1	The architecture of an intrusion in magmatic mush
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## 18 Abstract:

19 Magmatic reservoirs located in the upper crust have been shown to result from the repeated intrusions of new magmas, and spend much of the time as a crystal-rich mush. The 20 geometry of the intrusion of new magmas may greatly affect the thermal and compositional 21 evolution of the reservoir. Despite advances in our understanding of the physical processes that 22 may occur in a magmatic reservoir, the resulting architecture of the composite system remains 23 poorly constrained. Here we performed numerical simulations using a computational fluid 24 dynamics and discrete element method in order to illuminate the geometry and emplacement 25 dynamics of a new intrusion into mush and the relevant physical parameters controlling it. Our 26 results show that the geometry of the intrusion is to first order controlled by the density contrast 27 that exists between the melt phases of the intrusion and resident mush rather than the bulk density 28 contrast as is usually assumed. When the intruded melt is denser than the host melt, the intrusion 29 30 pounds at the base of the mush and emplaced as a horizontal layer. The occurrence of Rayleigh-31 Taylor instability leading to the rapid ascent of the intruded material through the mush was 32 observed when the intruded melt was lighter than the host one and was also unrelated to the bulk 33 density contrast as considered before. In the absence of density contrasts between the two melt 34 phases, the intrusion may fluidize the host crystal network and slowly ascend through the mush. 35 The effect of the viscosity contrast between the intruded and host materials was found to have a 36 lesser importance on the architecture of intrusions in a mush. Analyzing the eruptive sequence of well documented eruptions involving an intrusion as the trigger shows a good agreement with our 37

- 38 modeling results, highlighting the importance of specifically considering granular dynamics when
- 39 evaluating magmas and mush physical processes.
- 40 **Keywords:** Mush, Magma, Intrusion, Density contrast, CDF-DEM, Granular mechanics.

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## 42 Introduction:

43 Evidence for injections of new magmas, also called recharge events, are ubiquitous in magmatic systems (Wiebe, 2016). They are inferred to cause the formation of long-lived, 44 supersolidus magmatic reservoirs located in the upper crust (e.g. Annen et al., 2015, 2006; Dufek 45 and Bergantz, 2005; Karakas et al., 2017). Together with the thermal structure of the upper crust 46 and the frequency of recharge, the geometry and mode of emplacement of the intruded magma 47 48 was also identified as having a crucial effect on the long-term evolution of igneous bodies 49 (Annen et al., 2015). Diverse evidence supports the view that magmatic reservoirs reside most time in a mush state that is frequently disturbed by injection of new magmas (e.g. Bachmann and 50 Huber, 2016; Cashman et al., 2017, and reference therein). A magmatic mush is a crystal-rich 51 magma in which crystals are in close and sometimes frictional contacts, forming a semi-rigid 52 53 framework where stress is transmitted by force chains (Bergantz et al., 2017). As a result, mushes transition between crystal-rich suspensions to a 'lock-up' state that inhibits the ability of the 54 magma to erupt. 55

The injection of hotter magma into a cooler host has been suggested as a means to trigger volcanic eruptions (e.g. Caricchi et al., 2014) and the intrusion style plays a fundamental role in the way mush rejuvenates (process of recycling the mush to generate an eruptible magma) prior to eruption (Parmigiani et al., 2014, and references therein). Several scenarios assume that the intruder is emplaced as sills at the base of the mush, and rejuvenate it by supplying heat but no mass except possibly exsolved volatiles (Bachmann and Bergantz, 2006; Bergantz, 1989; Burgisser and Bergantz, 2011; Couch et al., 2001; Huber et al., 2011). Other scenarios consider

that the injected magma may penetrate the mush, producing various degrees of mixing with the resident mush depending on its buoyant acceleration (e.g. Bergantz and Breidenthal, 2001; Koyaguchi and Kaneko, 2000; Weinberg and Leitch, 1998). Whether an intrusion generates extensive mass transfer, or is limited to thermal exchanges between an underplated intruder and a host mush is thus a key element shaping the outcome of open-system events. A major obstacle to our current understanding of the formation and evolution of igneous bodies is that little is known about the architecture of intrusions and controlling physical parameters.

71 Traditionally, mush rejuvenation scenarios have been based on the results of experiments 72 performed with pure fluids mimicking the bulk physical properties (density and viscosity) of the magmas (e.g. Huppert et al., 1986; Jellinek and Kerr, 1999; Snyder and Tait, 1995). Mush 73 74 dynamics, however, differs from that of pure fluids because of the complex rheological feedbacks between melt and crystals. An essential physical process is that melt and crystals may experience 75 relative motions. Numerical simulations explicitly accounting for such decoupled motions as well 76 as the building and destruction of force chains between crystals (Bergantz et al., 2015; Schleicher 77 et al., 2016; Schleicher and Bergantz, 2017) have revealed that the local injection of pure melt of 78 79 the same density and viscosity as the mush interstitial melt easily fluidizes, penetrates, and partially mixes with the overlying mush if it is sufficiently vigorous. This local unlocking of a 80 mush suggests that the conditions of efficient mass transfer and mixing are easier to achieve than 81 previously thought. Conversely, it is adding constraints on rejuvenation scenarios based on the 82 emplacement of an underlying mafic gravity current (e.g. Bachmann and Bergantz, 2006; 83

Burgisser and Bergantz, 2011) by suggesting that underplating may require contrasts in densities
and/or viscosities to hinder fluidization.

86 Our capacity to interpret the various natural expressions of open-system events, such as eruptive products containing both the intruded magma and the resident mush, is hindered by our 87 88 partial understanding of the architectural end-members of these events, such as fluidization or underplating. To characterize the geometry and emplacement styles of intrusion events into a 89 residing mush, we performed numerical simulations using a combination of fluid mechanics and 90 91 discrete elements (Bergantz et al., 2015; Schleicher et al., 2016; Schleicher and Bergantz, 2017). 92 As the dissimilarities between the density and viscosity of the two melts require special attention to better characterize the end-member cases of open-system events, we explored how these 93 94 parameters condition the dynamics of the intruded material when injected into a mush. We first introduce the numerical model and the dimensionless parameters controlling recharge dynamics 95 that are varied in the simulations. Results of numerical simulations involving magmas of 96 97 contrasted physical properties are then presented in the framework of the dimensionless parameters. Finally, we relate our results to well-documented cases of eruptions triggered by an 98 intrusion event. 99

100

## 101 **2: Method**

102 In order to characterize the geometry and emplacement mechanism of intrusion in mush 103 accounting for granular dynamics, we performed Computational-Fluid-Dynamic and Discrete-

Element-Method (CFD-DEM) numerical simulations by using the MFIX-DEM software (https:// 104 mfix.netl.doe.gov/). Details about the theory and implementation of the model can be found in 105 106 Garg et al. (2012), Syamlal (1998), Syamlal et al. (1993), and validation of the DEM approaches in Garg et al. (2012) and Li et al. (2012) (see supplementary information 1 for a list of the 107 equations we used). To ensure stability and efficiency of the simulations, we used the composite 108 implicit force, which includes gravitational, pressure and drag forces, proposed by Burgisser et al. 109 (in review) instead of the usual numerical forces evaluations (Garg et al., 2012). The composite 110 force expression do not requires the use of time steps shorter than the characteristic durations of 111 the hydrodynamic processes accounted. As a result, the viscosity of the melt phases may be 112 increased without decreasing the simulation time step compared to that required to ensure the 113 stability of a dry (zero viscosity) granular simulations. 114

The computational domain is a 3D medium of  $1.6 \times 0.8 \times 0.05$  m (length  $\times$  height  $\times$ 115 116 width) filled with a resident mush (Fig. 1). This geometry also allowed us to populate the mush with mm-size particles, thereby ensuring a 1:1 scale compared to nature. We will show a 117 posteriori that our particle bed behaves identically to a bed twice as thick (Bergantz et al., 2015). 118 119 Our runs are thus representative of an open system event despite the small size of the domain compared to a natural system We used such geometry instead of a two dimensional one to ensure 120 that the build-up and breaking of force chains have a sufficient degree of freedom in space to 121 replicate best the mechanics of the granular phase. We created a mush layer of  $\sim 0.3$  m height 122 123 with an initial crystal content of  $\sim 0.64$  by simulating the settling of the particles in a vacuum and positioning them at the base of the domain. We used the same density for all particles ( $\rho_p = 3300$ 124

kg m<sup>-3</sup>) and three different diameters (4.5, 5, and 5.5 mm) to avoid artificial clustering. All 125 simulations use the same initial particle bed. A crystal-free magma is injected at the base of the 126 mush layer with a superficial vertical velocity,  $U_{ini}$ , through an inlet having a width,  $W_{ini}$ . The 127 128 density and the viscosity of the injected melt are kept constant between all the simulations (  $\rho_i = 2500 \text{ kg m}^{-3}$ ;  $\eta_i = 1 \text{ Pa s}$ , see table 2 for the list of the parameters kept constant). We used a 129 conduit of 3.2 cm in height to supply the inlet to ensure that the intruder enters the mush as a 130 Poiseuille flow. At the top of the domain, we used a pressure outflow boundary conditions to 131 ensure the overall mass conservation within the entire domain, which is consistent with an open-132 system event. The boundary conditions at the front and back of the domain are cyclical, which 133 134 means that the intruder corresponds to a dyke having one infinite dimension. All the other boundary conditions are non-slip walls (Fig 1). To maintain constant values of melt density and 135 viscosity during the runs (and hence constant density and viscosity contrasts), thermal effects are 136 ignored. This is consistent with the small dimensions of the computational domain that ensure run 137 times shorter than those allowing significant heat exchanges. 138

We performed simulations by varying the density and viscosity of the host melt. In order to compare simulations, we used dimensionless quantities to scale the effects of the contrasts in densities and viscosities, and injection velocities. The injection velocity and melt viscosity control the stress applied by the input of new materials to the mush. These parameters enter the minimum fluidization velocity,  $U_{mf}$  (Schleicher et al., 2016, see supplementary information 2 for derivation of  $U_{mf}$ ), which expresses the minimum superficial velocity required for the injection to entrain the host solids and generate the fluidization of the particle bed. As the injected melt

differs from the host melt, two minimum fluidization velocities can be calculated depending on which melt is considered. For all simulations, we used the minimum of these two velocities, which here always corresponds to that using the host melt properties. The dimensionless injection velocity,  $U^*$ , is defined as:

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$$U^* = \frac{U_{inj}}{U_{mf}}$$
 (1)

In simulations having identical  $U^*$ , the injection imposes the same stress to the overlying mush. However, the time needed to inject the same new melt volume changes between simulations because  $U_{mf}$  varies. We thus used a dimensionless time,  $t^*$ , to scale the simulation time (Bergantz et al., 2017):

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$$t^* = \frac{t U_{inj}}{H_{bed}},$$
 (2)

where *t* is the simulation time. In this way, simulations having identical  $t^*$  implies that the same volumes of intruder have been injected until that dimensionless time and simulation results can be compared directly. The density contrast between the two materials is scaled using the reduced buoyancy of the intruder. A negative reduced buoyancy indicates that the intruder is buoyant compared to the mush, whereas a positive one indicates a tendency to sink. Two reduced buoyancies may be defined. The first one,  $\rho^*$ , expresses the buoyancy contrast between the two melts:

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$$\rho^* = \frac{\rho_i - \rho_h}{\rho_i},\tag{3}$$

where  $\rho_i$  is the density of the intruded melt, and  $\rho_h$  is the host melt density. The second one,  $\rho_b^*$ , takes the presence of crystals in the host material into account and scales the bulk densities:

166 
$$\rho_b^* = \frac{\rho_i - \left(\rho_h (1 - \Phi) + \rho_p \Phi\right)}{\rho_i}, \qquad (4)$$

167 where  $\rho_p$  is the density of the host solids, and  $\Phi$  is the particle volume fraction. The viscosity 168 contrast,  $\eta^*$ , between the two melts is expressed as:

169 
$$\eta^* = \frac{\eta_h}{\eta_i},\tag{5}$$

170 where  $\eta_h$  is the host dynamic viscosity and  $\eta_i$  is that of the injected melt.

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## 172 **3: Results**

We performed 25 numerical simulations to explore the influence of the host melt density and viscosity (See Table 3 for a list of all the simulations and corresponding parameters). For these simulations, the injection velocities are such that the ratio with the respective minimum fluidization velocity,  $U^*$ , remains constant at  $U^*=21.2$ . This ratio is chosen to match that used previously in similar works (Schleicher et al., 2016; Schleicher and Bergantz, 2017) according to the formula presented in the supplementary material 2. We performed an additional 4 simulations at higher injection velocities to explore the effect of  $U^*$  on intrusion dynamics.

Figure 2 plots the simulations at the lowest  $U^*$ , 21.2, as functions of the dimensionless quantities  $\rho^*$ ,  $\rho_b^*$ , and  $\eta^*$ . It shows that the intrusions can be classified in three regimes as a function of the reduced buoyancy between the two melts,  $\rho^*$ . When  $\rho_i = \rho_h$ , the *fluidization* regime is observed. If  $\rho_i > \rho_h$ , the *spreading* regime occurs, whereas if  $\rho_i < \rho_h$ , the *rising* regime occurs (see next paragraph for a detailed description of the regime dynamics). The bulk density contrast  $\rho_b^*$  is always negative and the regime transition occurs at a value (-0.2025) of no particular physical significance. The three regimes do no depend on the viscosity contrast  $\eta^*$ .

The *fluidization* regime was observed in the simulations once  $\rho_i = \rho_h$ , and consists in the 187 development of a fluidized area above the inlet in which the intruded melt rises through the mush 188 (Fig. 3A-C), as described previously (Bergantz et al., 2015; Schleicher et al., 2016). The 189 fluidization of the mush is initiated by the dilation of the crystal framework to crystal volume 190 fraction below 0.3 above the inlet that locally destabilizes the forces chains network that supports 191 the bed and separates the crystals in contact. The fluidized volume grows vertically above the 192 inlet because of two mechanisms. The first is the upward entrainment of the particles localized 193 above the fluidized cavity, which results in bulging the top surface of the mush layer (Fig. 3A -194 C). The second mechanism is the progressive erosion of the crystals jammed at the boundary 195 between the mush and the fluidized volume. Once separated, crystals start settling in the fluidized 196 area because of this process of mush erosion, causing the fluidized area to ascend faster than the 197 198 intruded melt (green outline in Fig 3A-C). The intruder flows mainly vertically with a minor 199 lateral porous flow. When the fluidized cavity reaches the top of the particle bed, its width

progressively decreases to stabilize in the shape of a vertical chimney. At steady state, when  $t^*>1$ , the crystals located within the chimney show both upward and downward motions whereas the ones located around the chimney flow slowly in the direction of the inlet, forming a 'mixing bowl' as a whole, fully recovering the dynamics first described in Bergantz et al. (2015).

The *spreading* regime, which prevails in simulations once  $\rho_i > \rho_h$ , is characterized by the 204 lateral spreading of the injected melt similarly to a gravity current hugging the floor of the host 205 reservoir (Fig. 3D-F). The main difference with a pure fluid gravity current is that the melt is 206 progressively flowing across the mush as permeable flow. At the start of the injection, the crystal 207 framework experienced a dilation, which initiates host crystals settling in the same fashion as in 208 the *fluidization* regime. The lateral flow of the intruded melt is able to laterally entrain the host 209 210 crystals, creating two counter rotating granular vortexes in the residing mush with downward motions above the inlet (Fig. 3D-F). Such granular vorticity affects the flow pattern of the fluid 211 212 in the mush. The fluidized volume grows either predominantly laterally or vertically, depending on the relative importance between the lateral entrainment of the host solids by the intruder and 213 214 the vertical settling of the mush crystals. As the lateral propagation of the intruder progresses, so 215 does the size of the two granular vortexes, making this style of intrusion affect a larger mush volume than the *fluidization* regime. 216

The *rising* regime (Fig. 3G-I), is characterized by the ascent of the intruded melt within the mush that occurred in simulations once  $\rho_i < \rho_h$ . Runs start with the initial growth above the inlet of a cavity filled with the intruded fluid. The cavity becomes gravitationally unstable and ascends within the mush, forming a Rayleigh-Taylor instability. The ascent of the intruder

continues above the particle bed, entraining solids from the host. The instability is driven by its head because of the buoyant batch of intruded melt. This driving batch is surrounded by a volume of fluidized host mush (Fig. 3G-I). The dimensionless time at which the intrusion reaches the mush top ( $t^*\sim 0.3$ ) is shorter than that of the two other regimes because the Rayleigh-Taylor instability significantly accelerates the transport of the intruder.

Figure 2 suggests that the viscosity contrast does not control the end-member shape of the intruder flow. Larger viscosity contrasts, however, increase the trends of some aspects of mush dynamics. Figure 3 illustrates how viscosity bears on flow patterns.

In the *fluidization* regime, the increase of the host viscosity enhances the formation of 229 crystal-poor batches at the top of the intruded volume (Fig. 3A-C). Because the minimum 230 231 fluidization velocity within the intruded melt is lower than for the host, the crystals are not fluidized and sediment in the intruded melt to accumulate atop the inlet (Fig 3B-C). Because we 232 defined  $t^*$  to scale the dynamics of the mush, the increase of the host melt viscosity decreases the 233 injection velocity and the duration, t, required to reach the dimensionless time  $t^*=1$ . As a result, 234 increasing melt viscosity increases the ability for the intruded melt to experience lateral porous 235 flow through the host crystal frameworks (Fig. 3B-C). It also lengthens the time span for a 236 crystal to settle over the same characteristic distance between the intruded and host melts, which 237 results in the formation of the crystal poor volume at the top of the intruded volume (Fig. 3B-C). 238 The increase in the host melt viscosity, however, does not affect the volume of mush showing a 239 decrease in crystal volume faction and a distortion of the force chains. 240

In the spreading regime, high viscosity contrasts enhance the lateral spreading of the 241 intruder and the entrainment of the host crystals in the two counter rotating vortexes (Fig 3E-F). 242 Large host melt viscosity causes the lateral entrainment of the solids to be more efficient than 243 particle settling, which results in the elongation of the fluidized volume in the horizontal 244 direction. In the same fashion as in the *fluidization* regime, the lower superficial injection rate 245 enhances the ability of the lateral porous flow of the intruder. This effect is expressed by the 246 decrease of the thickness of the intruded layer with the increase of the host viscosity (Fig 3D-F). 247 It results that reaching the same volume of mush entrained by the intrusion requires less intruded 248 material as the viscosity of the host melt increases. 249

In the *rising* regime, increasing the viscosity contrast enlarges the vortexes sizes and the 250 separation distance between their centers (Fig 3G-I). The dimensionless time,  $t^*$ , at which the 251 intruder instability occurs decreases with the viscosity of the host. The volume of the intruded 252 253 melt driving the Rayleigh-Taylor instabilities is lower when a viscosity contrast exists. When a viscosity contrast is present, the volume of the intruded driving the instability does not vary 254 255 significantly (Fig 3H-I). The larger volume of the intruder driving the Rayleigh-Taylor instability can be addressed by the ratio between the dimensional injection rate and Rayleigh-Taylor 256 growing rate. In Fig. 3G, this ratio is higher than in Fig 3H–I, and a significant volume of fluid is 257 injected during the growth and entrainment of the instability. On the contrary, in Fig 3H–I, this 258 ratio is sufficiently small so that the amount of melt injected during the growth of the instability 259 260 is negligible compared to the volume required to initiate it. However, the volume of the mush

remobilized by the intruder flow does not significantly vary with the host melt viscosity (Fig.3G-I).

The additional 4 simulations in the spreading regime suggest that buoyancy effects 263 dominate the intruder flow up to  $U^* \simeq 10^5$ . Figure 4 shows the temporal evolution of the height 264 reached by the intruded volume,  $H^*$ , as a function of injection rate. All injections grow purely 265 vertically at first  $(t^* \le 0.1)$ . As seen above, at the low injection rate of 21.2, the intrusion stalls 266 rapidly and spreads laterally (simulation A25, Fig. 4). Increasing the injection rate causes stalling 267 to occur later and higher. When  $t^* > 0.2$ , injection growth switches from vertical to radial. When 268  $U^* > 10^5$ , the behavior of the intruder is dominated by the injection rate, which causes the radially 269 growing intrusion to reach the top of the bed at  $H^* = 1$ . Despite that all simulations have the same 270 271 intruder shape before stalling, the size of the region surrounding the intruder that is affected by dilatancy increases with  $U^*$ . The highest injection rate (simulation B4 with  $U^* = 10^6$ ) strictly 272 follows the theoretical curve for a radial growth and reaches  $H^*=1$  at  $t^*\approx 2.5$ , as predicted by 273 geometrical arguments (supplementary information 3). 274

The decoupling between the motions of the two phases results from processes unique to granular mechanics that our discrete numerical model is able to capture. Mush dilation is key for permeable melt flow to occur. The initiation of the intrusion increases the pore pressure in the mush around the inlet (Fig. 5A). This overpressure progressively propagates outwards and decreases the crystal volume fraction in the overlying mush (Fig. 5B). As the intrusion propagates, the effect of the overpressure is supplemented with the Reynolds dilatancy generated

by the granular vortexes in the mush (Fig 5C). The dilation of the solid framework increases its 281 permeability of the solid framework and in turn the possibility of relative motion between the 282 283 crystals and the interstitial melt (Fig. 5C). This phenomenon is particularly clear in the case of the rising regime. The intruder is surrounded by a volume of mush that underwent such dilation that 284 it is in the dilute regime. The contact region between the two magmas is dominated by melt-melt 285 286 interface interspersed with isolated crystals. As a result, entrainment is ruled by melt vorticity. Efficient entrainment of two fluids with a viscosity contrast occurs only when the most viscous 287 288 fluid bears large levels of vorticity (Jellinek and Kerr, 1999). In our runs, the intruder melt 289 viscosity is equal or less than that of the host, and the vorticity is concentrated close to or inside the intrusion (Fig. S4 in the supplementary information 4). This situation yields the weak 290 entrainment observed in the rising regime and the transition from vertical growth to spreading of 291 the intrusion melt as injection velocity decreases (Fig. 4). The concept of bulk reduced buoyancy 292 thus fails to predict the intrusion geometry for two reasons. First, it assumes the absence of 293 relative motion and thus ignores the transfer of crystals from host to intrusion. Second, in cases 294 when sufficient mush dilation occurs, entrainment is controlled by the melt-melt interface and 295 the associated density and viscosity contrasts. The interplay between pore pressure, dilation, melt 296 297 interface dynamics, and permeable flow controls the transport of mass within our modeled magmatic reservoir. 298

#### 4: Comparison with natural systems 299

To test the applicability of our results to natural cases, we gathered from the literature the 300 physical parameters of 15 eruptions involving the intrusion of new magma (Table S3-S4 in the 301 Preprint submitted to Earth and Planetary Science Letters 16

supplementary information 5). All host magmas are mushes but for a few cases that either have crystal gradients in their reservoirs (Krakatau), or for which there is ambiguity on the respective roles of the intruder and host magmas (Unzen, Minoan, and Katmai–Novarupta). In the studies surveyed, melt viscosity and melt density of host magmas were most often directly determined from eruptive products and pre-eruptive conditions such as pressure, temperature, and melt water content (details on how parameters were obtained are in Table S3–S4 (see supplementary information 5)).

The cases are organized into three categories depending on the observed eruptive 309 sequence. In the first category, the intruder was erupted first, followed by the emission of host 310 311 magma or a mixture of host and intruder. This category implies that the intruder magma was able to efficiently penetrate and pass through the host magma. In the second category, both host and 312 intruder magmas were erupted simultaneously, with the intruder most often forming enclaves or 313 314 mingling structures. The last category feature cases where the mixing was so thorough that the eruptive products only bear cryptic traces of the intruder, such as isolated intruder crystals 315 floating in the host or crystal disequilibrium textures. 316

Figure 6A shows the ratios of bulk viscosities and bulk densities between the intruder magma and the host magma(s) for the 15 eruptions. Figure 6A contains two physically meaningful thresholds, that of neutral buoyancy at the bulk density ratio of 0 and that of equal viscosity at the bulk viscosity ratio of one. The three types of eruptive sequence are not sorted following any of these thresholds. Figure 6B shows the same eruptions plotted as functions of melt properties instead of bulk properties. Our numerical runs cover the full range of natural

density ratios and a more restricted range of viscosity ratios (from 1 to  $10^2$  vs.  $10^{-1}$  to  $<10^4$  in nature). Figure 6B also shows the dividing line between rising and spreading dynamics at the level of neutral buoyancy with respect to the melts. With the possible exception of two cases (see *Discussion*), the Minoan eruption and the 1912 Katmai–Novarupta eruption, the *rising* regime is populated by the eruptions that first ejected intruder material. This divide between cases where at least some of the intruder magma had the capacity to go unscathed through the host and cases where none of it escaped from host interaction is consistent with our numerical results.

## 330 **5: Discussion**

Our results are helpful to predict the behavior of an intrusion within a mush. The reduced 331 buoyancy between the two melts,  $\rho^*$ , is the parameters having a first order control on the 332 333 geometry of the intrusion. On the contrary, the commonly used level of neutral bulk buoyancy (e.g. Huppert et al., 1986; Snyder and Tait, 1995) does not mark any particular change in 334 dynamic behavior (Fig. 2). This result illustrates that the relative motion between the solids and 335 surrounding melt is of primary importance when studying mush processes. Experiments, or 336 numerical simulations, that account of the presence of the solids or exsolved volatiles as discrete 337 entities (Barth et al., 2019; Bergantz et al., 2015; Girard and Stix, 2009; Hodge et al., 2012; 338 339 McIntire et al., 2019; Michioka and Sumita, 2005; Parmigiani et al., 2014; Schleicher et al., 2016; 340 Schleicher and Bergantz, 2017) are the most likely to faithfully reproduce mush dynamics. 341 Neglecting phase decoupling by considering the magma as a single-phase fluid having effective properties such as bulk density or bulk viscosity will not capture the blending of crystal contents 342 between host and intruder and the simultaneous but independent evolution of the melt-melt 343

interface (Fig. 5C). This sheds light on the importance of granular mechanisms such as porepressure, dilatancy and permeable flow in shaping the end-member cases of mush intrusion.

We characterized the parameter ranges of a series of well-documented cases of eruptions 346 that features magma mixing, focusing on the densities and viscosities of the two end-member 347 348 magmas involved and on the order of the eruptive sequence. Two cases, Katmai and the Minoan eruption, straddle two eruptive sequence categories because the intruders may have been 349 350 transported alongside (as opposed to through) the host magmas. Both cases are close to the 351 neutral buoyancy level, regardless of the scenario considered (Fig. 6B). Importantly, each 352 individual scenario is consistent with our regimes. The Katmai eruption first emitted rhyolite. The Katmai scenario corresponding to a rhyolite intruding a more mafic host (Eichelberger and 353 354 Izbekov, 2000) is consistent with it being located in the *rising* regime. In the other scenario (Singer et al., 2016), the rhyolite is part of the host reservoir, which is consistent with that 355 scenario being in the spreading regime. The Minoan scenario located in the rising regime 356 (Cadoux et al., 2014) would have indeed emitted the intruder first, but it feature a host filled by 357 low-crystallinity magma, which is at odds with our hypothesis that the host is in a mush state. 358 359 The other Minoan scenario (Druitt, 2014; Flaherty et al., 2018; Martin et al., 2010) involves a mushy host compatible with this hypothesis and is consistent with the spreading regime that 360 hinders first emission of the intruder. The overall good agreement between the observed eruptive 361 sequences and our numerical results (Fig. 6B) constitutes a serious argument in favor of the fact 362 that open-system events are, to first order, controlled by the density contrast between the melt 363

phases of the intrusion and mush. It also suggests that injection momentum was quicklyexhausted, letting buoyancy control the unfolding of the event.

Two special natural cases can be added to the comparison between our dynamics regime 366 and natural data (Fig. 6B). The first is the 1883 eruption of Krakatau volcano (Mandeville et al., 367 368 1996), which resulted from remobilization by basaltic intruder of a stratified magma chamber 369 featuring three compositions, none of them being in a mush state (andesite, dacite, and rhyodacite). Evidence that the basalt intruder was erupted first comes from basaltic ashes 370 371 collected during the first phase of the eruption (Self, 1992). The presence of several magmas in the host reservoir, however spatially distributed, causes a large uncertainty in the host properties. 372 As a result, the Krakatau eruption spans the divide between the regimes established by our 373 simulations (Fig. 6B). It is thus an inconclusive case where the intruder was erupted first. The 374 second natural case is the 1991–1995 eruption of Unzen volcano, for which the intruder could 375 376 have been either andesitic (Holtz et al., 2004), or basaltic (Browne et al., 2006). Regardless of its composition, the intrusion caused thorough mixing and the first magma erupted was the product 377 of this mixing. If the intruder was basaltic, it was buoyant with respect to the felsic host and if it 378 379 was andesitic, it was denser that the host. As a result, Unzen spans the divide between the *rising* and *spreading* regime (Fig. 6B). Considering that the intruder input was large (>30 wt% of the 380 eruptive products; Holtz et al., 2005), and if any credit is given to our inferences, the intruder was 381 more likely to be andesitic than basaltic because this latter composition would have been prone to 382 383 preserve its integrity while going through the host mush, erupting first.

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## 385 6: Conclusions

386 This study highlights the importance of granular mechanics in mush processes, which differ significantly from ones expected with purely fluid models. As expected, our simulations 387 show that when the injection velocity is high  $(U^* > 10^5)$ , intrusion dynamics is dominated by the 388 injection momentum and the intruded cavities grow radially. When the injection velocity is below 389 390 this threshold, however, buoyancy controls the behavior of the intruder in an unexpected way. Bulk buoyancy contrasts appear to play no role in the way the intruder flows. Instead, the density 391 contrast between the host and intruded melts exerts a first-order control on the architecture of an 392 393 intrusion event in a mush. When the two melt densities are identical, the intruder fluidizes the mush and creates a mixing bowl, as described in Bergantz et al. (2015). When the intruded melt 394 395 is lighter than that of the host, it rises through the mush. Mush dilation around the intruder causes the contact region between the two magmas to be dominated by melt-melt interface interspersed 396 with isolated crystals. Entrainment in this rising regime is ruled by the amount of vorticity of the 397 most viscous melt. As our in our runs the intruder melt viscosity was equal or lower than that of 398 the host, no entrainment was observed. Intruder melts denser than the host spread laterally partly 399 as permeable flows through the host mush. The lateral spreading of the intruder generates two 400 401 counter rotating granular vortexes with downward motions above the inlet, which maximizes the volume of the mush entrained by the gravity current. In this spreading regime, the combined 402 effects of the initial pore overpressure at the inlet and the Reynolds dilatancy resulting from the 403 404 lateral spreading of the intruder are able to fluidize the overlying mush.

We tested whether the first-order effect of melt density contrast was expressed in nature. We tallied 15 well-documented eruptive sequences, classifying them according to the expected outcomes of the three dynamic regimes we defined. We found overall good agreement between eruption sequences and our model predictions, which suggests that granular mechanisms such as pore pressure, dilatancy, and permeable flow play a fundamental role in the unfolding of opensystem events. Granular dynamics and the decoupling of melt and crystals are thus key in shaping reservoir and volcanic processes.

412

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## 560 Tables:

Symbol (unit)	Definition
$d_{p}(m)$	Particle diameter
<u> </u>	Particle Young modulus
$\overline{F_{CDD}}(N)$	Gravity-Pressure-Drag force
$\vec{q}$ (m s <sup>-2</sup> )	Gravity acceleration vector
$\overline{H}_{hed}$ (m)	Particle bed thickness
H <sub>max</sub> (m)	Intruded layer maximum height above the inlet
$\overline{H^*}$	Dimensionless height of the intruded volume
$m_{\rm n}$ (kg)	Particle mass
P (Pa)	Fluid pressure
R (m)	Intruder batch radius
	Reduced time
$\overline{U_{ini}}$ (m s <sup>-1</sup> )	Injection superficial velocity
$U_{mf}$ (m s <sup>-1</sup> )	Minimum fluidization superficial velocity
$\overline{U^*}$	Dimensionless injection velocity
$\vec{V}_f$ (m s <sup>-1</sup> )	Fluid velocity vector
$\overline{V_n}$ (m s <sup>-1</sup> )	Particle velocity vector
$W_{ini}$ (m)	Injection width
$\rho_f (\text{kg m}^{-3})$	Fluid density
$\eta$ (Pa s)	Fluid dynamic viscosity
 τ <sub>ν</sub> (s)	Particle viscous response time
$\beta$ (kg s <sup>-1</sup> )	Momentum transfer coefficient
$\Delta t$ (s)	DEM time step
η (Pa s)	Fluid dynamic viscosity
$\eta_i$ (Pa s)	Intruder melt dynamic viscosity
$\eta_h$ (Pa s)	Host melt dynamic viscosity
n n	Melts dynamic viscosity ratio
μ	Particle friction coefficient
$\rho_h$ (kg m <sup>-3</sup> )	Host melt density
$\rho_i (\text{kg m}^3)$	Intruder melt density
$\rho_n (\text{kg m}^3)$	Average density of the particles
	Melts reduced buoyancy
	Melts bulk reduced buoyancy
	Poisson coefficient
$\overline{\tau_{v(s)}}$	Particle viscous response time
$\Phi$	Solid volume fraction

## 561 Table 1: List of symbols and their meaning

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Parameter	Value or range
$\rho_p$	3300 kg m <sup>-3</sup>
$d_{p}$	4.5-5.5 mm
Nb crystals	208495
H <sub>bed</sub>	0.3 m
W <sub>ini</sub>	0.1 m
$\rho_i$	2500 kg m <sup>-3</sup>
$\eta_i$	1 Pa s
Ε	2 10 <sup>7</sup> Pa
Ø	0.32
μ	0.3

#### 563 Table 2: Parameters kept constant during the parametric study

Run nb.	$ ho_h$ (kg m <sup>-3</sup> )	$ ho_{b}(host)$ (kg m-3)	ρ*	$\rho_h^*$	$\eta_h$ (Pa s)	$U_{mf}$ (m s <sup>-1</sup> )	U <sub>ini</sub> (m s <sup>-1</sup> )
A1	2500	3012	0	-0.2048	1	2.956 10-4	6.268 10-3
A2	2500	3012	0	-0.2048	5	5.913 10-5	1.254 10-3
A3	2500	3012	0	-0.2048	10	2.957 10-5	6.268 10-4
A4	2500	3012	0	-0.2048	50	5.913 10-6	1.254 10-4
A5	2500	3012	0	-0.2048	100	2.957 10-6	6.268 10-5
A6	2450	2994	0.02	-0.1976	1	3.141 10-4	6.660 10-3
A7	2450	2994	0.02	-0.1976	5	6.283 10-5	1.332 10-3
A8	2450	2994	0.02	-0.1976	10	3.141 10-5	6.660 10-4
A9	2450	2994	0.02	-0.1976	50	6.283 10-6	1.332 10-4
A10	2450	2994	0.02	-0.1976	100	3.141 10-6	6.660 10-5
A11	2550	3030	-0.02	-0.212	1	2.772 10-4	5.876 10-3
A12	2550	3030	-0.02	-0.212	5	5.544 10-5	1.175 10-3
A13	2550	3030	-0.02	-0.212	10	2.772 10-5	5.876 10-4
A14	2550	3030	-0.02	-0.212	50	5.544 10-6	1.175 10-4
A15	2550	3030	-0.02	-0.212	100	2.772 10-6	5.876 10-5
A16	2200	2904	0.12	-0.1616	1	4.065 10-4	8.618 10-3
A17	2200	2904	0.12	-0.1616	5	8.130 10-5	1.724 10-3
A18	2200	2904	0.12	-0.1616	10	4.065 10-5	8.618 10-4
A19	2200	2904	0.12	-0.1616	50	8.130 10-6	1.724 10-4
A20	2200	2904	0.12	-0.1616	100	4.065 10-6	8.618 10-5
A21	2150	2886	0.14	-0.1544	1	4.250 10-4	9.010 10-3
A22	2150	2886	0.14	-0.1544	5	8.500 10-4	1.802 10-3

Run nb.	$ ho_h$ (kg m <sup>-3</sup> )	$ ho_b(host)$ (kg m <sup>-3</sup> )	ρ*	$\rho_{b}^{*}$	$\eta_h$ (Pa s)	$U_{mf}$ (m s <sup>-1</sup> )	U <sub>ini</sub> (m s <sup>-1</sup> )
A23	2150	2886	0.14	-0.1544	10	4.250 10-5	9.010 10-4
A24	2150	2886	0.14	-0.1544	50	8.500 10-6	1.802 10-4
A25	2150	2886	0.14	-0.1544	100	4.250 10-6	9.010 10-5
B1	2150	2886	0.14	-0.1544	100	4.250 10-6	4.250 10-3
B2	2150	2886	0.14	-0.1544	100	4.250 10-6	4.250 10-2
B3	2150	2886	0.14	-0.1544	100	4.250 10-6	4.250 10-1
B4	2150	2886	0.14	-0.1544	100	4.250 10-6	4.250 10°

564 Table 3: List of the simulation performed for this chapter and corresponding variables.





Figure 1: Simulations initial condition. [A] The drawing represents the computational domain 566 viewed from the front. The medium is composed by rectangular box, which is fed by a conduit at 567 its based. Particles are settled to generate a particle bed having a thickness  $H_{bed}$ . The background 568 colors indicates which fluid is present initially in the computational domain. The blue color 569 corresponds to the host melt and the green color to the intruded melt. The red arrows below the 570 conduit represent the velocity profile of the injected fluid (Poiseuille flow). The arrows atop the 571 domain indicate that the boundary condition is a fixed pressure outflow. The hatched walls 572 indicate non-slip boundary conditions. [B] Side view of the computational domain. The green 573 dashed lines indicate that cyclical boundary conditions are used for these walls. The dotted circles 574 indicate particles overlapping with one of the two cyclical boundary conditions and that are also 575 considered to be present on the opposite side. 576

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**Figure 2:** Regime diagram of intrusion behavior for  $U^*=21.2$ . The diagram represents the positions of the simulations A1–25 as functions of the reduced buoyancy (abscissa) and viscosity ratios (ordinate). Each square represents a simulation. Square colors depend on the observed regime (blue=rising; black=fluidization; red=lateral spreading). Similarly, the background color interpolates the observed regimes (blue= rising; red=lateral spreading) and the vertical dashed line interpolates where the fluidization is expected to prevail.

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**Figure 3:** Comparison of the effects of buoyancy and viscosity contrasts. Each section represents the advancement of the simulation at  $t^*=1$  (or when the rising instability is above the particle bed). The injected melt contours are indicated with green curves. The dashed black arrows indicate the presence and direction of granular flows. The thin white curves indicate the fluid streamlines with small arrowheads indicating flow direction.





**Figure 4:** Evolution of the height,  $H^*$ , of the intruded volume as a function of the dimensionless time  $t^*$ . Each square represents the height of the top of the intruded volume measured in the simulations. Square colors indicate injection rate. Dashed lines indicate the theoretical intruder front height evolution in the case of vertical propagation (supplementary information 3) The black curve is the theoretical front height for a radial growth, and the horizontal dotted lines

indicate the front height evolution during lateral spreading. The three insets illustrate intrusionbehaviors.



**Figure 5:** Evolution of the pore pressure and crystal volume fraction. On each inset, the color depend on the difference between the local crystal volume fraction,  $\Phi$ , and the maximum one,  $\Phi_{max}$  ( $\Phi_{max}$ =0.64), in a logarithmic scale. The overpressure respect to the initial hydrostatic pressure field is indicated with contour that corresponds to the isosurfaces where the overpressure are equal to 5, 25, 50, and 100 Pa. The pink dashed curves represent the boundary between the

611 injected and resident melt. Inset [A] and [B] are captured after 1s and 6s. Both only displayed the
612 portion of the mush layer that present overpressure and dilation. Inset [C] is acquired after 45s
613 and cover a slice of the entire computational domain. The two dashed rectangle indicate the
614 extend of insets [A] and [B].



617 Figure 6: [A] Ratios of bulk properties for the host and intruder magmas involved in 15 eruptions. The bulk viscosity ratio is that of the host over that of the intruder and the bulk density 618 ratio is that of the difference between the intruder and the host over that of the intruder. Eruptions 619 are sorted according to whether the intruder magma was erupted first ("First"), at the same time 620 621 as (or mixed with) the host ("Together"), or fully mixed with the host ("Cryptic"). [B] Ratios of melt properties for the host and intruder magmas involved in 15 eruptions. The melt viscosity 622 ratio is that of the host over that of the intruder and the melt density ratio is that of the difference 623 between the intruder and the host over that of the intruder. Eruptions are sorted according to 624 whether the intruder magma was erupted first ("First"), at the same time as (or mixed with) the 625 host ("Together"), or fully mixed with the host ("Cryptic"). The gray area covers the runs done in 626 this study and the cross marks the parameters used in the numerical study of Bergantz et al. 627 (2015). See text for details regarding the special cases of Unzen and Krakatau. 628

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# 632 Supplementary Information 1:

This Supplementary Information includes two tables summarizing the equation systemsolved in our numerical simulations (Tables S1–S2).

Equation names	Equations	Ref.
Mass conservation	$\frac{\partial \varepsilon_f}{\partial t} + \nabla \cdot (\varepsilon_f  \vec{v}_f) = 0$	1
Momentum conservation	$\rho_f \left( \frac{\partial}{\partial t} (\varepsilon_f  \vec{v_f}) + \nabla \cdot (\varepsilon_f  \vec{v_f} \otimes \vec{v_f}) \right) = \nabla \cdot (\sigma_f) + \varepsilon_f  \rho_f  \vec{g} + \vec{I_f}$	1
Stress tensor	$\dot{\sigma_f} = P_f \delta_{ij} + \frac{2}{3} \eta_f tr(\dot{\epsilon_f}) \delta_{ij} + 2 \eta_f \dot{\epsilon_f}$	1
Euler velocity integration	$\vec{v_p}^{(k)}(t+\Delta t) = \vec{v_p}^{(k)}(t) + \Delta t \frac{\vec{F_{GPD}}^{(k)}(t) + \sum_{l=1}^{N_t^{(k)}} \left(\vec{F_C}^{N(k,l)}(t) + \vec{F_C}^{T(k,l)}(t)\right)}{m^{(k)}}$	Eq. (4.4)
Euler displacement integration	$\overrightarrow{X}_{p}^{(k)}(t+\Delta t) = \overrightarrow{X}_{p}^{(k)}(t) + \Delta t  \overrightarrow{v}_{p}^{(k)}(t+\Delta t)$	2
Euler rotation integration	$\overrightarrow{\omega_{p}^{(k)}}(t+\Delta t) = \overrightarrow{\omega_{p}^{(k)}}(t) + \Delta t \frac{\sum_{l=1}^{N_{l}^{(k)}} \left(\overrightarrow{T_{C}^{(k,l)}} + \overrightarrow{T_{L}^{(k,l)}}(t)\right)}{I^{(k)}}$	2
Normal contact force	$\overline{F_{c}^{N(i,j)}(t)} = \left(-k_{n}^{(i,j)}(t)\delta_{n}^{(i,j)}(t) + \eta_{n}^{(i,j)}(t)\Delta\overline{V_{p}^{N(i,j)}(t)}\right)\overrightarrow{n_{ij}}$	25
Tangential contact force	$\overrightarrow{F_c}^{T(i,j)}(t) = -k_t^{(i,j)}(t)\delta_t^{(i,j)}(t) + \eta_t^{(i,j)}(t)\overrightarrow{\Delta V_p}^{T(i,j)}(t)$	2 5
Collisional torque	$\vec{T}_{c}^{(i,j)}(t) = \frac{d_{p}^{(i)} - \delta_{n}^{(i,j)}(t)}{2} \vec{F}_{c}^{T(i,j)}(t); \vec{T}_{c}^{(j,i)}(t) = \frac{d_{p}^{(j)} - \delta_{n}^{(i,j)}(t)}{2} \vec{F}_{c}^{T(i,j)}(t)$	2
normal spring (Hertzian model)	$k_{n}^{(i,j)}(t) = \frac{4}{3} \frac{E^{(i)} E^{(j)} \sqrt{R_{eff}^{(i,j)}}}{E^{(j)} (1 - \sigma^{(i)2}) + E^{(i)} (1 - \sigma^{(j)2})} \delta_{n}^{(i,j)\frac{1}{2}}(t)$	2
tangential spring (Hertzian model)	$k_{t}^{(i,j)}(t) = \frac{16}{3} \frac{G^{(i)}G^{(j)}\sqrt{R_{eff}^{(i,j)}}}{G^{(j)}(2-\sigma^{(i)}) + G^{(i)}(2-\sigma^{(j)})} \delta_{t}^{(i,j)\frac{1}{2}}(t)$	2

635 **Table S1:** List of the equations implemented in the CFD-DEM model

Equation names	Equations	Ref.
Elastic modulus	$G = \frac{E}{2(1+\sigma)}$	2
Normal damping coefficient	$\eta_{n}^{(i,j)}(t) = \frac{2\sqrt{m_{eff}^{(i,j)}k_{n}^{(i,j)}(t)}  \ln e_{n} }{\sqrt{\pi^{2} + \ln^{2} e_{n}}} \delta_{n}^{(i,j)}(t)^{\frac{1}{4}}$	2 5
Tangential damping coefficient	$\eta_t^{(i,j)} = \frac{2\sqrt{m_{eff}^{(i,j)} k_t^{(i,j)}(t)}  \ln e_t }{\sqrt{\pi^2 + \ln^2 e_t}} \delta_t^{(i,j)}(t)^{\frac{1}{4}}$	2 5
effective radius	$R_{eff}^{(i,j)} = \frac{2\left(d\left p^{(i)} + d_{p}^{(j)}\right)}{d_{p}^{(i)}d_{p}^{(j)}}$	2
Effective mass	$m_{eff}^{(i,j)} = \frac{m^{(i)} + m^{(j)}}{m^{(i)}m^{(j)}}$	2
Solids/Fluid momentum exchange on REV	$\vec{I}_{f}(t) = \frac{1}{\mathbf{v}_{REV}} \sum_{k=1}^{N_{k}} \vec{F}_{D}^{(k)}(t) K_{REV}(X_{p}^{(k)})$	2
Drag forces (for the fluid)	$\overline{F}_{D}^{(k)}(t) = -\nabla P_{f}(t) \left(\frac{\pi}{6} d_{p}^{(k)3}\right) + \frac{\beta_{fs}^{(k)}(t)}{\left(1 - \varepsilon_{f}(t)\right)} \left(\frac{\pi}{6} d_{p}^{(k)3}\right) \left(\overrightarrow{v_{f}}(t) - \overrightarrow{v_{p}}^{(k)}(t)\right)$	2
Local fluid/solid momentum transfer	$\beta_{fs}^{(k)}(t) = \begin{cases} \frac{3}{4} C_{D}^{(k)}(t) \frac{\rho_{f} \varepsilon_{f}(t) (1 - \varepsilon_{f}) \  \vec{v}_{f} - \vec{v}_{s}^{(k)} \ }{d_{p}^{(k)}} \varepsilon_{f}^{-2.65} \varepsilon_{f} \ge 0.8 \\ \frac{150 (1 - \varepsilon_{f}(t))^{2} \eta_{f}}{\varepsilon_{f}(t) d_{p}^{(k)2}} + \frac{1.75 \rho_{f} (1 - \varepsilon_{f}(t)) \  \vec{v}_{f}(t) - \vec{v}_{s}^{(k)}(t) \ }{d_{p}^{(k)}} \varepsilon_{f}^{(k)} \end{cases}$	3 4
Drag coefficient	$C_{D}^{(k)}(t) = \begin{cases} \frac{24}{Re^{(k)}(t)(1+0.15 Re^{(k)}(t)^{0.687})} Re^{(k)}(t) < 1000\\ 0.44 Re^{(k)}(t) \ge 1000 \end{cases}$	34
Particle Gravity-Drag- Pressure force	$\overline{F}_{GPD}(t) = \frac{m_p}{\Delta t} \left( \vec{v}_f + \tau_v \left( \vec{g} - \frac{\nabla P}{\rho_p} \right) - \vec{v}_p(t) \right) \left( 1 - e^{\frac{-\Delta t}{\tau_v}} \right)$	Eq. (4.5)
Reynolds number	$Re^{(k)}(t) = \frac{d_m^{(k)} \ \vec{v_f}(t) - \vec{v_s}^{(k)}(t)\  \rho_f}{\eta_f}$	3

636

<sup>&</sup>lt;sup>1</sup> Syamlal et al., (1993)

- 637 <sup>2</sup> Garg et al., (2010)
- 638 <sup>3</sup> Benyahia et al., (2012)
- 639 <sup>4</sup> Gidaspow, (1986)
- 640

## 641 **Table S2 :** Symbols used in Table S1

Symbol	Definition
$C_D^{(k)}$	Drag coefficient of the $k^{\rm th}$ particle
$m{d}_{p}^{(i)}$	i <sup>th</sup> particle diameter
$e_n$	Particle normal restitution coefficient
$e_t$	Particle tangential restitution coefficient
$oldsymbol{E}^{(i)}$	i <sup>th</sup> particle Young modulus
$\overrightarrow{F}_{C}^{N(k,l)}$	Normal contact force between $k^{^{th}}$ particle and its $l^{^{th}}$ neighbor
$\overrightarrow{F}_{C}^{T(k,l)}$	Tangential contact forces between $k^{\mbox{\tiny th}}$ particle and its $l^{\mbox{\tiny th}}$ neighbor
$\overline{F}_{D}^{(k)}$	Drag force on k <sup>th</sup> particle
$\vec{g}$	Gravitational vector (m s <sup>-2</sup> )
$oldsymbol{G}^{(oldsymbol{k})}$	k <sup>th</sup> particle shear moduli
$m{h}^{(i,j)}$	Distance between i <sup>th</sup> and j <sup>th</sup> particles edges
$\vec{I}_f$	Fluid-solid momentum exchange
$oldsymbol{I}^{(oldsymbol{k})}$	k <sup>th</sup> particle moment of inertia
$K_{REM}$	Generic kernel to determine the influence of a particle located at $\overrightarrow{X}_p^{(k)}$ on the REV
$k_n^{(i,j)}$	Normal spring coefficient between $i^{\mbox{\tiny th}}$ and $j^{\mbox{\tiny th}}$ particles contact
$k_t^{(i,j)}$	Tangential spring coefficient between $i^{\text{th}}$ and $j^{\text{th}}$ particles contact
l	Neighbors index
$m{m}^{(m{k})}$	k <sup>th</sup> particle mass
$m_{e\!f\!f}^{(i,j)}$	$i^{th}$ and $j^{th}$ particles effective radius

$oldsymbol{N}_l^{(k)}$	Number of neighbors of the k <sup>th</sup> particle
$N_k$	Number of particles
$\vec{n}_{ij}$	Normal vector between i <sup>th</sup> and j <sup>th</sup> particles
$P_{f}$	Fluid pressure (Pa)
REV	Representative elementary volume
$Re^{(k)}$	i <sup>th</sup> particle Reynolds number
$R_{e\!f\!f}^{(i,j)}$	i <sup>th</sup> and j <sup>th</sup> particles effective radius
$R^{(i,j)}_{\square}$	Contact area radius between $i^{\mbox{th}}$ and $j^{\mbox{th}}$ particles
$\overrightarrow{T}_{C}^{(k,l)}$	Contact torque between $k^{\text{th}}$ particle and its $l^{\text{th}}$ neighbor
$\overrightarrow{T}_{L}^{(k,l)}$	Lubrication torque between $k^{^{th}}$ particle and its $l^{^{th}}$ neighbor
$\vec{v}_f$	Fluid velocity vector (m s <sup>-1</sup> )
$\overrightarrow{\boldsymbol{v}_{p}}^{(k)}$	$k^{th}$ particle velocity vector (m s <sup>-1</sup> )
$\overrightarrow{X}_{p}^{(k)}$	k <sup>th</sup> particle position (m)
$oldsymbol{eta}_{\mathit{fs}}^{\scriptscriptstyle{(k)}}$	k <sup>th</sup> particle – fluid momentum transfer coefficient
$\Delta V_p^{N(i,j)}$	Normal relative velocity between i <sup>th</sup> and j <sup>th</sup> particles
$\Delta V_p^{T(i,j)}$	Tangential relative velocity between $i^{\mbox{th}}$ and $j^{\mbox{th}}$ particles
${oldsymbol{\delta}}_{\scriptscriptstyle ij}$	Kronecker tensor
$\delta_n^{(i,j)}$	Normal overlap between $i^{\mbox{th}}$ and $j^{\mbox{th}}$ particles
${\boldsymbol \delta}_t^{\scriptscriptstyle (i,j)}$	Tangential displacement during the contact between $i^{\mbox{th}}$ and $j^{\mbox{th}}$ particles contact
ε	Roughness distance below which lubrication is ineffective (m)
$\varepsilon_{f}$	Fluid volume fraction
$\epsilon_{f}$	Fluid strain rate tensor
$\eta_f$	Fluid viscosity (Pa s)
$\eta_n^{(i,j)}$	Normal damping coefficient between $i^{\text{th}}$ and $j^{\text{th}}$ particles
$\eta_t^{(i,j)}$	Tangential damping coefficient between $i^{\mbox{\tiny th}}$ and $j^{\mbox{\tiny th}}$ particles

v	Domain volume (m-3)
$\rho_{f}$	Fluid density (kg m <sup>-3</sup> )
$oldsymbol{\sigma}^{(i)}$	i <sup>th</sup> particle Poisson coefficient
$\acute{\sigma_f}$	Fluid stress tensor
$ec{\omega}_{p}^{(k)}$	k <sup>th</sup> particle rotation vector (rad s <sup>-1</sup> )
$\Delta$	Nabla operator
8	Outer product

642

643

## 644 Supplementary Information 2:

645 This supplementary information presents an updated derivation of the minimum 646 fluidization velocity compared to those used in the literature.

647 The onset of fluidization of a crystal bed occurs when the upward drag force exerted by 648 the injected fluid exceed its net weight. Shi et al. (1984) proposed a formula to predict the 649 minimum fluidization velocity of a random packed bed due to a localized injection of fluid. These authors made the assumption that the fluid velocity is only vertical and uniformly distributed on 650 horizontal cross-sectional area (Fig. S1). The total upward drag force is computed with the 651 652 Ergun's formula (Ergun, 1952) for a bed fluidized uniformly. Later, Cui et al. (2014) adapted this 653 formula by considering the fluid velocity uniform along a semi-circular cross sectional area. Here, we modify the approach of Cui et al. (2014) to predict the minimum fluidization velocity in 654 655 the experimental apparatus geometry because the original derivation incorrectly assumed the 656 distance between the injection point and center of the inlet,  $r_0$ , and the boundaries of the 657 integral in their Eq. (13).

658 The total upward drag force applied by the inlet on the particle bed is computed as:

659 
$$F_D = \int_{r_0}^{H+r_0} \left( A U_r + B U_r^2 \right) S(r) dr,$$
 (S1)

660 where  $r_0$  correspond of the vertical coordinates of the bottom and  $H+r_0$  is the position of the 661 top of the particle bed. The variable *r* corresponds to the radial distance from a hypothetic 662 injection point (Fig. S1). *A* and *B* are given by Ergun (1952):

663 
$$A = 150 \frac{\phi^2}{(1-\phi)^3} \frac{\eta_f}{d_p^2},$$
 (S2)

664 
$$B=1.75 \frac{\phi}{(1-\phi)^3} \frac{\rho_f}{d_p}$$
 (S3)

665 S(r) represents the area of the curved surface on which the fluid velocity is uniform, and it is 666 computed as a function of r as:

$$667 \quad S(r) = 2 \alpha (r + r_0) W_1. \tag{S4}$$

 $U_r$  is the fluid velocity at a radial distance r.  $U_r$  may be computed by considering that the injected flux is conserved through the particle bed height, which yields:

$$670 \quad Q_{inj} = U_r S(r), \tag{S5}$$

671 and, with (S4):

672 
$$U_r = \frac{Q_{inj}}{2\alpha (r+r_0) W_l}$$
 (S6)

673 Substituting Eqs. (S6) and (S4) into Eq. (S1) yields:

674 
$$F = AQ_{inj}H_0 + \frac{BQ_{inj}^2}{2\alpha W_l}\ln\left(\frac{H_0 + 2r_0}{2r_0}\right)$$
 (S7)

675 In this geometry, the net weight of the bed, W, is given by:

676 
$$W = \left[ (r_0 + H_0)^2 \tan \alpha - \frac{W_{inj} r_0}{2} \right] W_l (\rho_p - \rho_f) g \phi.$$
 (S8)

677 Introducing  $r_0 = W_{ini}/(2 \tan \alpha)$ , the onset of fluidization occurred when F = W, which yields:

678 
$$AQ_{inj}H_0 + \frac{BQ_{inj}^2}{2\alpha W_l} \ln\left(\frac{2\tan\alpha}{W_{inj}} + 1\right) - \left[H_0(W_{inj} + H_0\tan\alpha)\right] W_l(\rho_p - \rho_f)g\phi = 0$$
(S9)

Figure S2 displays comparison of the minimum fluidization velocities computed with formulas from Ergun (1952), Shi et al. (1984), Cui et al., (2014), and Eq. (S9), function of the particle bed height. It shows that Eq (S9) is closer to the result predicted with the formulas from Ergun (1952) and Shi et al. (1984). The incorrect formula derived by Cui et al., (2014) results in the significant overestimations of the minimum fluidization velocity.

684



685	Figure S1: Conceptual framework to derive the minimum fluidization velocity. The top draw is a
686	view from the top. The bottom draw is a front view. On both draws, the thick black lines
687	represent the boundaries of the volume of the particle bed, which is fluidized. The red dashed
688	curves indicate the cross sectional areas where the magnitude of the fluid velocity is uniform.
689	The arrows represent the direction of the fluid flow. The black dots represent the positions of
690	the theoretical injections point and intersections between the cross sectional areas where the
691	fluid velocity is uniform and the vertical boundary of the fluidized particle bed.



697 Figure S2: Comparison of the minimum fluidization velocities function of the initial particle bed
698 height. The curves represent the minimum fluidization velocities derived by authors and the one
699 given here.

700

701

## 702 Supplementary Information 3:

This supplementary information presents the derivation of the maximum height of the intrusion as a function of the time for end member scenarios.

We consider two end-members for the growth of the intrusion volume (vertical or radial). The first end member considers the vertical ascent (dyking) of the intruded melt above the inlet over a width,  $W_{inj}$ . In this case, the ratio,  $H^*$ , between  $H_{max}$  and the initial particle bed thickness,  $H_{bed}$  ( $H^* = H_{max}/H_{bed}$ ), reads:

709 
$$H^* = t^*$$
. (S10)

In the case of radial growth, we consider as spherical intrusion having a unknown radius, R, and fed by an inlet of width  $W_{inj}$  (Fig. S3). The inlet truncates the sphere at a vertical distance, h, which depends on both R and  $W_{inj}$ . The objective is to compute the distance from the inlet to the top of the sphere, H, knowing the area A and injection width  $W_{inj}$ . The total area,  $A_{tot}$ , of the sphere is the sum of the area A, where the intruded fluid is present and the truncated area B as:

$$716 \quad A_{tot} = A + B. \tag{S11}$$

The area *A* depends on injection velocity and time. The area  $A_{tot}$  may be expressed using the sphere radius *R*. Replacing *A* and  $A_{tot}$  in equation (S11) and rearranging yields:

719 
$$\pi R^2 = W_{inj} H_{bed} t^* + A_B.$$
 (S12)

The area *B* may be approximated with a good accuracy as (Harris and Stöcker, 1998, pp 92-93):

721 
$$A_B \approx \frac{2}{3} W_{inj} h + \frac{h^3}{2 W_{inj}}$$
 (S13)

722 Inserting Eq. (S13) in Eq. (S12) gives:

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723 
$$0 = W_{inj}H_{bed}t^* + \frac{2}{3}W_{inj}h + \frac{h^3}{2W_{inj}} - \pi R^2.$$
 (S14)

Equation (S14) contains two unknowns, R and h, which can be related to each other tanks to geometry:

726 
$$0 = \frac{W_{inj}^{2}}{4} + (R - h)^{2} - R^{2}.$$
 (S15)

Using that H = 2R - h,  $H_{max}$  may be computed as a function of  $t^*$  by solving Equations (S14–S15).

Figure S3: Schematics of the geometrical setup. The drawing represents a section
perpendicular to the intrusion. The area covered by the injected melt is in gray and the area

## 737 Supplementary information 4:



This supplementary figures displays the magnitude of the vorticity.



- 739 **Figure S4:** Magnitude of the vorticity. Simulations correspond to the ones represented in Fig.
- 740 3 for the same time steps. The green curves indicate the injected melt contour.

#### 741 Supplementary information 5:

742

This supplementary section present the physical properties of the end members materials 743 744 involved in the 15 eruption considered in this study. In cases where mixing was so preeminent that 745 only mixed products were erupted (e.g., Unzen), pre-mixing host characteristics, including crystal 746 content, were determined using indirect evidences such as crystal rims in disequilibrium with the 747 surrounding melt. Viscosities and densities of intruder magmas were sometimes directly 748 characterized because they were erupted (e.g., Pinatubo; Pallister et al., 1996) or approximated using petrological inferences (e.g., Usu, where the melt SiO<sub>2</sub> content was estimated by Tomiya and 749 750 Takahashi, 1995, from mixing lines and end-members). The software Conflow (Mastin, 2002) was 751 used to calculate densities and viscosities when necessary.

752 All host magmas are mushes except one simple case and three complex cases. The Usu reservoir contained a nearly aphyric (2-5 vol.% crystals) rhyolite prior to the 1663 eruption (Tomiya 753 754 and Takahashi, 1995). We left this straightforward case in our analysis for completeness; removing it would not affect our results. We treated the next three complex cases separately in our analysis. 755 Krakatau is a compositionally zoned reservoir with a gradient in crystal content ranging from 4–15 756 vol.% in the felsic (dacitic to rhyodacitic) parts of the reservoir to aphiric in the more mafic (andesite) 757 758 parts of the reservoir (Mandeville et al., 1996). The second case is the Bronze Age eruption of 759 Santorini volcano known as the Minoan eruption. In one scenario, the reservoir that hosted the 760 Minoan eruption products had 10–20 vol% crystals (Cadoux et al., 2014). In others, more complex 761 scenarios have been proposed (Druitt, 2014; Flaherty et al., 2018; Martin et al., 2010). In one, the main rhyodacite would have instead acted as the intruder into an adjacent mushy, mafic reservoir 762

(Druitt, 2014). We reported these two possibilities. The 1912 eruption at Katmai-Novarupta is also a case where the roles of the intruder and host might be reversed (e.g. Coombs and Gardner, 2001; Eichelberger and Izbekov, 2000; Hammer et al., 2002; Singer et al., 2016). We reported the scenario in which the most crystal-rich components (andesite and dacite) are the hosts and the nearly aphyric rhyolite is the intruder (Eichelberger and Izbekov, 2000), as well as the scenario in which the host is composed of a zoned chamber and the intruder is a basaltic andesite (Singer et al., 2016).

769 There is a last complex case that is analyzed individually although its reservoir unambiguously contained a mush. Two mutually exclusive intrusion scenarios have indeed been proposed to explain 770 the 1991–1995 eruption of Unzen volcano. In both scenarios, the host magma was a phenocryst-rich, 771 low-temperature rhyolite mush and the intruder was a nearly aphyric, high-temperature magma 772 773 (Holtz et al., 2004; Nakamura, 1995). The composition of the intruder, which left only cryptic 774 indications of its presence such as reverse zoning of the outer rims of hornblende, plagioclase and 775 magnetite (Nakamura, 1995), could have been either andesitic (Holtz et al., 2004), or basaltic 776 (Browne et al., 2006).

777

778

**Table S3:** Host properties from natural cases (volcano names are followed by the starting year of the eruption). Minerals abbreviations are plagioclase (Plag), clinopyroxene (CPx), orthopyroxene (OPx), pyroxene (Px), and hornblende (Hb). Only the main mineral phases were taken into account and numbers in parenthesis are mineral volume proportions. Bulk densities were calculated with a plagioclase density of 2570 kg/m<sup>3</sup> and a density of 3200 kg/m<sup>3</sup> for all other minerals. Bulk viscosities were calculated as  $\eta_l (1 - \varphi/0.6)^{-2.5 \cdot 0.6}$ , where  $\eta_l$  is melt viscosity and  $\varphi$  is crystal volume fraction, except for the Minoan scenario 2 where the largest bul viscosity was capped at 10<sup>10</sup> Pa s because the higher bound of  $\varphi$  is >0.6. Abbreviations sat. and usat. mean saturated and undersaturated, respectively. Not used (n.u.) implies that melt densities and/or viscosities were directly given in the reference(s) corresponding to that case.

786

CASE	Name	Xtal	Minerals	Melt SiO <sub>2</sub>	Melt H <sub>2</sub> O	Melt density	Melt viscosity	Т	Р	Ref
		(vol%)		(wt%)	(wt%)	(kg/m³)	(Pa s)	(°C)	(MPa)	
Unzen 1991	Dacite	34-35	Plag (0.8) Cpx (0.2)	75	8	2229-2239	1.3×10 <sup>4</sup> -1.4×10 <sup>4</sup>	775	300	1
Vesuvius -79	White Pumice	31.6-40	Plag	53-57	sat.	2218-2300	2.4×10 <sup>3</sup> -3.0×10 <sup>3</sup>	875-900	150 <sup>b</sup>	2
Guadeloupe 1530	Andesite	48.3-57.5	Plag (0.8) Px (0.2)	73-75	5.5-6	2189-2203	1.2×10 <sup>4</sup> -2.5×10 <sup>4</sup>	825-875	135-200	3
Karymsky 1996	Andesite	25-32	Plag (0.8) Px (0.2)	63	sat.	2395-2378 ª	8.9×10 <sup>3</sup> -13×10 <sup>3</sup> <sup>a</sup>	1023-1057	200 <sup>b</sup>	4
Ruapehu 1995	Andesite	24.5-42	Plag (0.66) Px (0.33)	62-70	1-1.5	2380-2438	2.9×10 <sup>4</sup> -4.7×10 <sup>4</sup>	920-1030	40	5
Katmai 1912 -	Andesite	30-45	Plag (0.8) Px (0.2)	67.6-74	usat-sat.	2274-2284	1.2×10 <sup>4</sup> -1.3×10 <sup>4</sup>	920-970	75-120	6
scenario 1	Dacite	30-45	Plag (0.8) Px (0.2)	79.1	usat-sat.	2189-2220	2.0×10 <sup>5</sup> -8.1×10 <sup>5</sup>	850-910	60-25	_ 0
Katmai 1912 -	Andesite	30	Plag (0.8) Px (0.2)	67.6	usat.	2274	1.2×10 <sup>4</sup>	920	75	7
scenario 2	Rhyolite	2	Plag	77	4	2225	1.7×10 <sup>6</sup>	790	40	
Komagatake 1640	White Pumice	25-43.1	n.u.	74.7-76.1	3-4	2280-2300	4.4×10 <sup>4</sup> -2.9×10 <sup>5</sup> a	970-980	n.u.	8

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Montserrat 1995	Andesite	35-45	Plag	75-80	4.8	2171-2160	3.7×10 <sup>4</sup> -8.4×10 <sup>4</sup>	835-880	105-155	9
Redoubt 1990	Dacite	24-32	Plag	78.5-81	4	2164-2174	3.4×10 <sup>4</sup> -3.8×10 <sup>4</sup>	840-950	100	10
Krakatau 1883	White Rhyodacite	7-15	Plag	70-74	4	2220-2400	3.1×10 <sup>4</sup> -3.4×10 <sup>4</sup>	880-890	100-150	11
	Gray Dacite	4-12	Plag	66.5-75	4	2190-2200	1.3×10 <sup>4</sup> -1.4×10 <sup>4</sup>	890-913	100-150	_
Minoan – scenario 1	Rhyodacite	10-20	Plag	73.5-74	5-6	2222-2173	1.7×10 <sup>4</sup> -1.4×10 <sup>5</sup>	845-860	200-250	12
Minoan - scenario 2	Andesite	55-100	Plag (0.8) CPx (0.2)	71-77	sat. <sup>b</sup>	2213-2231	5.9×10 <sup>5</sup> -1.3×10 <sup>7</sup>	700-820	50	13
SW Trident 1953	Dacite	37-39	Plag (0.8) Px (0.2)	75	3.6	2190-2200	4.5×10 <sup>4</sup> -4.9×10 <sup>4</sup>	890	90	14
Dutton 1989	Dacite	35	Plag (0.8) OPx (0.2)	78	sat.	2481-2491	1.4×10 <sup>5</sup> -1.5×10 <sup>5</sup>	865	200 <sup>b</sup>	15
Pinatubo 1991	White Pumice	47	Plag (0.8) Hb (0.2)	76	6-6.5	2166	5.4×10 <sup>4</sup>	750-800	155-200	16
	Tan Pumice	15-26	Plag (0.8) Hb (0.2)	73	6-6.5	2194	5.6×10 <sup>4</sup>	750-800	155-200	_
Usu 1663	Silicic magma	2.6-5.3	Plag (0.8) OPx (0.2)	74	n.u.	2210-2224	9.5×10 <sup>4</sup> -2.6×10 <sup>5</sup>	750-800	n.u.	17

<sup>a</sup> Calculated from bulk values given in the reference(s).

<sup>b</sup> Assumed value.

789 <sup>c</sup> References are: 1) Holtz et al. (2005), Vetere et al. (2008)(andesite intruder), Browne et al. (2006)(basalt intruder); 2) Cioni et al. (1995), Scaillet et al. (2008); 3) Pichavant

790 et al. (2018); 4) Izbekov et al. (2002), Izbekov et al. (2004), Eichelberger and Izbekov (2000); 5) Nakagawa et al. (1999), Nakagawa et al. (2002), Kilgour et al. (2013); 6)

791 Eichelberger and Izbekov (2000), Coombs and Gardner (2001); 7) Hammer et al. (2002), Singer et al. (2016); 8) Takahashi and Nakagawa (2013); 9) Barclay et al. (1998),

792 Murphy et al. (2000), Couch et al. (2001), Humphreys et al. (2010), Plail et al. (2018); 10) Wolf and Eichelbeger (1997), Nye et al. (1994), Swanson et al. (1994); 11) Camus et

793 al. (1987), Self (1992), Mandeville et al. (1996); 12) Cottrell et al. (1999), Druitt et al. (1999), Cadoux et al. (2014), Flaherty et al. (2018); 13) Druitt (2014); 14) Coombs et al.

794 (2000), Coombs et al. (2002); 15) Miller et al. (1999); 16) Pallister et al. (1992), Pallister et al. (1996), Bernard et al. (1996); 17) Tomiya and Takahashi (2005).

Table S4: Intruder properties from natural cases. Minerals abbreviations are plagioclase (Plag), clinopyroxene (CPx),, pyroxene (Px), hornblende (Hb), olivine
 (Ol), and Augite (Aug). Abbreviations and references are the same as in Table S1.

CASE	Name	Xtal	Minerals	Melt SiO <sub>2</sub>	Melt H <sub>2</sub> O	Melt density	Melt viscosity	Т	Р
		(vol%)		(wt%)	(wt%)	(kg/m <sup>3</sup> )	(Pa s)	(°C)	(MPa)
Upzon 1991	Andesite	0-10	Plag <sup>b</sup>	62-64	4	2184-2194	3.2×10 <sup>2</sup> -3.2×10 <sup>2</sup>	1030-1130	300
012011771	Basalt	0-5	OI	50	sat. <sup>b</sup>	2351-2418	2.3-10	1030-1200 <sup>b</sup>	300 <sup>b</sup>
Vesuvius -79	K-rich basalt	0-20	Plag	50-52	usat.	2485-2441	13-16	1050-1140	150 <sup>b</sup>
Guadeloupe 1530	Basalt	0-12	Plag	50-53	5-6	2436-2420	5.4-9.3	975-1025	200 <sup>b</sup>
Karymsky 1996	Basalt	20	Plag	52	sat.	2545 °	22-54	1080-1115	200 <sup>b</sup>
Ruapehu 1995	High-T magma	0-10	Plag <sup>b</sup>	54.2-57.7	1-1.5	2530-2640	10-10 <sup>2</sup>	1100 <sup>b</sup> -1200 <sup>b</sup>	40
Katmai 1912 – scenario 1	Rhyolite	2	Plag	77	4	2225-2172	7.5×10 <sup>3</sup> -1.7×10 <sup>6</sup>	790-850	40-100
Katmai 1912 – scenario 2	Andesite	30-45	Plag (0.8) Px (0.2)	67.6-74	usatsat.	2274-2284	1.2×10 <sup>4</sup> -1.3×10 <sup>4</sup>	920-970	75-120
Komagatake 1640	Basalt	0		57	n.u.	2500 <sup>b</sup> -2540	5.0×10 <sup>3</sup> -1.0×10 <sup>3 a</sup>	1150	n.u.
Montserrat 1995	Mafic recharge	2-4.5	Plag	52-71	sat.	2400-2500	10-10 <sup>2</sup>	975-1196	105-155
Redoubt 1990	Andesite	24-32	Plag	64.5-66	4	2228-2238	1.6×10 <sup>4</sup> -1.8×10 <sup>4</sup>	840-950	100
Krakatau 1883	Basalt	0-10 <sup>b</sup>	Plag <sup>b</sup>	61.6	sat. <sup>b</sup>	2355-2363	24-31	984-1011	100-150
Minoan -	Mafia	22.40	Place (0, 9) CDv (0, 2)	61 60	cot b	0157 0147	6 1×10 <sup>3</sup> 6 7×10 <sup>3</sup>	990	50
scenario 1	Manc	22-40	Plag (0.8) CPX (0.2)	01-03	Sal.	2137-2107	0.1×10 -0./×10	000	50
Minoan -	Dhua da ait	wadaaita 10.00	Diag	70 5 74	E 4	2212 2172	1 7×104 1 4×105	945 940	200.250
scenario 2	кпуодасце	10-20	Plag	/3.3-/4	0-C	2213-21/3	1./×10 -1.4×10	842-800	200-250

SW Trident 1953	Andesite	28-43	Plag	74-63	3.5	2150-2295	8.3×10 <sup>2</sup> -10 <sup>4</sup>	990-1010	90
Dutton 1989	Mafic recharge	10-30	Plag	74	sat.	2546-2556	80-88	1080-1180	200 <sup>b</sup>
Pinatubo 1991	Basalt	19-25	Plag (0.75) Hb+Aug+Ol (0.25)	73.2	2-3 usat.	2159-2169	6.1×10 <sup>2</sup> -6.7×10 <sup>2</sup>	1250	250
Usu 1663	Mafic	0-1	Plag	54	n.u.	2351-2364	57-98	1000-1050	n.u.

<sup>a</sup> Calculated from bulk values given in the reference(s).

<sup>b</sup> Assumed value.

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