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1 **Critical fluid injection volumes for uncontrolled**
2 **fracture ascent.**

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6 **Key Points:**

- 7 • Three-dimensional threshold volumes for self-sustained fluid-filled fracture ascent
8 • We derive analytical equation and validate it through numerical boundary-element
9 simulations
10 • Assessing safe hydro-fracture operation volumes requires quantitative modeling
11 of in-situ complexities

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12 **Abstract**

13 Hydro-fracturing is a routine industrial technique whose safety depends on fractures re-
 14 maining confined within the target rock volume. Both observations and theoretical mod-
 15 els show that, if the fluid volume is larger than a critical value, pockets of fluid can prop-
 16 agate large distances in the Earth’s crust in a self-sustained, uncontrolled manner. Ex-
 17 isting models for such critical volumes are unsatisfactory, most are two-dimensional and
 18 depend on poorly constrained parameters (typically the fracture length). Here we de-
 19 rive both analytically and numerically in three dimensions scale-independent critical vol-
 20 umes as a function of only rock and fluid properties. We apply our model to gas, wa-
 21 ter and magma injections in laboratory, industrial and natural settings, showing that our
 22 critical volumes are consistent with observations and can be used as conservative esti-
 23 mates. We discuss competing mechanisms promoting fracture arrest, whose quantita-
 24 tive study could help to assess more comprehensively the safety of hydro-fracturing op-
 25 erations.

26 **Plain Language Summary**

27 Fractures in rocks can act as channels for fluids. Fracking, or hydro-fracturing, in-
 28 volves injection of fluids at high pressure in order to grow fractures within the rock and
 29 increase its permeability. Fluid volumes need to be kept below a threshold value: if the
 30 fluid volume is larger, then the stresses at the tips of the fluid pocket will be large enough
 31 for the fluids force their way around by fracturing the rock ahead of them. Previous the-
 32 oretical models for the critical volumes are unsatisfactory as they are two-dimensional
 33 and based on poorly constrained parameters. We derive and test a new three-dimensional
 34 equation that uses only rock and fluid parameters. We find that typical volumes injected
 35 in hydro-fracturing operations are over the limit we define. We argue they are still mostly
 36 safe as additional processes often hinder fracture growth. Further work is needed to com-
 37 prehensively quantify mechanisms that hinder hydro-fracture arrest.

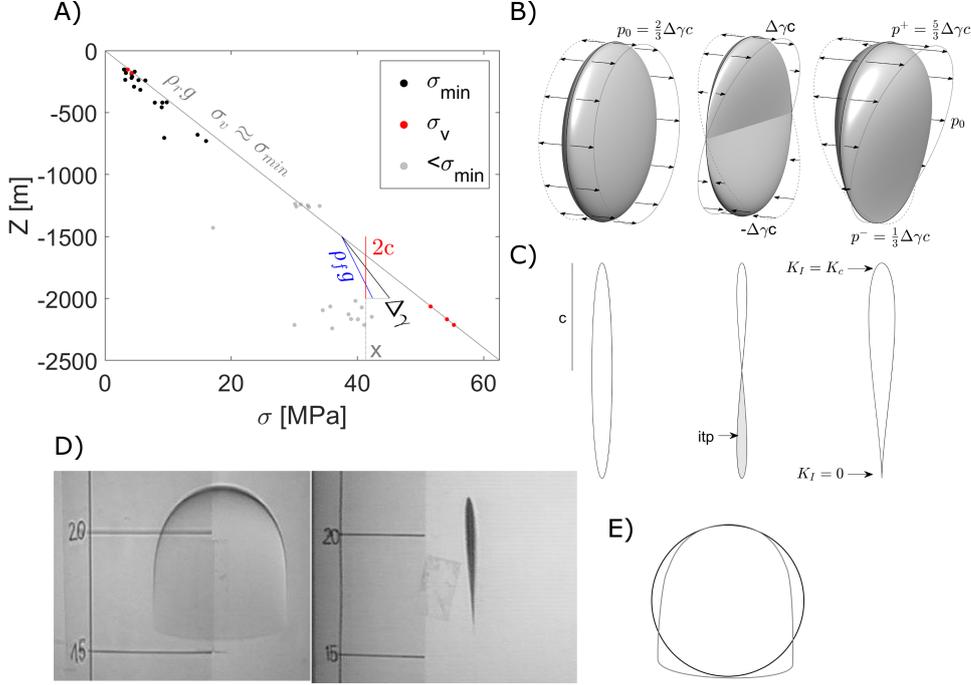
38 **1 Introduction**

39 Official guidelines for hydraulic fracturing (e.g., Mair et al., 2012; EPA, 2016), out-
 40 line safe operational practices for regulators. Such reports often state that during rou-
 41 tine operations fractures are unlikely to grow out of the target rock formation, as typ-
 42 ical injection pressures are too low for this to occur. These claims are substantiated with
 43 empirical observations from closed access microseismic data of scarce vertical fracture
 44 growth following injection (Fisher & Warpinski, 2012). Evidence for unsafe vertical mi-
 45 gration of such fluids remains ambiguous (Vidic et al., 2013).

46 Natural analogues of fluid migration by hydro-fracturing include drainage crevasses
 47 in melting glaciers and magma transport by dyking. Field and experimental observations
 48 provide some indication of typical rates of fracture ascent, in the order of mm/s to around
 49 half a m/s (Das et al., 2008; Tolstoy et al., 2006). For water-filled fractures in rock this
 50 has not been observed; estimates from geochemical analysis supply similar rates of ~ 0.01 -
 51 0.1 m/s, (1 km/day) (Okamoto & Tsuchiya, 2009). Theoretical arguments suggest that
 52 the migration velocity should have a dependency on volume (Heimpel & Olson, 1994;
 53 Dahm, 2000).

54 According to theory, tip-propagation occurs when a critical amount of fluid has ac-
 55 cumulated inducing enough stress to overcome the medium’s fracture toughness, K_c (Secor
 56 & Pollard, 1975). So far, critical ‘volumes’ are given in terms of the fracture length, which
 57 is not directly observable and difficult to estimate from observations (Secor & Pollard,
 58 1975; Dahm, 2000; Taisne et al., 2011); moreover, such analyses have been carried out
 59 in 2D only, not capturing the fracture’s 3D shape and scaling of volume vs length.

Figure 1. A) Stress vs depth in the crust, data from Bell et al. (1990), crack shown in red with length $2c$. B) Stress boundary conditions and 3D crack wall displacement. C) Cross sections of crack wall displacement, itp=interpenetration. D) Shape of an ascending air filled crack in gelatine from (Rivalta & Dahm, 2006). E) Air filled cracks tip-line vs a penny-shaped tip-line.



60 Here, after deriving a theoretical model and validating it with numerical simulations, we apply this to cracks filled with air, water, oil and magma in solids of varying
 61 stiffness and toughness, across a wide range of length scales.
 62

63 Methods

64 1.1 Hydrofracturing and stress gradients

65 We consider a pressurised penny-shaped crack of radius c and volume V in an elas-
 66 tic medium. The crack can only grow when the stress intensity K_I at its tip-line exceeds
 67 K_c . The elastic parameters of the medium (shear modulus, μ , and Poisson's ratio, ν) con-
 68 trol the fracture's aperture. The internal pressure p_0 must overcome the stress normal
 69 to the crack walls (generally the minimum compressive stress, σ_{min}) by an amount ac-
 70 commodating the volume V against the elastic forces, Fig. 1A/B.

71 When the crack is vertical, the gradient in the normal stress acting to close the crack
 72 and the gradient in the load due to the overlying fluid acting to open the crack, i.e. $\rho_r g$
 73 and $\rho_f g$ in Fig. 1A, where ρ_r and ρ_f are the densities of the host rock and fluid, respec-
 74 tively, result in a net stress gradient $\Delta\gamma$ acting to push open the crack walls in an in-
 75 verse 'teardrop' shape, Fig. 1B/C. When the crack is inclined $\Delta\gamma$ needs to be adjusted
 76 by $\cos(\theta)$, where θ is the cracks' angle away from vertical. Quantitative formulations used
 77 to assess industrial fracture heights neglect stress gradients (e.g., Xu et al., 2019; Yue
 78 et al., 2019). This contrasts with routine observations of stress gradients from industry

79 data (Fig. 1A) and the fact that these gradients are considered in the well design of in-
 80 dustrial operations (Lecampion et al., 2013; Mair et al., 2012). When this gradient is in-
 81 cluded in formulations, stress intensity varies around the fracture’s tip-line (Fig. 2). Where
 82 K_c is exceeded, the upper tip-line advances. The contained fluid flows into this newly
 83 created fracture surface while the bottom edge of the fracture is pinched shut as the in-
 84 ternal pressure drops. With a great enough volume this fluid movement maintains a crit-
 85 ically stressed upper tip-line and the fracture reaches a state of ‘self-sustaining propa-
 86 gation’. Fluid viscosity will cause some fluid to stay trapped in the tail trailing behind
 87 the fracture; if fluid viscosity is low enough, the contained fluid is virtually all transported.
 88 Provided the fracture’s shape and volume are maintained, no additional forces, such as
 89 pressure from injection, are required to aid this state of propagation.

90 1.2 Analytical formulation

91 Secor and Pollard (1975) define in 2D the size and pressure inside a vertical frac-
 92 ture subject to $\Delta\gamma = (\rho_r - \rho_f)g$ such that at the upper tip $K_I^+ = K_c$ and at the lower
 93 tip $K_I^- = 0$. We derive an analytical expression for the fluid volume needed for a three-
 94 dimensional crack to propagate in a self-sustained manner.

95 K_I for a mode I penny-shaped fracture of radius c subject to a generic linear stress
 96 gradient can be expressed as the superposition of K_I for a penny-shaped fracture sub-
 97 ject to a uniform pressure p_0 :

$$98 K_I = \frac{2}{\pi} p_0 \sqrt{\pi c} \quad (1)$$

99 and that for a penny-shaped fracture subject to a linear pressure gradient $\Delta\gamma$ where pres-
 100 sure is equal to 0 at the fracture’s midpoint (Tada et al., 2000, p. 355):

$$101 K_I^\pm = \pm \frac{4}{3\pi} \Delta\gamma c \sqrt{\pi c} \quad (2)$$

102 where the + refers to the propagating tip and the - to the basal tip. Requiring $K_I^- =$
 103 0 results in $p_0 = 2\Delta\gamma c/3$ and thus:

$$104 p^\pm = \left(\frac{2}{3} \pm 1\right) \Delta\gamma c \quad (3)$$

105 Requiring $K_I^+ = K_c$ and rearranging for c yields:

$$106 c = \left(\frac{3\sqrt{\pi}K_c}{8\Delta\gamma}\right)^{2/3} \quad (4)$$

107 We note that the 2D plane strain critical length is $\approx 0.9c$. The volume of the crack can
 108 be calculated based on the equation for a crack pressurised by uniform pressure p_0 , as
 109 the antisymmetric pressure contribution integrates to zero. Thus using (Tada et al., 2000):

$$110 V = \frac{8(1-\nu)}{3\mu} p_0 c^3 \quad (5)$$

111 results in:

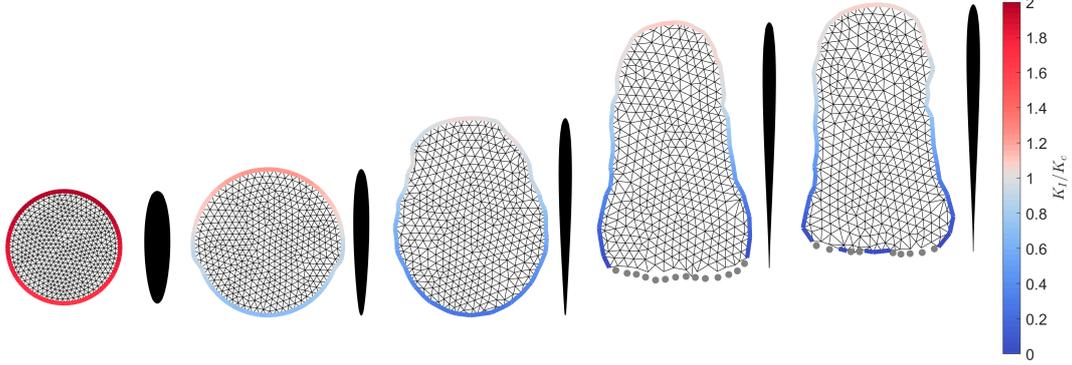
$$112 V_c^{an} = \frac{(1-\nu)}{16\mu} \left(\frac{9\pi^4 K_c^8}{\cos(\theta)\Delta\gamma^5}\right)^{1/3} \quad (6)$$

113 This equation requires validation in order to evaluate the bias due to approximating the
 114 shape of the propagating crack as circular (Fig. 1D/E).

115 1.3 Numerical model

116 To simulate propagation, we use a 3D Boundary Element program where each el-
 117 ement is a triangular dislocation with constant displacement (Fig. 2) (Nikkhoo & Wal-
 118 ter, 2015). The program computes fracture opening and stress intensities, based on frac-
 119 ture shape, rock and fluid parameters and external stresses Davis et al. (2019). Our work-
 120 flow during each iteration is as follows:

Figure 2. Numerical simulation of crack propagation (from left to right), looking at the fractures' face (left) and cross section (right). Grey points are edges that closed in the previous iteration.



- 121 1. We invert for the uniform internal fluid pressure, p_0 , necessary to open the crack
122 to match the required volume against all external and internal tractions. Non-linear
123 complementarity conditions are imposed such that the crack's faces cannot inter-
124 penetrate (Davis et al., 2019).
- 125 2. We calculate the crack opening and the stress intensity at the tipline using the method
126 of Davis et al. (2019). In order to reduce artefacts, we smooth the stress inten-
127 sity along the tip line by averaging the local K_I with its two neighbouring edges.
- 128 3. We calculate the advance or retreat of the tipline. At elements where K_I exceeds
129 K_c , the tip-line will advance proportional to K_I/K_c . This approximation is akin
130 to the "Paris fatigue law" (Lecampion et al., 2018). The maximum crack advance
131 will occur at the triangle where K_I is maximum; this advance is set equal to the
132 mesh's average triangle size. The triangular elements that close are removed. The
133 simulation assumes the fluid is inviscid, and, as such, we cannot retrieve time-dependent
134 propagation rates.
- 135 4. Once the fracture's edge has been updated, it is re-meshed and cleaned such that
136 the triangles on the fractures tip-line are approximately equal size and isosceles
137 (Da & Cohen-Steiner, 2019).

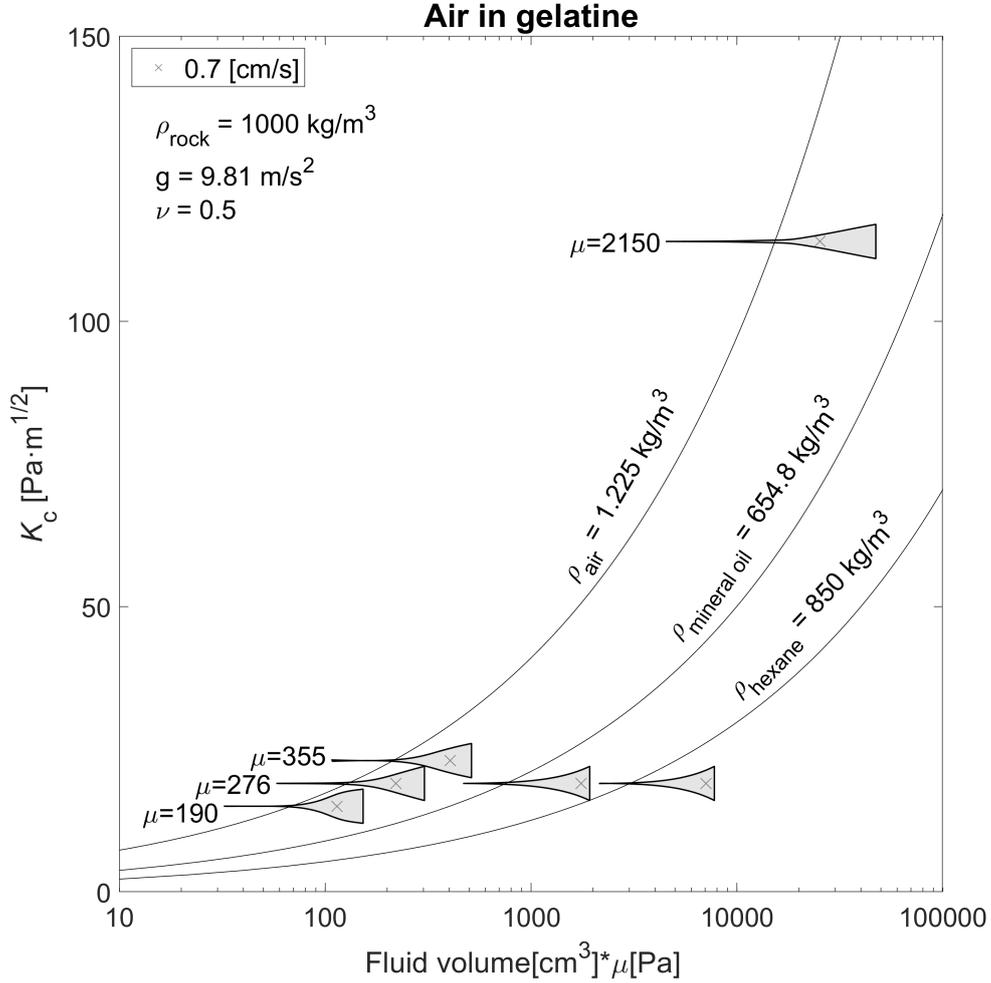
138 For a description of the numerical methods accuracy, see the appendix. We start
139 the simulation with a vertical penny-shaped crack. We fix the number of elements, K_c ,
140 $\Delta\gamma$, μ , ν and the volume of fluid, V . We set the initial radius to $0.4c$, (Eq. 4). In our
141 350+ simulations we use variables spanning several orders of magnitude: $G=190-5\cdot 10^{10}\text{Pa}$,
142 $\nu=0.25-0.49$, $\Delta\gamma=7.8\cdot 10^2-2.2\cdot 10^4\text{Pa}\cdot\text{m}^{-1}$ and $K_c=1-1\cdot 10^8\text{Pa}\cdot\text{m}^{0.5}$. We state the fracture
143 has reached self-sustaining ascent when its upper tip has travelled $4c$ upwards.

144 For all simulations, independent of mesh sampling, we find that if $V = 0.7V_c^{an}$
145 the numerical code returns a trapped fracture and if $V = 0.8V_c^{an}$ the fracture always
146 reaches self-sustaining propagation. Therefore, scaling Eq. 6 by 0.75 supplies the numer-
147 ical estimate of V_c , independent of the scale we use:

$$148 \quad V_c^{num} = 0.75 \frac{(1-\nu)}{16\mu} \left(\frac{9\pi^4 K_c^8}{\cos(\theta)\Delta\gamma^5} \right)^{1/3} \quad (7)$$

149 For all cracks that reached self-sustaining propagation the horizontal and vertical lengths
150 were greater than $\sim 0.6c$ and $\sim 1.14c$, respectively.

Figure 3. $V^*\mu$ vs K_c from Heimpel and Olson (1994). Eq. 7 predictions shown as black lines. The thickness of the grey filled patches represents the velocity of the crack as the volume increases, normalised by maximum observed velocity.



2 Applications

2.1 Analog gelatine experiments

The analog study of Heimpel and Olson (1994) inspects critical volumes of fluids ascending in gelatine blocks of different stiffness and fracture toughness (Fig. 3). The graph of volume vs speed from their experimental results shows a rapid increase in speed past a certain volume. The authors interpret that at velocities past ~ 0.7 cm/s (crosses in Fig. 3), the ascent transitions from a sub-critical propagation regime ($K_I < K_c$); where the fracture growth speed at the tip limits the velocity (Atkinson & Meredith, 1987), to a dynamic propagation regime. We test if our equation can predict volume of fluid that causes this transition in ascent speed. As Heimpel and Olson (1994) estimate K_c directly from this change in velocity, to verify that we can use this estimation, we calculate K_c differently; directly from the measured value of G . Strain energy release \mathcal{G} increases with greater stiffness in gelatin solids: $\mathcal{G}[\text{N/m}] \approx 6.66 \cdot 10^{-4} G[\text{Pa}]$ (Czerner et al., 2016). This

164 second independent estimate of K_c lies within $5 \text{ Pa}\cdot\text{m}^{1/2}$ of the original estimate. Us-
 165 ing $\rho_r=1000 \text{ kg}\cdot\text{m}^{-3}$, $\nu=0.5$ and setting μ , ρ_f and K_c to match the experiments of Heimpel
 166 and Olson (1994), we find that our value of V_c^{num} independently captures the point at
 167 which the velocity transitions, described above, supporting the previous interpretation
 168 that this describes the transition to dynamic fracture propagation.

169 2.2 Magmatic dykes

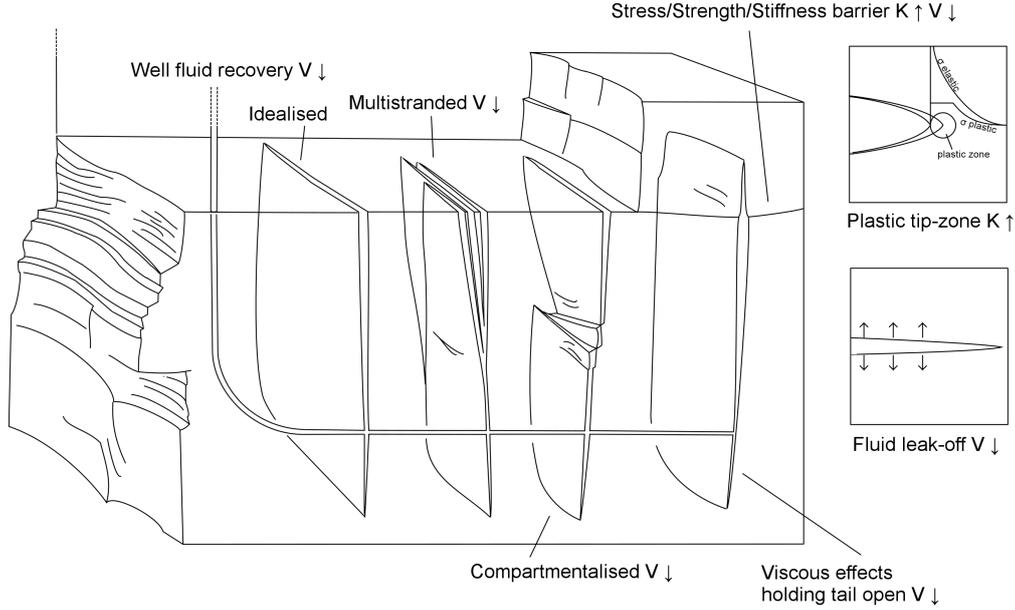
170 We consider magma propagation volumes at Piton de la Fournaise, La Réunion,
 171 to see how our equation matches observed dyke volumes. The volumes of the dyke in-
 172 trusions observed between 1998-2016 range from $0.05\text{-}3.2\cdot 10^6\cdot\text{m}^3$ (Froger et al., 2004; Fukushima
 173 et al., 2005, 2010; Smittarello et al., 2019). Using $\rho_r-\rho_f=100 \text{ kg}\cdot\text{m}^{-3}$, $\mu=5 \text{ GPa}$, $\nu=0.25$
 174 and K_c ranging from 29 to $112 \text{ MPa}\cdot\text{m}^{1/2}$ (Fukushima et al., 2010; Delaney & Pollard,
 175 1981), we retrieve $V_c^{num}=0.05\cdot 10^6$ and $2\cdot 10^6\cdot\text{m}^3$, respectively. The critical volumes we
 176 estimate are consistent with the observed dyke sizes. As such our approximation pre-
 177 dictes the correct scale in natural settings, provided K_c values estimated from field data
 178 are used, noting such field values appear to correct due to a number of additional pro-
 179 cesses that we have disregarded, instead of being representative of the rock strength at
 180 the scale of a laboratory sample.

181 2.3 Water injection into stiff rock

182 The UK government defines hydraulic fracturing as operations that use over 1,000
 183 m^3 of fluid per frack stage. During a hydro-fracturing procedure, proppant is injected
 184 in the final phase to maintain an open fracture (e.g. spherical quartz grains). After the
 185 operation, not all injected fluid is recovered when the wellhead valve is opened: Vidic
 186 et al. (2013) report an average of only 10% fluid recovery in flowback waters, noting that
 187 this recovery volume decreases when shut-in times are longer. Using $\rho_r=2700 \text{ kg}\cdot\text{m}^{-3}$,
 188 $\rho_f=1000 \text{ kg}\cdot\text{m}^{-3}$, $\mu=8.9 \text{ GPa}$, $\nu=0.25$ and K_c in the range $0.36\text{-}4.05$ to $7\text{-}25 \text{ MPa}\cdot\text{m}^{1/2}$,
 189 we obtain $V_c^{num} = 6\cdot 10^{-2}$ and 500 m^3 respectively. These K_c values are for laboratory-
 190 sized shale samples from 100 to 1000 m confining pressure and effective K_c values esti-
 191 mated for veins in the field, respectively (Gehne et al., 2020; Olson, 2003). Current op-
 192 erations use volumes around double our highest predicted limit. Few observations at-
 193 test to the fact that industrial operations can cause ascent of fluids in fractures. One such
 194 example, are the spectacular surface fissures created due to steam injection documented
 195 in Schultz (2016); additional examples can be found in Schultz et al. (2016). Geochem-
 196 ical data from aquifers above fracking operation sites has shown some evidence of the
 197 contamination of overlying units, which is attributed to poor well casing design, rather
 198 than fracture ascent (Vidic et al., 2013). Usually, microseismic monitoring of actual frack-
 199 ing operations show limited vertical extents of the fractures, however, these data are pro-
 200 prietary and methodological descriptions are scarce (Fisher & Warpinski, 2012). Exper-
 201 imental fracturing data is of little help as volumes injected are typically below or close
 202 to our volumetric limit, with injected volumes of 2 to 20 m^3 (Warpinski et al., 1982; Pan-
 203 durangan et al., 2016).

204 Natural degassing, such as CO_2 in the Cheb basin, Czech Republic, has chemical
 205 signatures of fluids that have ascended over 20 km through the crust (Weinlich, 2014).
 206 Fracture driven ascent can explain this phenomena without the requirement of perma-
 207 nent highly conductive fluid pathways at great depths. Supercritical CO_2 at depth has
 208 a similar density to water, and as such may be a good natural analog for water filled frac-
 209 ture ascent. We saw that in analogue and magmatic examples Eq. 7 predicts the cor-
 210 rect order of magnitude of critical volumes; at the same time, it appears that this equa-
 211 tion is conservative for high volume water injection as fracture ascent in these settings
 212 has rarely been observed.

Figure 4. Processes that can hinder fracture ascent, K and V relate to effective K_c and V_c operating in Eq. 7



3 Discussion and conclusions

In summary, Eq. 7 provides an estimate of the minimum fluid volume for self-sustained propagation of fluid-filled fractures, ranging from cm to tens of km. V_c is dependent on $K_c^{8/3}$; since K_c is often poorly constrained V_c suffers from large uncertainties. Values of K_c obtained in laboratory experiments show a strong dependency on pressure and temperature. Field estimates of effective K_c from trapped fractures can be orders of magnitude larger. An effective way to estimate K_c in Eq. 7 incorporating all processes affecting the energy needed to extend the fracture at different scales would clearly be beneficial for any fracture mechanics based analysis of rock masses and the resultant interpretations.

In our derivation we have neglected the effects of viscosity. Whether these effects will dominate over toughness in determining fracture growth can be assessed by evaluating the time scale needed for the fluid pressure to equilibrate within the crack, as this will mean that viscous dissipation is low and crack growth will be toughness-dominated (Bunger & Detournay, 2007). The model of Bunger and Detournay (2007) assumes a constant injection rate with no stress gradients, we assume this still provides a rough estimate of the timescale until this transition. Typical industrial operations use fluid viscosity of 0.001-0.01 Pa-s, injection rates between 0.5-10 m³/min and stiffness's of 10-40 GPa. Using low values of K_c from laboratory experiments in shale, 0.36 MPa·m^{1/2}, this transition time ranges between 1 minute to times exceeding the end of injection. Whereas, setting K_c higher, values for shale at depth, e.g. 4 MPa·m^{1/2} this significantly reduces this range from milliseconds to a maximum of 5 hours. This suggests that, depending on K_c , Eq. 7 can be a relevant estimate of V_c^{num} , independent of viscous forces.

While theory and experiments support Eq. 7, this appears to be overly conservative in practice, as injections of quantities of fluid exceeding this do not result in significant ascent in most cases. In part, this discrepancy results from our simplification of

239 the process, as mass conserving propagation in a homogeneous linear-elastic medium.
 240 Fig. 4 shows a schematic of processes not quantified in relation to critical fluid volumes
 241 which we review in detail below.

- 242 1. A series of mechanisms can reduce V during propagation and thus promote crack
 243 arrest. These include leak-off from the fractures faces, the fracture becoming mul-
 244 tistranded/compartmentalised, fluid recovery (extraction), or fluid remaining in
 245 the tail of the fracture due to added proppant or viscous forces (Taisne & Tait,
 246 2009).
- 247 2. Mechanisms that can lead to an effective increase of K_c , and thus also promote
 248 crack arrest, include plastic tip processes, the fracture entering in a zone of dam-
 249 age of the host rock (Sih et al., 1965; Kaya & Erdogan, 1980), or seismicity sur-
 250 rounding the fracture, causing reduction in the system’s energy/blunting the frac-
 251 ture’s tip (Rivalta et al., 2015).
- 252 3. Heterogeneous μ or K_c or stress barriers may also lead to arrest of fractures by
 253 deflection or promoting lateral growth (Maccaferri et al., 2011; Bungler & Lecam-
 254 pion, 2017; Warpinski et al., 1985),
- 255 4. Eq. 7 has a clear dependency on the fracture’s dip. If the minimum compressive
 256 stress is vertical, this promotes flat lying fractures.

257 Quantification of processes acting to halt fracture ascent, especially in the context
 258 of the variables in our equation, are critical to understand which volumetric limits can
 259 be deemed safe. In particular, the gradient in stress with depth must be included to as-
 260 sess this process. Without such quantification, regulation of this industrial process will
 261 continue to rely on empirical evidence for safe rates, volumes and depths from select op-
 262 erations that may not be representative.

263 Appendix A Numerical

264 A1 Numerical accuracy

265 We verify that our method to compute K_I is independent of crack shape and bound-
 266 ary condition. Previously this was only compared to solutions for a circular crack sub-
 267 ject to uniform stresses (Davis et al., 2019). We compare this to the analytical solution
 268 for the stress intensity around an elliptical crack, subject to a superposition of uniform
 269 pressure and a linear gradient of stress, such that, at the basal tip, $K_I = 0$ (Fig. 1) (Atroshchenko
 270 et al., 2009). We note that under a stress gradient, K_I for vertically aligned elliptical
 271 cracks is not maximal at its upper tip, due to the reduction in crack surface area prox-
 272 imal to this edge.

273 For a mesh with 650 triangles (Fig. A1A/B), the greatest vertical separation be-
 274 tween the numerical points and the analytical line is 0.09. For this test we required the
 275 edge points of the mesh’s triangles, not the midpoints of the triangles edge where K_I is
 276 calculated, to lie on the tip-line defined by the analytical solution. For a mesh with 1500
 277 triangles (Fig. A1C/D), the maximum vertical distance from the analytical solution of
 278 is 0.06, noting that greater sampling does not necessarily converge to a improved accu-
 279 racy, see appendix of Davis et al. (2019).

280 As a further test of numerical accuracy, we compare how well the numerical method
 281 approximates the opening volume of a penny shaped crack subject to tension (Tada et
 282 al., 2000). We find a sampling of 650 triangles overestimates the volume by 5.2%, by
 283 increasing the triangle count to 1500 this drops to 3.5%.

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Figure A1. Stress intensity factor approximation using the 3D displacement discontinuity method. A/C) Elliptical crack meshed with 650/1500 triangles respectively, B/D) Numerical (dots) and analytical (solid line) results. Results are normalised relative to the maximum analytical value of K_I .

