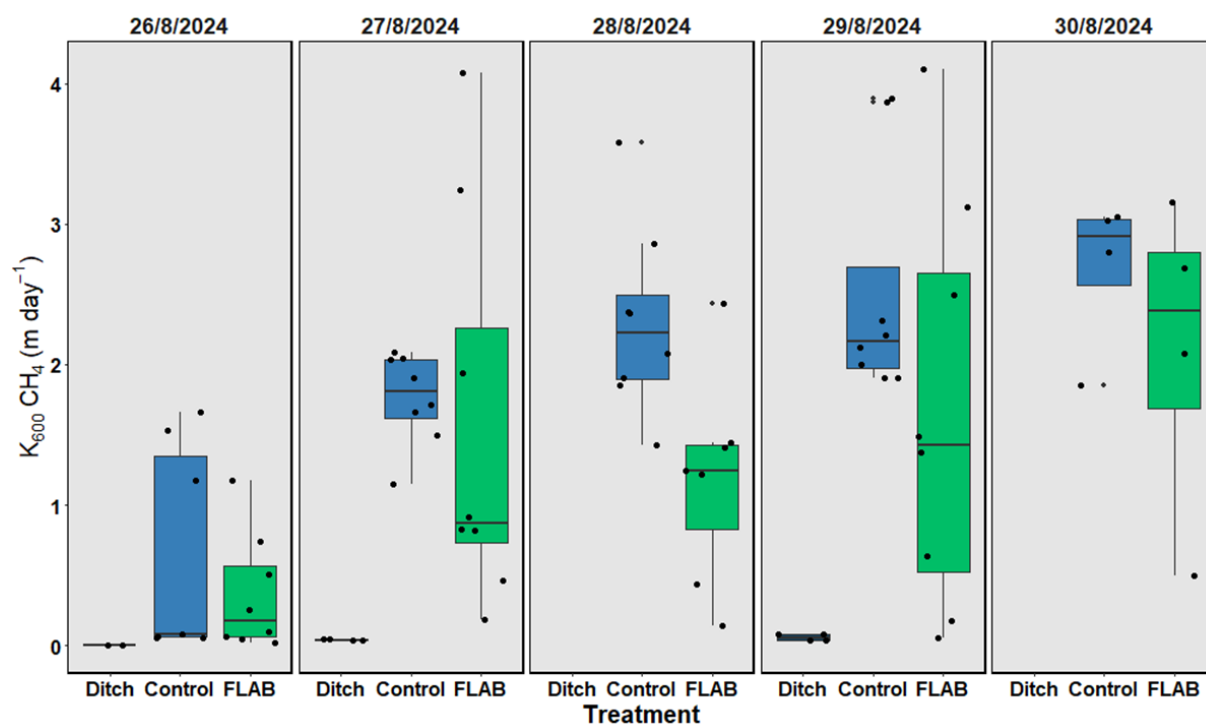


Figure S10. Methane (CH_4) standardized exchange velocities (K_{600}) for the ditch, the control and FLAB treatment. Each panel represents one day of the experimental period. For the ditch, the exchange velocity could be obtained for the same days as the CH_4 diffusive fluxes (26th, 27th and 29th of August).

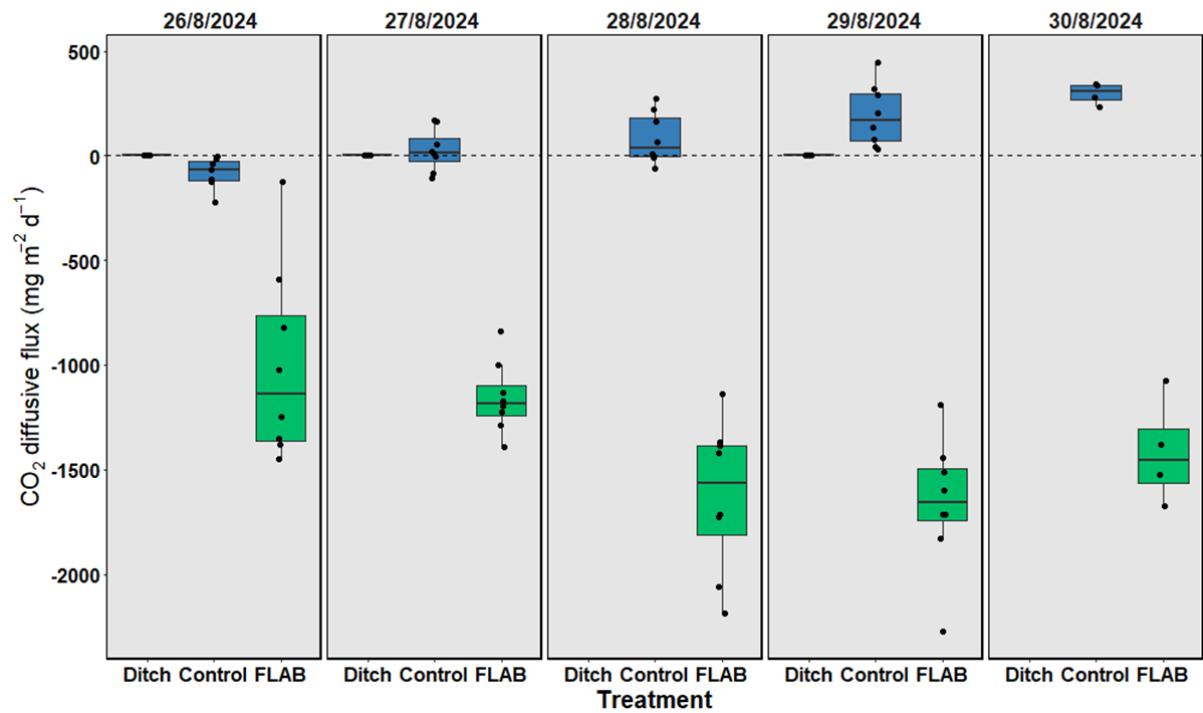


Figure S11. Carbon dioxide (CO₂) diffusive flux from the ditch, the control and FLAB treatment. Each panel represents one day of the experimental period. The dashed line represents a zero flux, higher fluxes indicate that the system is acting as a source of CO₂, whereas lower fluxes indicate that the system is acting as a sink of CO₂. Each data point from the control and FLAB treatment corresponds to a flux measured: between the 26th and the 29th two measurements were done *per* day and *per* replicate (morning and afternoon), whereas on the 30th one measurement was done *per* replicate (morning). Each data point for the ditch, corresponds to the automatically measured diffusive fluxes in the morning and/or afternoon of that day. All measurements were done during daytime.

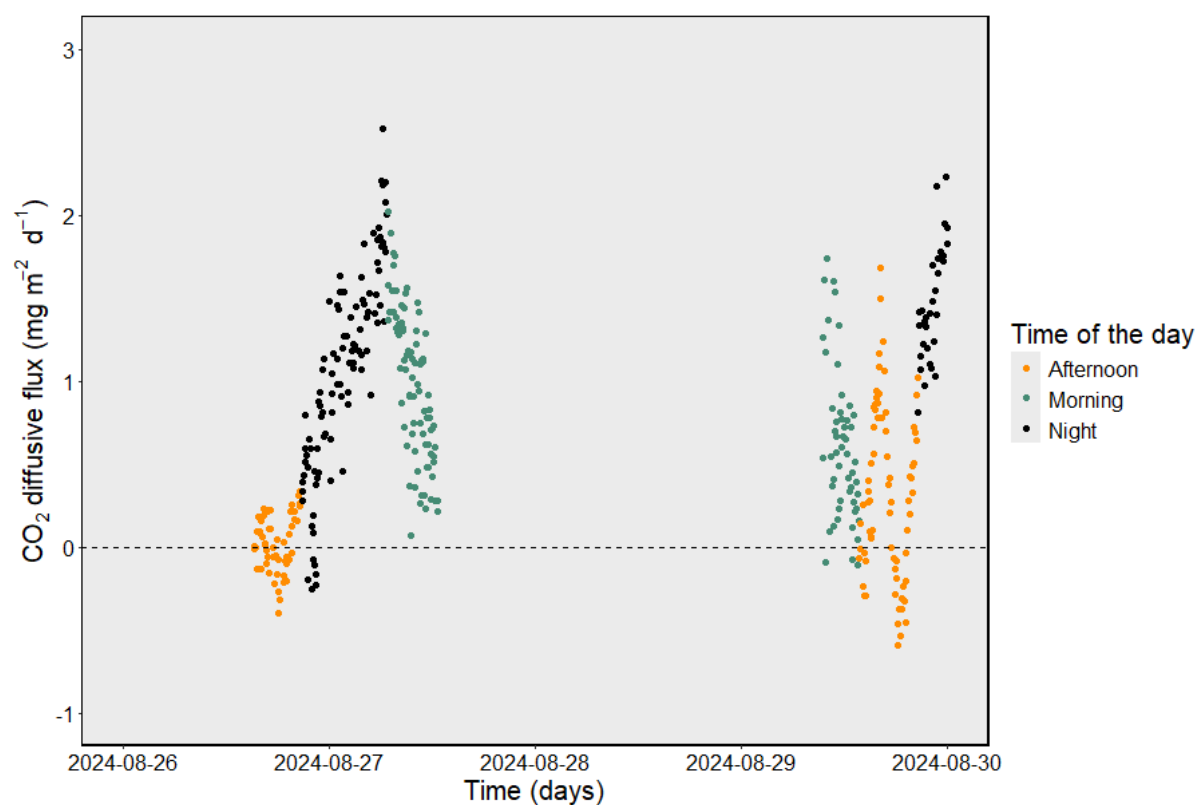


Figure S12. Carbon dioxide (CO₂) diffusive fluxes from the ditch, obtained with the automatic chambers. The different colours represent the moment of the day: afternoon (yellow), morning (green) or night (black). Data could be collected for the afternoon and night of the 26th of August, morning of 27th August, morning and afternoon of the 29th and night of the 30th of August 2024. The dashed line represents a zero flux, higher fluxes indicate that the system is acting as a source of CO₂ to the atmosphere, whereas lower fluxes indicate that the system is acting as a sink of CO₂.

Table S2: Sediment CH₄ production rates obtained from the intact core incubations and obtained from the laboratory sediment slurry incubations, as well as sediment CH₄ oxidation rates obtained from the sediment slurry incubations.

Sediment cores (n = 7)	Ditch		
	Min	Mean	Max
nmol CH ₄ g wet weight sediment ⁻¹ h ⁻¹	0.04	0.47 ± 0.44	1.4
Sediment incubations in laboratory	Ditch	Control	FLAB
CH ₄ production nmol CH ₄ g wet weight sediment ⁻¹ h ⁻¹	0.64 ± 0.11	0.47 ± 0.03	0.57 ± 0.04
CH ₄ oxidation nmol CH ₄ g wet weight sediment ⁻¹ h ⁻¹	-1.96 ± 0.00	-1.88 ± 0.00	-0.86 ± 0.02

For the sediment cores measured *in-situ* with an LGR, a minimum, mean ± standard deviation and maximum value from all seven measured cores was calculated. For the sediment incubations, the mean ± standard deviation of production or oxidation was calculated for the core obtained from each treatment or the ditch.

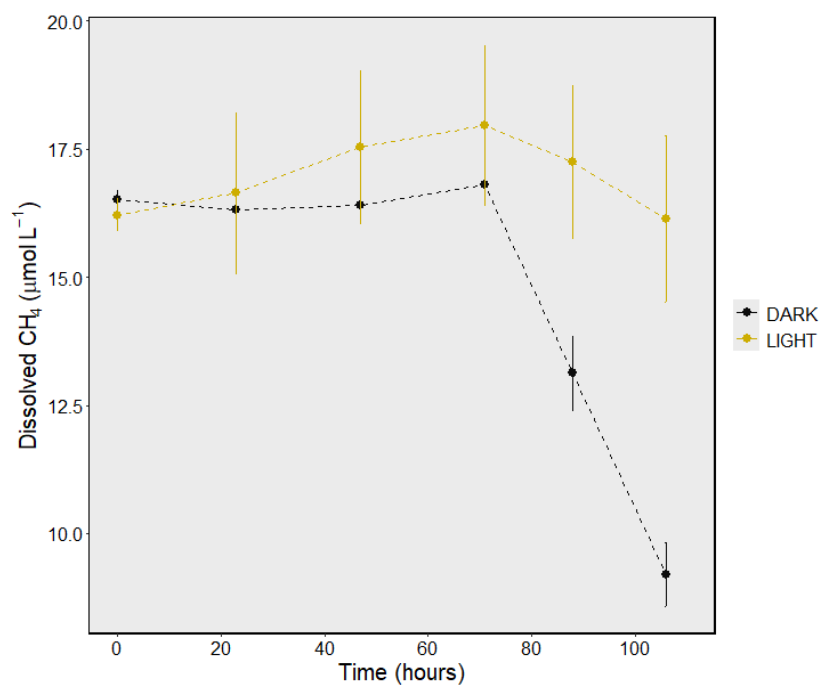


Figure S13. Incubations of water from the ditch under light (yellow) and dark (black) conditions, in all cases adding 1ml of pure CH₄ to the incubations. Data from 70h onwards was used to calculate the MOX rate for light and dark conditions, obtained as the slope of the regression between dissolved CH₄ and time. The obtained rates were $-0.05 \mu\text{mol L}^{-1} \text{h}^{-1}$ ($-1.3 \mu\text{mol L}^{-1} \text{d}^{-1}$) for light conditions, and $-0.2 \mu\text{mol L}^{-1} \text{h}^{-1}$ ($-5.3 \mu\text{mol L}^{-1} \text{d}^{-1}$) for dark conditions.

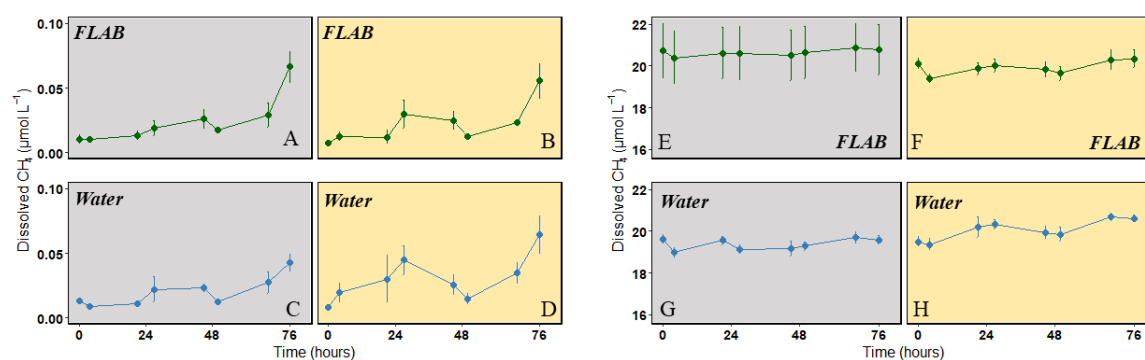


Figure S14. Incubation results for the replicates just with water (blue; C, D, G, H) of the replicates with water + FLAB (green; A, B, E, F), from the treatment under complete dark (grey) or light (yellow) conditions, and for the incubations where there was no extra addition of CH_4 (A, B, C and D) and for the incubations where CH_4 was added to the headspace (E, F, G, H). The patterns of the replicates with water or with water + FLAB do not differ in the conditions either with or without CH_4 addition.

Table S3. Scenarios selected to model FLAB effect in each one of the replicates from each treatment.

Treatment	Replicate ID	<i>Sed</i>	<i>MOX</i>	<i>I</i>	<i>f</i>	<i>NRMSE</i>
FLAB	1	Low	Low	26.7	0.04	27.2
	5	Mean	Mean	37.5	0.03	33.5
	6	Mean	Mean	45.2	0.03	44.9
	8	Low	Mean	44.4	0.01	26.0
Control	2	Low	Low	NA	NA	45.4
	3	Low	Low			39.9
	4	Low	Low			40.6
	7	Low	High			66.8

For sediment CH₄ production (*Sed*) the low, mean and maximum scenarios corresponded to 6.2, 97.8 and 323.6 mg m⁻² d⁻¹; for methane oxidation rates (*MOX*) the low, mean and maximum scenarios corresponded to 1.3, 3.3 and 5.3 μmol L⁻¹ d⁻¹; *I* value correspond to the input rate of OC (g day⁻¹) originating from decaying FLAB; *f* is the fraction of OC that is converted to CH₄ (unitless); NRMSE is the normalized root mean square error of the model fit (as a measure of how well the model explained the measured CH₄ concentrations); values of *I* and *f* for control replicates are NA because in those cases there was no FLAB.

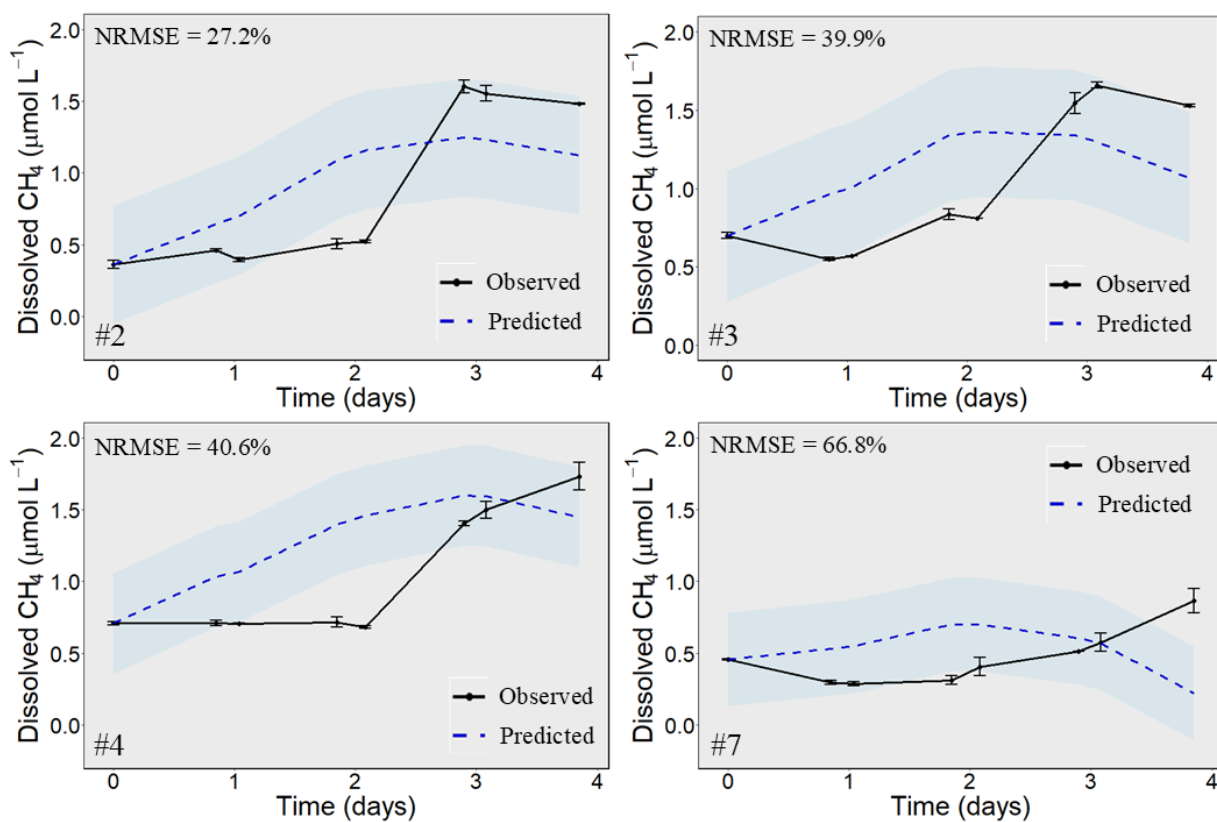


Figure S15. Modelled (blue) versus observed (black) CH_4 concentrations in each one of the four replicates of the control treatment. The shaded area around the blue curve corresponds to the standard deviation of the residuals from the model. The points and error bars of the black curve correspond to the measured time points and their standard error bars.

References

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