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1	Effect of solution chemistry on the iodine release from iodoapatite in aqueous environments
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# 15 Highlights

16	•	First study on the effect of aqueous ions on the degradation of waste form for I-129
17	•	First summary on probable iodine release pathways in various aqueous environments
18	•	Accelerated iodine release by enhanced ion-exchange, basicity or acidity, and ionic
19		strength
20	•	Discovered secondary phase vanadinite Pb5(VO4)3Cl and hydroxylvanadinite
21		Pb5(VO4)3OH
22	•	Low ionic content and neutral pH are vital to the disposal safety of nuclear waste

#### 24 Abstract

25 To ensure the safe disposal of nuclear waste, understanding the release process of radionuclides 26 retained in the nuclear waste forms is of vital importance. Iodoapatite Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub>, a potential 27 waste form for iodine-129, was selected as a model system for ceramic waste forms in this study to understand the effect of aqueous species on iodine release. Semi-dynamic leaching tests were 28 29 conducted on bulk samples in cap-sealed Teflon vessels with 0.1 mol/L NaCl, Na<sub>2</sub>CO<sub>3</sub>, Na<sub>3</sub>PO<sub>4</sub>, and Na<sub>2</sub>SO<sub>4</sub> solutions under 90 °C, fixed sample surface area to solution volume ratio of 5/m, 30 and periodic replacement of leaching solutions. The reacted solutions were then analyzed by 31 Inductively Coupled Plasma-Mass Spectrometry and Inductively Coupled Plasma-Optical 32 Emission Spectrometry; the leached surfaces were characterized by X-ray diffraction, scanning 33 electron microscopy, and infrared spectroscopy. The result shows that, compared to deionized 34 water, the ion-rich solutions enhanced the iodine release as a result of the increased ionic 35 strength, reduced activity coefficient of dissolved species, and increased solution pH. Surface 36 37 reactions can lead to the formations of secondary phases by ion-exchange and precipitation. These findings suggest that an ion-rich environment in the geological repository can be 38 detrimental to the disposal safety of the nuclear waste form. 39

# 40 1 Introduction

Nuclear energy is emission-free. The deployment of nuclear energy is motivated by the 41 pressing demand to mitigate climate change.<sup>1</sup> Sustainable development of the nuclear energy 42 requires concrete plans to safely dispose radionuclides waste generated by nuclear fission.<sup>2</sup> 43 Among those radionuclides, iodine-129 is particularly challenging to handle due to its long half-44 life (15.7 million years), high yield (0.7% yield per fission of uranium-235),<sup>3</sup> and weak 45 interactions with common materials in repository environments such as engineering barrier and 46 rock in geology formation.<sup>4,5</sup> Iodide (I<sup>-</sup>) is the most stable form of iodine in an environment with 47 pH and redox potential typically found in nature.<sup>6-8</sup> Under highly oxidizing conditions, iodide 48 can be oxidized to iodine  $(I_2)$  and/or iodate  $(IO_3^-)$ . All these iodine species are highly mobile in 49 nature given their high volatility and or high solubility.<sup>9,10</sup> Iodine, as an essential element for 50 human health, can accumulate in human bodies.<sup>11</sup> For a healthy adult, 30% of the total iodine, 51 approximately 15-20 mg, is concentrated in the thyroid gland.<sup>12</sup> Chronical radiation from iodine-52 129 beta decay can induce cancer to the thyroid follicular cells.<sup>11</sup> Therefore, iodine-129 is a 53 primary contributor of the radiation dosage when analyzing the safety of disposal environments.<sup>4</sup> 54 The immobilization of iodine-129 is one of the critical research subjects for nuclear waste 55 management.4,13-18 56

The most probable scenarios that compromise nuclear waste forms in a repository environment are the contact with aqueous solutions.<sup>19,20</sup> In a typical repository, nuclear waste forms are packed into corrosion resistant metallic canisters underground.<sup>21</sup> Canister corrosion and degradation are anticipated to be the result of corrodents carried by groundwater.<sup>22</sup> Through infiltration and percolation of precipitation and groundwater aquifer, water can reach the canisters and supply corrodents to react with the canister material. Upon the breaching of the canister, the waste forms are exposed to an aqueous environment. Owing to the long half-life of
iodine-129, it is crucial to predict the long-term chemical durability of iodine waste forms. To
enable such prediction, it is necessary to obtain a fundamental understanding of corrosion
mechanisms of waste forms and how iodine in the host material is released in various solutions
that may occur under repository conditions.

68 Several waste form materials including glass, ceramics, glass-ceramics, cement, and composite have been proposed to immobilize iodine.<sup>18,23</sup> These waste forms immobilize iodine 69 70 via two major mechanisms: encapsulation and incorporation. To encapsulate iodine, the host 71 matrices need to contain iodine in a designated phase different from the host material. One example is zeolite structure, in which iodine-bearing phases can be adsorbed on zeolite's 72 framework.<sup>17,24</sup> Iodine can also be incorporated as a compositional element into the host matrix 73 structure through chemical bonding, such as iodoapatite Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>I and sodalite 74 Na4(AlSiO<sub>4</sub>)<sub>3</sub>I.<sup>13,25-27</sup> 75

76 The difficulty to study the durability of different waste forms varies on a case-by-case basis. It is particularly challenging to evaluate the encapsulation waste forms due to the complexity of 77 multi-phase and microstructures. On the other hand, characterizing the corrosion mechanism can 78 be relatively straightforward for single-phase crystal waste forms which have well-defined 79 crystal structures and simple microstructures. Based on the simplicity of its crystal structure and 80 81 microstructure, iodoapatite is chosen in this study as the model system of ceramic waste forms that can incorporate radionuclides. In addition, apatite ceramics is a promising material due to its 82 thermal, mechanical, and chemical stability.<sup>13,25,28,29</sup> These advantages are also demonstrated in 83 84 nature as apatite has been found as a retention matrix for actinides and fission products in natural fission reactors at Franceville basin in Africa.<sup>22,30</sup> 85

86	Several chemical durability tests have been performed on single-phase crystal waste forms.
87	Uno et al. in 2001 conducted soxhlet leach method on apatite $Pb_{10}(VO_4)_6I_2$ . <sup>31</sup> Soxhlet leach
88	method is designed to maximize the number of leachable constituents in leachant by allowing a
89	continuous contact between the waste and recycling leachant in a closed system. <sup>32</sup> The iodine
90	release rate, $3.98 \times 10^{-5}$ g·cm <sup>-2</sup> ·d <sup>-1</sup> , was reported. <sup>31</sup> Guy et al. in 2002 studied apatite
91	Pb <sub>10</sub> (VO <sub>4</sub> ) <sub>4.8</sub> (PO <sub>4</sub> ) <sub>1.2</sub> I <sub>2</sub> dissolution in aqueous solutions. <sup>33</sup> The resulting data shows that iodine
92	release was incongruent and exhibited dependency on temperature and pH. They also discovered
93	a secondary phase, lead vanado-phosphate, precipitated at the sample surface. Zhang et al. in
94	2007 performed static leaching test on Pb5(VO4)3I powder in a basic KOH/KHCO3 buffer
95	solution. <sup>34</sup> Spectroscopic evidences show that $OH^2$ and $CO_3^{22}$ can substitute I <sup>2</sup> and $VO_4^{32}$ in
96	apatite. Maddrell et al. in 2014 conducted static leach tests on crushed powder iodide sodalite
97	Na <sub>4</sub> (AlSiO <sub>4</sub> ) <sub>3</sub> I in KOH/KHCO <sub>3</sub> buffer solutions. <sup>26</sup> The result suggests a congruent dissolution. <sup>26</sup>
98	Three leaching static experiments with durations of 3, 7, and 14 days exhibited a logarithmic
99	increase of iodine release. More recently, in 2017 Coulon et al. applied static leaching technique
100	to study the iodate-substituted hydroxyapatite in deionized water and groundwater. <sup>35</sup> They
101	reported that the iodine release is controlled by congruent dissolution under unsaturated
102	conditions and controlled by diffusion through ion exchange under saturated condition.
103	Interestingly, when groundwater was used as leachant, secondary phase hydroxyapatite
104	precipitated on the sample surface. Based on these studies, static leach test is a preferable method
105	to study the waste form durability due to the following reasons: 1) its simple procedure can
106	accommodate a wide range of test conditions; 2) the resultant data can be used to interpret the
107	release mechanism. <sup>36</sup> Static leaching method assumes that the solution feedback is negligible,
108	which is valid under conditions of sufficiently low surface to volume ratio. <sup>36</sup> However, the

solution feedback can gradually increase over time in a static leaching experiment. In cases 109 where the solution is oversaturated for phases of low solubility, secondary phases can precipitate 110 at the leached surface. Therefore, it can be problematic to use data from static leaching tests to 111 predict waste form behavior in a repository environment.<sup>37</sup> To address the issues of solution 112 feedback, a semi-dynamic leaching method was implemented by Zhang et al. in 2018 to quantify 113 the processes involved in the iodine release of an iodine-bearing apatite.<sup>29</sup> In their experiment, 114 deionized water solutions, as the leachant, were replaced periodically to minimize the solution 115 feedback. They demonstrated that iodine released from apatite is driven by short-term diffusion 116 117 and long-term matrix dissolution. This semi-dynamic approach was employed to produce essential datasets to parameterize a mechanistic model suitable for predicting the kinetics of 118 iodine release under different conditions.<sup>37</sup> 119

Since the aqueous systems in natural environment contain a variety of dissolved species, it is 120 necessary to understand how these aqueous species affect the iodine release from iodine waste 121 forms in an aqueous environment. For instance, the iodine release from apatite structured 122 materials can be enhanced by rapid substitution of halogen element<sup>38-41</sup> or inhibited by 123 precipitation of secondary phase.<sup>33,35,37</sup> In this study, we conducted semi-dynamic leach tests on 124 single phase crystal ceramics of iodoapatite in 0.1 mol/L NaCl, Na<sub>2</sub>CO<sub>3</sub>, Na<sub>3</sub>PO<sub>4</sub> and Na<sub>2</sub>SO<sub>4</sub> 125 solutions. The goal is to examine the impact of the solution chemistry on the kinetics of 126 127 iodoapatite dissolution. We hypothesized that dissolved aqueous species, via ion exchange and precipitation, can substantially impact the dissolution kinetics; this effect should highly depend 128 on the chemistry of the aqueous species and the surface reactions of specific phases. The finding 129 of this study is expected to provide important insight into the long-term performance of iodine 130 waste forms and guidance to improve the disposal safety of nuclear waste. 131

# **132 2** Experimental

#### 133 **2.1 Materials and methods**

Our samples, obtained from previous studies,<sup>25</sup> were dense ceramic chips in 134 quadrilateral shape: 4.7 - 10.3 millimeter long by 1.1 - 1.8 millimeter thick with a 135 chemical composition of Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub> according to the EDS and X-ray diffraction 136 refinement, as shown in Figs. 1, 2 and 4. The iodoapatite samples were synthesized by 137 using high energy ball milling (HEBM) and spark plasma sintering (SPS) techniques. 138 Sample surfaces were polished by 4000-grit sandpaper on a mechanical polishing wheel 139 lubricated with ethanol. Details of the synthesis and characterization of these samples 140 were reported previously in separate publications.<sup>25,29,37</sup> 141

The leaching method was adopted from ASTM C1308 standard test, as described in 142 the previous study<sup>29,37</sup>. Four parallel experiments were conducted simultaneously for 14 143 144 days in four different leaching solutions: 0.1 mol/L NaCl, 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>, and 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>. Sample surface area  $(m^2)$  to solution volume  $(m^3)$  ratios 145 146 (S/V) of all four tests were fixed and maintained at 5/m. The leached solutions were replaced every 24 hours. All reactor vessels were weighed before and after each interval 147 148 to monitor the solution losses which were within 0.5 % of the initial solution mass. In addition, a control test was conducted in deionized water under identical conditions for 7 149 days using the same protocol. All samples after leaching experiments were collected, 150 rinsed by deionized water and ethanol, and air-dried. 151

#### 152 **2.2 Characterization**

153	The elements of interest in the leachate solutions are I, Pb, and V. The leached
154	solutions, depending on the solution chemistry, were analyzed by Inductively Coupled
155	Plasma-Mass Spectrometry (ICP-MS, PerkinElmer Elan 9000) and/or Inductively-
156	Coupled Plasma-Optical Emission Spectrometry (ICP-OES, SPECTRO Ametek Spectro
157	ARCOS). Two standard solutions from Inorganic Ventures were used in the solution
158	analysis: 1) 1.001 $\pm$ 0.007 $\mu g/$ mL iodide in H2O solution and 2) 1.000 $\pm$ 0.007 $\mu g/$ mL
159	lead and $1.000 \pm 0.006 \ \mu\text{g}/\text{ mL}$ vanadium in 1% HNO <sub>3</sub> solution. Chemical properties of
160	solution at equilibrium state such as pH, ionic strength, speciation, and activity were
161	calculated by Visual MINTEQ package.
162	Samples were characterized by Scanning Electron Microscopy (SEM), Infrared
163	spectroscopy (IR), and X-ray diffraction spectroscopy (XRD). SEM images were taken by
164	a FEI Quanta SEM system with FEI Versa 3D DualBeam. Infrared spectroscopy was
165	performed on a Thermo Nicolet Continuum Infrared Microscope under Specular
166	Reflection mode and transmission mode with a fixed incident angle and an aperture area
167	of 10 by 10 $\mu$ m covering 4000 to 650 cm <sup>-1</sup> at a spectral resolution of 2 cm <sup>-1</sup> . XRD data
168	were collected from PANalytical Empyrean X-Ray Diffractometer equipped with
169	monochromated Cu-K $\alpha$ radiation ( $\lambda$ = 1.5406 Å), operated at 45 kV, 40 mA, a step size of
170	0.026°, and a scanning range from 5 to 100°.
171	The crystal structures were refined by Le Bail algorithm using Jana2006 program. <sup>42</sup>

The crystal structures were refined by Le Bail algorithm using Jana2006 program.<sup>42</sup> All parameters were refined by the least-squares method. The pseudo-Voigt function was used as the peak profile function. Structural parameters of Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub> measured by Audubert et al. were used as initial input (hexagonal, space group P63/m, a = b = 10.422 $Å, c = 7.467 Å, \alpha = \beta = 90^{\circ}; \gamma = 120^{\circ}).^{43}$ 

#### 176 **3 Results**

#### 177 **3.1 Leached surface characterization by SEM/EDS**

In Fig. 1 (a-c), no changes observable by naked eyes occurred on the surfaces of 178 samples leached by NaCl and NaSO<sub>4</sub> solutions for 14 days, whereas white layers were 179 180 gradually formed on the sample surfaces leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions within the first week of the experiments. The SEM images in Fig. 1 (d-i) show that the surface 181 alterations on samples leached by NaCl and Na<sub>2</sub>SO<sub>4</sub> solutions were moderate, similar to 182 the water leached surface. However, samples leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions 183 demonstrated significant surface corrosion and possible formation of new phases. The 184 surface leached by Na<sub>2</sub>CO<sub>3</sub> exhibited large grains, while congregated structures of similar 185 size appeared on the surface leached by Na<sub>3</sub>PO<sub>4</sub>. 186

187 According to EDS analysis, the surface chemical compositions in Fig. 2 indicate 188 considerable changes between the leached samples and the pristine one. The key features of EDS spectrum of pristine iodoapatite are: a carbon peak at 0.3 keV from background 189 190 (carbon tape), an oxygen peak at 0.5 keV, a broad Pb band from 2.34 to 2.45 keV 191 shouldered with two small Pb peaks at 1.8 and 2.6 keV, three iodine peaks at 3.9, 4.2, and 192 4.5 keV, and vanadium peaks at 4.9 and 5.4 keV. Overall, the iodine peaks at 3.94 keV are nearly diminished in the EDS spectra of all four leached surfaces. The samples 193 leached by NaCl and Na<sub>3</sub>PO<sub>4</sub> exhibited a substantial amount of chloride and phosphorus 194 195 signals at 2.62 and 2.01 keV, respectively. On the sample leached by NaCl, the Pb peak at 2.62 keV is comparable to the Pb peak at 1.8 keV, while the 2.62 keV peaks of the rest 196 samples are much weaker than their corresponding 1.8 keV peaks. Carbon signal at 0.27 197

keV from Na<sub>2</sub>CO<sub>3</sub> leached sample cannot be properly quantified due to the background 198 interference from carbon tape and the graphite impurity introduced during sample 199 synthesis. Sulfur EDS peak at 2.31 keV overlaps with the broad central peak of Pb at 2.34 200 keV. Na<sub>2</sub>SO<sub>4</sub> leached surface exhibited no sulfur peak near 2.3 keV given the 201 resemblance of the band shape between the sample leached by Na<sub>2</sub>SO<sub>4</sub> and the rest. We 202 203 noticed variations of carbon and oxygen EDS signals among these samples which were induced by the instrumentation settings such as sample orientation and beam parameters. 204 Therefore, carbon and oxygen were not considered in the EDS analysis. 205

# **3.2 Leached surface characterization by IR analysis**

The IR spectroscopy results are listed in Fig. 3. All these four samples yielded two 207 main peaks near 750 and 890 cm<sup>-1</sup>, which are attributed to V-O bond.<sup>34</sup> Pristine 208 iodoapatite and samples leached by water, Na<sub>2</sub>SO<sub>4</sub>, and NaCl showed nearly identical 209 spectra. Surfaces leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> exhibited position shifts of these two 210 V-O peaks to the region of 700 to 900 cm<sup>-1</sup> and multiple new bands. Sample leached by 211 Na<sub>2</sub>CO<sub>3</sub> yielded sharp bands near 785, 890, 960, 1200, and 1450 cm<sup>-1</sup>, in which the broad 212 band at 1450 cm<sup>-1</sup> is attributed to the stretching vibration of  $CO_3^{2-44,45}$  The Na<sub>3</sub>PO<sub>4</sub> 213 leached surface generated IR peaks near 785, 870, 950, 1110, 1420, 1800, and 2200 cm<sup>-1</sup>, 214 in which some can be assigned to the PO<sub>4</sub><sup>3-</sup> (e.g.  $v_1 - 950$  cm<sup>-1</sup>,  $v_3 - 1100$  cm<sup>-1</sup>).<sup>44</sup> 215 Interestingly, both CO<sub>3</sub><sup>2-</sup> and PO<sub>4</sub><sup>3-</sup> leached surfaces showed visible OH<sup>-</sup> stretching 216 vibration near 3500 cm<sup>-1</sup>,<sup>34,44</sup> which also occurred on water leached surface under IR 217 transmission mode.<sup>29</sup> 218

#### 219 **3.3 Leached surface characterization by XRD**

The XRD data are shown in Fig. 4. All these leached samples demonstrated 220 substantial differences compared to the pristine sample. Based on the XRD pattern, these 221 leached samples can be categorized into two groups: I) surfaces leached by NaCl and 222 Na<sub>2</sub>SO<sub>4</sub> solutions, the pristine, and water leached sample; II) surfaces leached by Na<sub>2</sub>CO<sub>3</sub> 223 and Na<sub>3</sub>PO<sub>4</sub> solutions, which were similar to the standard hydroxylvanadinite. The XRD 224 225 patterns of Group I are alike, which indicates no substantial structural changes compared to the pristine. The XRD patterns of Group II display enhanced peak splitting between 226 25° and 28°. The original peak splitting of the pristine sample reflects the apatite structure 227 228 deformation which accommodates the relatively large iodide incorporated in the apatite framework. The peak splitting of Na<sub>2</sub>SO<sub>4</sub> leached surface is slightly enhanced, compared 229 to the pristine, but is weaker than the water leached sample. Interestingly, NaCl leached 230 surface yielded a diminished splitting at 26° and a new peak occurred at 29°, later 231 identified as 131 shown in Fig. 5. The Full Width at Half Maximum (FWHM) of XRD 232 from NaCl leached surface was considerably broadened to  $\sim 0.4^{\circ}$  compared to  $\sim 0.2^{\circ}$  from 233 other samples, which may be attributed to the peak overlapping resulting from the 234 presence of a secondary phase. Both Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> leached samples exhibited 235 nearly identical XRD pattern, resembling the pattern of standard hydroxylvanadinite 236  $Pb_{10}(VO_4)_6(OH)_2$ . The two highest bands on  $Pb_{10}(VO_4)_6(OH)_2$  standard are 112 and  $1\overline{3}1$ 237 with an order of intensity  $I_{112} < I_{1\overline{3}1}$ . Same bands 112 and  $1\overline{3}1$  also have the highest 238 intensity on Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> leached samples, however, the intensity of 112 is higher 239 than that of  $1\overline{3}1$ ,  $I_{112} > I_{1\overline{3}1}$ . 240

The Le Bail method was applied to obtain structural information from the XRD data.
Table 1 compares the refined lattice parameters between sample surfaces of different

conditions and standards. No noticeable changes occurred in the crystal structures of 243 samples leached by deionized water and Na<sub>2</sub>SO<sub>4</sub> when compared to that of pristine 244 sample (their length of a-, b-, and c-axes are approximately  $\sim 10.4$ ,  $\sim 10.4$ , and  $\sim 7.5$  Å, 245 respectively). On the other hand, a  $\sim 0.2$  Å contraction along both the *a*- and *b*-axes were 246 observed for the samples leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions while the *c*-axis 247 remains the same and is consistent with other samples at ~7.45 Å. The observed and 248 calculated diffraction patterns, the residual and the indices of the main reflections of NaCl 249 leached sample are shown in Fig. 5. We identified a secondary phase vanadinite 250 251 Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>Cl, indicating the substitution of iodine by chlorine during NaCl leaching.

#### 252

#### 3.4 Solution composition analysis by ICP-MS and ICP-OES

The results of the solution analysis on the leachates collected from the leach tests are 253 shown in Fig. 6. The release rates of iodine, lead, and vanadium are depicted as green 254 circles, blue squares, and red triangles, respectively. In Fig. 6(a), iodine release in NaCl 255 256 solution gradually increased over time, reaching a maximum rate near 0.8 mmol/ $m^2/d$  at day 11, and then slightly decreased near the end of the 14-day test. The Pb and V release 257 exhibited similar patterns with a relatively high initial rate around 0.075 mmol/ $m^2/d$ , then 258 gradually decreased, and eventually approached a plateau near 0.05 mmol/m<sup>2</sup>/d. In Fig. 259 6(b), the release patterns of iodine and vanadium in Na<sub>2</sub>CO<sub>3</sub> are similar: release rates 260 rapidly reached maximum near day 2 and then gradually decreased over time approaching 261 a plateau. However, the long-term rate of Pb in Na<sub>2</sub>CO<sub>3</sub> appears to be constant. In Fig. 262 6(c), the iodine release in Na<sub>2</sub>SO<sub>4</sub> exhibited a high initial rate approximately 0.32 263 mmol/m<sup>2</sup>/d and then its rate gradually decreased, eventually approaching a plateau around 264 0.15 mmol/m<sup>2</sup>/d. Despite no high initial release, the Pb and V release patterns follow the 265

trend of iodine release: gradually decreased over time and then rebounded near day 10.
The Fig. 6(d) describes the element release of iodoapatite in Na<sub>3</sub>PO<sub>4</sub>, which shows
constant rates of ~4.5, ~3.5, and ~13 mmol/m<sup>2</sup>/d for the release for iodine, Pb, and V,
respectively. Due to the instrumentation limitation and sample consumption, only four
leachates from the Na<sub>3</sub>PO<sub>4</sub> experiment was analyzed for their Pb content.

271 Leaching rates of I, Pb, and V based on the solutions analysis are compared in Figs. 7(a-c), respectively. In general, leaching tests conducted in the ionic solutions present 272 significantly higher element release rates than those of deionized water in the order of 273 274  $Na_3PO_4 > Na_2CO_3 > Na_2SO_4 >$  water, except in the NaCl solution. In Fig. 7(a), iodine release from Na<sub>3</sub>PO<sub>4</sub>, Na<sub>2</sub>CO<sub>3</sub>, and Na<sub>2</sub>SO<sub>4</sub> solutions exhibited a long-term leach pattern 275 276 similar to that of water leaching: started with a high initial release, then gradually decreased, and eventually stabilized and reached a plateau. The iodine release in NaCl 277 solution, however, presents a different pattern: iodine rate increased from the beginning 278 of leach test to day 11, when the rate reached maximum and then stabilized. The release 279 rates of Pb and V from NaCl test are relatively constant but not higher than those of water 280 leached as shown in Figs. 7(b, c). 281

The molar ratios in leachate solutions are illustrated in Figs. 7(d, e). Except for the anomalous NaCl data, the long-term I/V ratios in Fig. 7(d) fluctuate around the ratio of water-leached sample within the range of [0.34, 1.02], which are higher than the stoichiometric value 0.28. In Fig. 7(e), the long-term Pb/V ratios of NaCl and Na<sub>2</sub>SO<sub>4</sub> tests are 1.36 and 1.65, approximate to the stoichiometric value 1.64, whereas the longterm ratios from Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> tests are 0.95 and 0.27, significantly lower than 1.64.

#### 3.5 Overview of leaching rates in solutions

290 The phases of interest in this study are the aqueous solutions and the solid surfaces. 291 The leachate solution chemistry in Fig. 7 shows that iodine release from the sample 292 leached by the NaCl solution has a distinctive pattern. For the other leach tests, the longterm iodine rates (plateau region in Figs. 6-7) are at least one magnitude higher than that 293 294 from water leaching. And the order of iodine leach rate, based on solution analysis in Fig. 7 (a), is consistent with the orders of Pb and V rates in Fig. 7 (b, c):  $R_{Pb/V/I}$  (Na<sub>3</sub>PO<sub>4</sub>) > 295  $R_{Pb/V/I}$  (Na<sub>2</sub>CO<sub>3</sub>) >  $R_{Pb/V/I}$  (Na<sub>2</sub>SO<sub>4</sub>) >  $R_{Pb/V/I}$  (deionized water). In the following section, 296 297 we will analyze the anomalous result of NaCl leach test and then explain how element release behaviors differentiate due to the different solution chemistry, such as pH and 298 ionic species. 299

#### **4 Discussion**

### **4.1 Anomaly of the sample leached by NaCl solution**

Iodoapatite sample leached by 0.1 mol/L NaCl solution exhibited unique surface 302 phase composition and iodine release pattern. The XRD data in Figs. 4 and 5 show 303 leached surface has no apparent splitting in the region from  $25^{\circ}$  to  $28^{\circ}$  (2 $\theta$ ) and a new 304 peak  $(1\overline{3}1)$ , attributed by a vanadinite phase. This anomaly suggests a reduced structural 305 distortion, which can be contributed by substituting iodide with smaller chloride. The 306 307 refinement in Fig. 5 confirmed new phase vanadinite was formed on the surface, which resembles the XRD pattern of iodoapatite Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub>. The XRD data is consistent 308 309 with the EDS result and solution analysis. The Pb EDS band at 2.6 keV, in Fig 2, is 310 comparatively enhanced due to the overlap by chlorine signal at 2.6 keV. The release

rates of iodine from the NaCl test in Fig. 6(a) suggest the new phase was growing until 311 the equilibrium state was reached. A similar iodine release pattern was observed in a pH 4 312 semi-dynamic leaching experiment, of which the rate anomaly was caused by the 313 formation of a secondary phase.<sup>37</sup> The molar ratios of Pb/V in Fig. 7(e) approximate to 314 the stoichiometric value 1.6, indicating a congruent dissolution of Pb and V. The variation 315 316 of I/V molar ratios in Fig. 7(d) is consistent with that of iodine rates in Fig. 6(a). Both the I/V ratios and iodine rates suggest an incongruent release for iodine, unlike the congruent 317 Pb and V. The SEM images in Figs. 1(b, e) show that both surfaces leached by NaCl and 318 319 deionized water share similar morphology. The new phase vanadinite Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>Cl, confirmed by the XRD refinement, suggests ion-exchange process between iodide and 320 chloride. This postulation is supported by the solution and surface analysis that 1) a 321 322 significant amount of iodine was released into NaCl solution while the Pb and V rates are comparable to the data of water leach test as shown in Figs. 6-7; 2) the surface alteration 323 revealed by SEM in Fig. 1 and the surface chemistry by EDS in Fig. 2 resemble those of 324 deionized water. Interestingly, the structural deformation of the original iodine-bearing 325 apatite  $Pb_{9.85}(VO_4)_{6I_{1.7}}$  appeared to be restored in the chlorine-substituted structure 326 vanadinite Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>Cl. Given that the ionic radius of chloride (Cl<sup>-</sup>, 1.68  $\pm$  0.19 Å) is 327 considerably smaller than that of iodide  $(I^2, 2.11 \pm 0.19 \text{ Å})$ ,<sup>46</sup> exchanging the iodide with 328 329 smaller chloride seems to have repaired the structural deformation.

330

#### 4.2 Effect of pH on iodine release and secondary phase formation

The solution pH has a strong effect on the iodine release of the iodoapatite. Chemical properties of the leaching solutions calculated by VMINTEQ are listed in Table 2. According to our previous studies, iodoapatite dissolution in deionized water can be

334	represented by the congruent release of Pb and V. <sup>29</sup> In Fig. 7 (b, c), the Pb and V rates
335	from different solutions are generally constant, indicating a constant-dissolution
336	controlled process. The overall dissolution rates from low to high appears to be: $R$
337	(deionized water) $< R$ (Na <sub>2</sub> SO <sub>4</sub> ) $< R$ (Na <sub>2</sub> CO <sub>3</sub> ) $< R$ (Na <sub>3</sub> PO <sub>4</sub> ), which corresponds to the
338	solution pH values ~6.1, ~6.2, ~10.3, and ~10.9 under 90 °C as listed in Table 2.
339	Therefore, increasing pH from neutral to basic can increase the iodine release by
340	enhancing the overall dissolution of the iodoapatite, which is consistent with previous
341	experimental results on synthetic iodoapatite and natural apatites <sup>33,47</sup> . However, due to the
342	secondary phase formed in Na <sub>2</sub> CO <sub>3</sub> solutions, the dissolution process was being
343	continuously hindered by the accumulating precipitates. Interestingly, the trend of iodine
344	released in Na <sub>2</sub> CO <sub>3</sub> solution of pH 10.3 resembles that of leaching iodoapatite under pH
345	4. <sup>37</sup> Despite the rate difference, both surfaces leached by pH 4 and pH 10.3 formed
346	secondary phases (chervetite and hydroxylvanadinite, respectively). Our previous study
347	showed that the equivalent long-term rate of iodine release under pH 6 is $8.1 \text{ mmol/m}^2/d$ ,
348	over two magnitudes higher than that of the deionized water 0.036 mmol/m <sup>2</sup> /d. <sup>37</sup>
349	Nevertheless, the release rates of iodine leached by the solutions of non-neutral pH are at
350	least one magnitude higher than that of the neutral pH solutions due to the enhanced
351	dissolution process.

Surface characterizations indicate the presence of new phases under the basic
conditions. The XRD analysis in Fig. 4 and Table 1 shows the surfaces leached by the
Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions were dominated by secondary phases resembling
hydroxylvanadinite Pb<sub>10</sub>(VO<sub>4</sub>)<sub>6</sub>(OH)<sub>2</sub>. The SEM in Fig. 1 reveals different grain shapes
and sizes from the water leached, while the EDS in Fig. 2 demonstrates that iodine was

depleted on the surface. The solution analysis also supports the formation of new phase 357 given the similar element release pattern to that of pH 4 and incongruent Pb/V ratios far 358 away from the stoichiometric value. As shown in Fig. 7, the leaching rates of all elements 359 are at least one magnitude higher than the water leach rates of corresponding elements. 360 The results from this study and those from relevant literature suggest that the solution pH 361 362 exerts significant effects on the dissolution rate and the secondary phase formation in aqueous environments such as chervetite and hydroxyvanadinite precipitated under acidic 363 and basic conditions, respectively.<sup>37,48,49</sup> 364

#### 365

# 4.3 Effect of ionic species on the dissolution rate

In this study, dissolved species affected the sample dissolution process by increasing 366 the ionic strength in solution, which consequently reduced the activity coefficient of 367 dissolved species. As a result, saturation state and solution feedback were reduced, which 368 in return increased the dissolution rate.<sup>47</sup> Although the 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub> and 0.1 mol/L 369 370 NaCl solutions have approximately the same solution pH as deionized water, the dissolution rates in these ionic solutions are significantly higher than that of the deionized 371 water. As shown in Table 2, 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub> solution gives total ionic strength of 0.26 372 mol/L, 0.1 mol/L NaCl solution 0.098 mol/L, and deionized water 2.04×10<sup>-6</sup> mol/L close 373 to zero. The vast difference in ionic strength leads to different degrees of saturation state. 374 The activity coefficient of the major ions Na<sup>+</sup>, Cl<sup>-</sup>, and SO<sub>4</sub><sup>2-</sup> in these ionic solutions are 375 ranging from 0.25 to 0.76, considerably lower than the major ions  $H^+$  and  $OH^-$  with a 376 respective activity coefficient 1.00 in the deionized water. The dissolution rate in 0.1 377 378 mol/L Na<sub>2</sub>SO<sub>4</sub> solution is higher than the rate in the 0.1 mol/L NaCl solution and deionized water under the same pH and reaction mechanism, as shown in Fig. 7. 379

Moreover, the average release rate of iodine in Na<sub>3</sub>PO<sub>4</sub> (pH 10.9) is about one magnitude higher that of Na<sub>2</sub>CO<sub>3</sub> (pH 10.3) despite their similar pHs. The difference in rates can be inferred from the difference in ionic strength: 0.29 mol/L for 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub> and 0.25 mol/L for Na<sub>2</sub>CO<sub>3</sub> solution.

In addition, no substantial structure change happened to the sample leached by 0.1384 mol/L Na<sub>2</sub>SO<sub>4</sub> solution. It is unlikely that anion SO<sub>4</sub><sup>2-</sup> can be incorporated into apatite 385 structure as there is no evidence from surface characterization and solution analysis to 386 support that. No structural change was detected by the XRD characterization. The SEM 387 388 images and EDS analysis in Figs. 1 and 2 show that the Na<sub>2</sub>SO<sub>4</sub> and water leached surfaces have a similar grain size, surface morphology, and chemical composition. The 389 element release rates and ratios in Fig. 7 and 8 demonstrate a similar leach behavior 390 between samples leached by Na<sub>2</sub>SO<sub>4</sub> and deionized water. The similarities in surface 391 alteration and leaching behavior between samples leached by Na<sub>2</sub>SO<sub>4</sub> and water suggest 392 that the iodine release in Na<sub>2</sub>SO<sub>4</sub> solution was controlled by short-term diffusion and 393 long-term dissolution and the release of Pb and V is controlled by congruent dissolution. 394 No precipitated was observed on Na<sub>2</sub>SO<sub>4</sub> leached surface, which is also similar to the 395 surface leached by water. 396

In terms of the surface precipitation, the SEM images in Figs. 1 (c, f) reflect intense surface alterations in the solutions of Na<sub>3</sub>PO<sub>4</sub> and Na<sub>2</sub>CO<sub>3</sub>. The leached surfaces yielded XRD patterns similar to the standard hydroxyvanadinite Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>OH. However, significant contractions of *a*- and *b*-axes as shown in Table 2 indicate the size of VO<sub>4</sub> site was reduced, which could be caused by a substitution of smaller groups.<sup>50</sup> The IR spectroscopy of the sample leached by Na<sub>3</sub>PO<sub>4</sub> confirms the existence of P-O bond and

 $OH^-$ . Furthermore, the EDS detected phosphorus signal, which also supports that  $PO_4$ 403 group was in VO<sub>4</sub> site. The molar ratios of Pb/V in Fig. 7 show a deficiency of Pb relative 404 to V in Na<sub>3</sub>PO<sub>4</sub> leaching test. These evidences suggest the precipitates are a product of 405 hydroxyvanadinite with mixed site: Pb<sub>10</sub>(VO<sub>4</sub>)<sub>n</sub>(PO<sub>4</sub>)<sub>6-n</sub>(OH)<sub>2</sub>. The site mixing is possible 406 since  $Pb_{10}(VO_4)_x(PO_4)_{6-x}(OH)_2$  can occur during wet chemistry reactions under similar 407 conditions.<sup>48</sup> Carbonate is known to be incorporated into apatite structure by 408 substitution.<sup>50–53</sup> Given that phosphate (PO<sub>4</sub><sup>3-</sup>, ionic radius  $2.30 \pm 0.42$  Å)<sup>46</sup> can replace 409 vanadate in iodoapatite,<sup>48</sup> it is reasonable to presume that carbonate of a smaller ionic 410 radius  $(CO_3^{2-}, 1.89 \pm 0.19 \text{ Å})^{46}$  can substitute vanadate in a similar crystal structure. 411 Therefore, the secondary phase formed on in the Na<sub>2</sub>CO<sub>3</sub> solution is  $Pb_{10}(VO_4)_{6-1}$ 412  $m(CO_3)_{1.5m}(OH)_2.$ 413

# 414 4.4 Mechanism of iodoapatite dissolution and surface reactions in aqueous 415 environments

Fig. 8 generalizes the mechanism of iodoapatite dissolutions with multiple processes 416 contributing to the iodine release. Our previous study on iodine release in deionized water 417 suggests that the iodine release is driven by short-term diffusion and long-term 418 dissolution.<sup>29</sup> Diffusion and dissolution are affected by various factors of the solution 419 chemistry, such as solution ionic strength, pH, and secondary phase formation resulted 420 from a supersaturation of the solution with respect to low solubility species. In neutral pH 421 solutions, the iodine release is subjected to the substitution of iodine by anionic species in 422 solution such as OH<sup>-</sup> and Cl<sup>-</sup>. When dealing with solutions of comparable pH, a higher 423 424 ionic strength, due to the ionic content, can enhance the dissolution by changing saturation conditions. Solution pH other than near neutral can increase the dissolution by 425

426 exponentially accelerating the dissolution process. The resulting rapid dissolution can 427 often lead to the precipitation of secondary phases when the solution approaches the 428 supersaturation state of low solubility phases. Possible secondary phases include 429 chervetite  $Pb_2V_2O_7$  under acidic condition<sup>37</sup> and hydroxylvanadinite  $Pb_5(VO_4)_3OH$  under 430 basic condition.

### 431 **5** Conclusions

The present study focuses on effects by solution compositions on iodoapatite 432 dissolution. The results suggest that the higher ionic strength can accelerate dissolution by 433 decreasing the activity coefficient of reacting aqueous species, thus promoting iodine 434 release from apatite. Non-neutral pH conditions clearly increase the dissolution rate and 435 often lead to precipitations of secondary phases, such as chervetite and 436 hydroxylvanadinite. The secondary phase precipitation at the surfaces hinders the 437 438 dissolution rate by reducing the available reacting surface area. However, the overall iodine release rates in both basic and acidic solutions are exponentially higher than those 439 in the near-neutral pH conditions, especially in deionized water. Current understanding of 440 dissolution is mostly based on leaching experiments conducted in deionized water. Our 441 investigation on the impact of solution chemistry reveals new complexities of the 442 dissolution kinetics of crystalline waste form during environmental degradation. Unlike 443 fresh water with low ion content, high concentrations of aqueous species commonly 444 found in underground brines can compromise the chemical durability of crystalline waste 445 form in a geological repository. For this specific waste form, maintaining neutral pH and 446 low ion content in aqueous solutions is important to the disposal safety of radioactive 447 iodine. Since iodine is one of the most challenging radionuclides to immobilize, building 448

- 449 a comprehensive theoretical framework of iodine immobilization can significantly
- 450 advance the research in nuclear waste disposal safety.

# 451 **Conflicts of interest**

452 There are no conflicts to declare.

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#### 463 **Date Availability**

464 Data will be made available on request

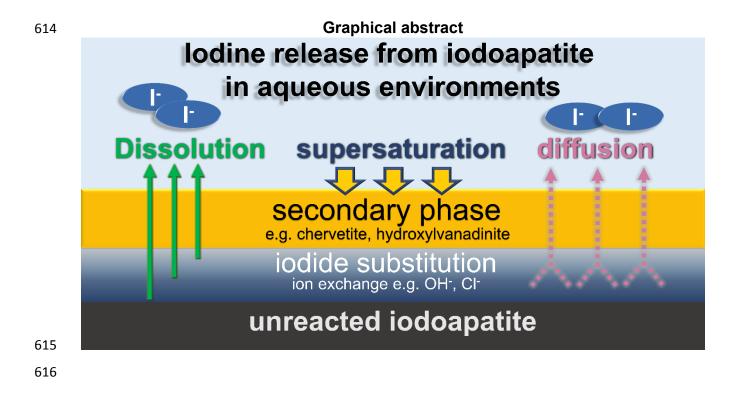
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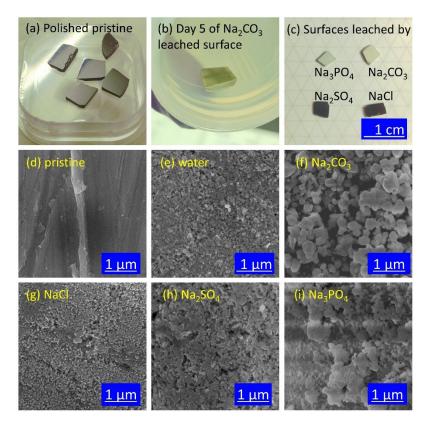


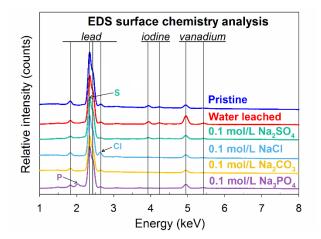
Fig. 1.(a) Polished pristine iodoapatite samples before test, (b) iodoapatite leached

surface during the 5<sup>th</sup> replacement of Na<sub>2</sub>CO<sub>3</sub> solution, (c) surface leached by at the end

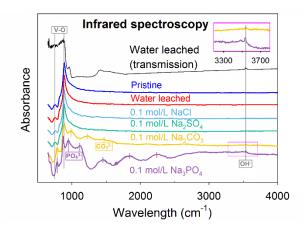
of 14-day leaching tests, SEM images of (a) a polished pristine iodoapatite and the

samples leached by (b) deionized water, (c) 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, (d) 0.1 mol/L NaCl, (e)

622 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>, and (f) 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>.



- Fig. 2. EDS spectra of a pristine iodoapatite and the samples leached by deionized
- water, 0.1 mol/L NaCl, 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>, and 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>
- 627 solutions.



- Fig. 3. Infrared spectroscopy of pristine iodoapatite and leached samples by deionized
- water, NaCl, Na<sub>2</sub>SO<sub>4</sub>, Na<sub>2</sub>CO<sub>3</sub>, and Na<sub>3</sub>PO<sub>4</sub> solutions.

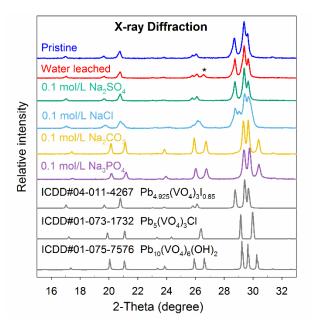


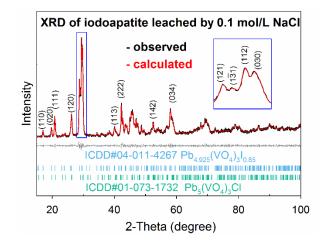
Fig. 4. XRD patterns of a pristine iodoapatite and the samples leached by deionized

635 water, 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>, 0.1 mol/L NaCl, 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, and 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>. In

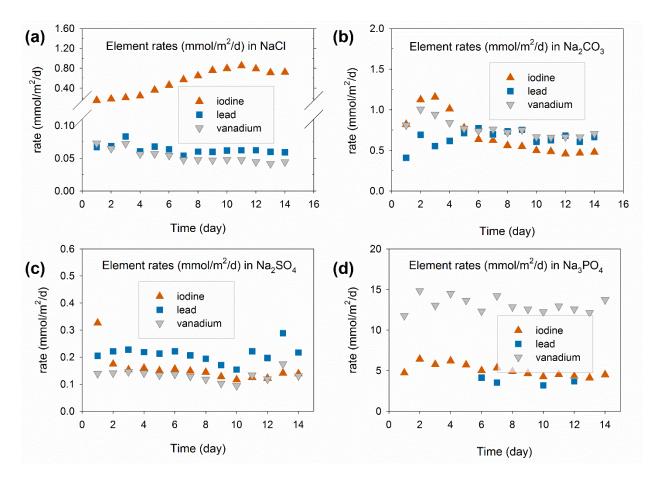
addition, standard XRD spectra of iodoapatite, vanadinite, and hydroxylvanadinite are

637 listed for comparison. \* denotes the graphite impurity introduced during sample

638 synthesis.<sup>25</sup>



- Fig. 5. XRD phase analysis of the iodoapatite sample surface leached by 0.1
- 641 mol/L NaCl solution. Two phases were identified: iodoapatite and vanadinite.



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Fig. 6. Solution analysis of collected leachates from 14 days semi-dynamic leach tests

on iodoapatite samples in (a) 0.1 mol/L NaCl, (b) 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, (c) 0.1 mol/L
Na<sub>2</sub>SO<sub>4</sub>, and (d) 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>.

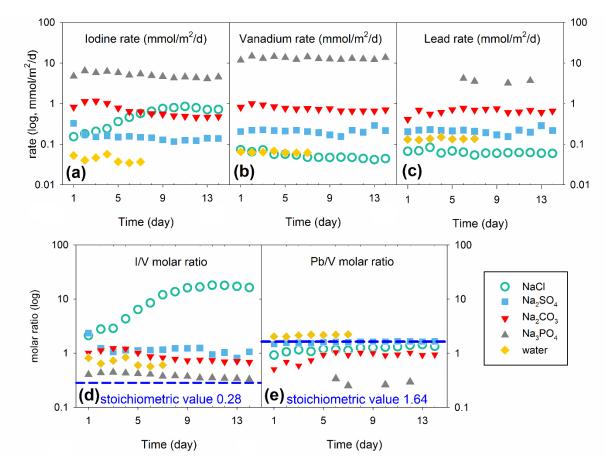


Fig. 7. Comparison of element release rate of iodine (a), vanadium (b), and lead (c) in the leachate solutions from different leach tests. Molar ratios of Pb/V (d) and I/V (e) in leachate solutions from leach tests in NaCl, Na<sub>2</sub>SO<sub>4</sub>, Na<sub>2</sub>CO<sub>3</sub>, Na<sub>3</sub>PO<sub>4</sub>, and deionized water.

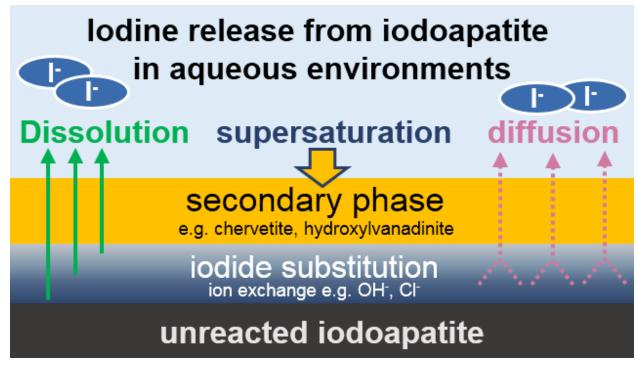


Fig. 8. Schematic diagram illustrates major processes that control the iodine release

657 from iodoapatite in aqueous environments

Table. 1 Crystallographic parameters based on the XRD refinements by Le Bailalgorithm.

Leach test	Refined parameters					
condition	a, b (a=b, Å)	c (Å)	GoF	R <sub>p</sub> (%)	R <sub>wp</sub> (%)	
Pristine	10.4420 (3)	7.4756 (3)	1.32	5.16	6.53	
Water	10.4325 (3)	7.4864 (3)	1.63	6.04	7.73	
0.1 mol/L Na₂SO₄	10.4336 (2)	7.4837 (2)	1.39	4.60	5.93	
0.1 mol/L Na <sub>2</sub> CO <sub>3</sub>	10.1923 (2)	7.4656 (2)	1.65	4.85	6.44	
0.1 mol/L Na₃PO₄	10.1984 (2)	7.4449 (2)	1.43	4.74	6.23	
0.1 mol/L NaCl (2 phases)	10.4443 (6)	7.4796 (5)				
(_ pilacoo)	10.3536 (8)	7.3735(8)	1.17	4.12	5.28	
Pb <sub>4.925</sub> (VO <sub>4</sub> ) <sub>3</sub> I <sub>0.85</sub> [ICDD#04-011-4267]	10.422	7.467	Crystal system: hexagonal			
Pb₅(VO₄)₃(OH) [ICDD#01-075-7576]	10.2242	7.4537	Space group: P63/m #176;			
Pb₅(VO₄)₃Cl [ICDD#01-073-1732]	10.31	7.34	α=90° β=90° γ=120°			

mol/L 90 °C	Deionized water	0.1 mol/L NaCl	0.1 mol/L Na₂SO₄	0.1 mol/L Na₂CO₃	0.1 mol/L Na₃PO₄
pH (unitless)	6.1	6.1	6.2	10.3	10.9
Ionic strength	2.04 × 10 <sup>-6</sup>	0.098	0.26	0.25	0.29
Major cation	H⁺	Na <sup>+</sup>	Na⁺	Na⁺	Na⁺
Concentration	6.52×10 <sup>-7</sup>	0.098	0.18	0.18	0.22
Activity	6.51×10 <sup>-7</sup>	0.074	0.13	0.13	0.15
Activity coefficient	1.00	0.76	0.72	0.72	0.68
Major anion	OH-	CI-	<b>SO</b> 4 <sup>2-</sup>	CO3 <sup>2-</sup>	PO4 <sup>3-</sup>
Concentration	8.72×10 <sup>-7</sup>	0.098	0.079	0.069	0.012
Activity	8.70×10 <sup>-7</sup>	0.074	0.02	0.017	0.00049
Activity coefficient	1.00	0.76	0.25	0.24	0.041

Table 2. Solution chemistry at equilibrium state calculated by Visual MINTEQ under90 °C.