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1	Effect of solution chemistry on the iodine release from iodoapatite in aqueous environments
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#### 15 Abstract

To ensure the safe disposal of nuclear waste, understanding the release process of radionuclides 16 17 retained in the nuclear waste forms is of vital importance. Iodoapatite Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub>, a potential 18 waste form for iodine-129, was selected as a model system for ceramic waste forms in this study to understand the effect of aqueous species on iodine release. Semi-dynamic leaching tests were 19 20 conducted on bulk samples in cap-sealed Teflon vessels with 0.1 mol/L NaCl, Na<sub>2</sub>CO<sub>3</sub>, Na<sub>3</sub>PO<sub>4</sub>, and Na<sub>2</sub>SO<sub>4</sub> solutions under 90 °C, fixed sample surface area to solution volume ratio of 5/m, 21 and periodic replacement of leaching solutions. The reacted solutions were then analyzed by 22 23 Inductively Coupled Plasma-Mass Spectrometry and Inductively Coupled Plasma-Optical Emission Spectrometry; the leached surfaces were characterized by X-ray diffraction, scanning 24 electron microscopy, and infrared spectroscopy. The result shows that, compared to deionized 25 water, the ion-rich solutions enhanced the iodine release as a result of the increased ionic 26 strength, reduced activity coefficient of dissolved species, and increased solution pH. Surface 27 28 reactions can lead to the formations of secondary phases by ion-exchange and precipitation of secondary phases. These findings suggest that an ion-rich environment in the geological 29 repository can be detrimental to the disposal safety of the apatite waste form. 30

# 31 **1 Introduction**

Nuclear power supplies low-carbon energy. The deployment of nuclear energy is motivated 32 by the pressing demand to mitigate climate change.<sup>1</sup> Sustainable development of the nuclear 33 energy requires concrete plans to safely dispose radionuclides waste generated by nuclear 34 fission.<sup>2</sup> Among those radionuclides, iodine-129 is particularly challenging to handle due to its 35 long half-life (15.7 million years), high yield (0.7% yield per fission of uranium-235),<sup>3</sup> and weak 36 interactions with common materials in repository environments such as engineering barrier and 37 rock in geology formation.<sup>4,5</sup> Iodide (I<sup>-</sup>) is the most stable form of iodine in an environment with 38 pH and redox potential typically found in nature.<sup>6-8</sup> Under highly oxidizing conditions, iodide 39 can be oxidized to iodine  $(I_2)$  and/or iodate  $(IO_3^-)$ . All these iodine species are highly mobile in 40 nature given their high volatility and or high solubility.<sup>9,10</sup> Iodine, as an essential element for 41 human health, can accumulate in human bodies.<sup>11</sup> For a healthy adult, 30% of the total iodine, 42 approximately 15-20 mg, is concentrated in the thyroid gland.<sup>12</sup> Chronical radiation from iodine-43 129 beta decay can induce cancer to the thyroid follicular cells.<sup>11</sup> Therefore, the iodine-129 is a 44 primary contributor of the radiation dosage when analyzing the safety of disposal environments.<sup>4</sup> 45 The immobilization of iodine-129 is one of the critical research subjects for nuclear waste 46 management.4,13-18 47

The most probable scenarios that compromise nuclear waste forms in a repository environment are the contact with aqueous solutions.<sup>19,20</sup> In a typical repository, nuclear waste forms are packed into corrosion resistant metallic canisters underground.<sup>21</sup> Canister corrosion and degradation are anticipated to be the result of corrodents carried by groundwater.<sup>22</sup> Through infiltration and percolation of precipitation and groundwater aquifer, water can reach the canisters and supply corrodents to react with the canister material. Upon the breaching of the canister, the waste forms are exposed to an aqueous environment. Owing to the long half-life of
iodine-129, it is crucial to predict the long-term chemical durability of iodine waste forms. To
enable such prediction, it is necessary to obtain a fundamental understanding of corrosion
mechanisms of waste forms and how iodine in the host material is released in various solutions
that may occur under repository conditions.

59 Several waste form materials including glass, ceramics, glass-ceramics, cement, and composite have been proposed to immobilize iodine.<sup>18,23</sup> These waste forms immobilize iodine 60 via two major mechanisms: encapsulation and incorporation. To encapsulate iodine, the host 61 62 matrices need to contain iodine in a designated phase different from the host material. One example is zeolite structure, in which iodine-bearing phases can be adsorbed on zeolite's 63 framework.<sup>17,24</sup> Iodine can also be incorporated as a compositional element into the host matrix 64 structure through chemical bonding, such as iodoapatite Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>I and sodalite 65 Na4(AlSiO<sub>4</sub>)<sub>3</sub>I.<sup>13,25-27</sup> 66

The difficulty to study the durability of different waste forms varies on a case-by-case basis. 67 It is particularly challenging to evaluate the encapsulation waste forms due to the complexity of 68 multi-phase and microstructures. On the other hand, characterizing the corrosion mechanism can 69 be relatively straightforward for single-phase crystal waste forms which have well-defined 70 crystal structures and simple microstructures. Based on the simplicity of its crystal structure and 71 72 microstructure, iodoapatite is chosen in this study as the model system of ceramic waste forms that can incorporate radionuclides. In addition, apatite ceramics is a promising material due to its 73 thermal, mechanical, and chemical stability.<sup>13,25,28,29</sup> These advantages are also demonstrated in 74 75 nature as apatite has been found as a retention matrix for actinides and fission products in natural fission reactors at Franceville basin in Africa.<sup>22,30</sup> 76

77	Several chemical durability tests have been performed on single-phase crystal waste forms.
78	Uno et al. in 2001 conducted soxhlet leach method on apatite $Pb_{10}(VO_4)_6I_2$ . <sup>31</sup> Soxhlet leach
79	method is designed to maximize the number of leachable constituents in leachant by allowing a
80	continuous contact between the waste and recycling leachant in a closed system. <sup>32</sup> The iodine
81	release rate, $3.98 \times 10^{-5}$ g·cm <sup>-2</sup> ·d <sup>-1</sup> , was reported. <sup>31</sup> Guy et al. in 2002 studied apatite
82	Pb <sub>10</sub> (VO <sub>4</sub> ) <sub>4.8</sub> (PO <sub>4</sub> ) <sub>1.2</sub> I <sub>2</sub> dissolution in aqueous solutions. <sup>33</sup> The resulting data shows that iodine
83	release was incongruent and exhibited dependency on temperature and pH. They also discovered
84	a secondary phase, lead vanado-phosphate, precipitated at the sample surface. Zhang et al. in
85	2007 performed static leaching test on Pb5(VO4)3I powder in a basic KOH/KHCO3 buffer
86	solution. <sup>34</sup> Spectroscopic evidences show that $OH^2$ and $CO_3^{22}$ can substitute I <sup>2</sup> and $VO_4^{32}$ in
87	apatite. Maddrell et al. in 2014 conducted static leach tests on crushed powder iodide sodalite
88	Na <sub>4</sub> (AlSiO <sub>4</sub> ) <sub>3</sub> I in KOH/KHCO <sub>3</sub> buffer solutions. <sup>26</sup> The result suggests a congruent dissolution. <sup>26</sup>
89	Three leaching static experiments with durations of 3, 7, and 14 days exhibited a logarithmic
90	increase of iodine release. More recently, in 2017 Coulon et al. applied static leaching technique
91	to study the iodate-substituted hydroxyapatite in deionized water and groundwater. <sup>35</sup> They
92	reported that the iodine release is controlled by congruent dissolution under unsaturated
93	conditions and controlled by diffusion through ion exchange under saturated condition.
94	Interestingly, when groundwater was used as leachant, secondary phase hydroxyapatite
95	precipitated on the sample surface. Based on these studies, static leach test is a preferable method
96	to study the waste form durability due to the following reasons: 1) its simple procedure can
97	accommodate a wide range of test conditions; 2) the resultant data can be used to interpret the
98	release mechanism. <sup>36</sup> Static leaching method assumes that the solution feedback is negligible,
99	which is valid under conditions of sufficiently low surface to volume ratio. <sup>36</sup> However, the

solution feedback can gradually increase over time in a static leaching experiment. In cases 100 where the solution is oversaturated for phases of low solubility, secondary phases can precipitate 101 at the leached surface. Therefore, it can be problematic to use data from static leaching tests to 102 predict waste form behavior in a repository environment.<sup>37</sup> To address the issues of solution 103 feedback, a semi-dynamic leaching method was implemented by Zhang et al. in 2018 to quantify 104 the processes involved in the iodine release of an iodine-bearing apatite.<sup>29</sup> In their experiment, 105 deionized water solutions, as the leachant, were replaced periodically to minimize the solution 106 feedback. They demonstrated that iodine released from apatite is driven by short-term diffusion 107 108 and long-term matrix dissolution. This semi-dynamic approach was employed to produce essential datasets to parameterize a mechanistic model suitable for predicting the kinetics of 109 iodine release under different conditions.<sup>37</sup> 110

Since the aqueous systems in natural environment contain a variety of dissolved species, it is 111 necessary to understand how these aqueous species affect the iodine release from iodine waste 112 forms in an aqueous environment. For instance, the iodine release from apatite structured 113 materials can be enhanced by rapid substitution of halogen element<sup>38-41</sup> or inhibited by 114 precipitation of secondary phase.<sup>33,35,37</sup> In this study, we conducted semi-dynamic leach tests on 115 single phase crystal ceramics of iodoapatite in 0.1 mol/L NaCl, Na<sub>2</sub>CO<sub>3</sub>, Na<sub>3</sub>PO<sub>4</sub> and Na<sub>2</sub>SO<sub>4</sub> 116 solutions. The goal is to examine the impact of the solution chemistry on the kinetics of 117 118 iodoapatite dissolution. We hypothesized that dissolved aqueous species, via ion exchange and precipitation, can substantially impact the dissolution kinetics; this effect should highly depend 119 on the chemistry of the aqueous species and the surface reactions of specific phases. The finding 120 of this study is expected to provide important insight into the long-term performance of iodine 121 waste forms and guidance to improve the disposal safety of nuclear waste. 122

## 123 **2 Experimental**

#### 124 **2.1 Materials and methods**

The samples, obtained from previous studies,<sup>25</sup> were dense ceramic chips in 125 quadrilateral shape: 4.7 - 10.3 millimeter long by 1.1 - 1.8 millimeter thick with a 126 chemical composition of Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub> according to the EDS and X-ray diffraction 127 refinement, as shown in Figures 1, 2 and 4. The iodoapatite samples were synthesized by 128 using high energy ball milling (HEBM) and spark plasma sintering (SPS) techniques. 129 Sample surfaces were polished by 4000-grit sandpaper on a mechanical polishing wheel 130 lubricated with ethanol. Details of the synthesis and characterization of these samples 131 were reported previously in separate publications.<sup>25,29,37</sup> 132

The leaching method was adopted from ASTM C1308 standard test, as described in 133 the previous study<sup>29,37</sup>. Four parallel experiments were conducted simultaneously for 14 134 135 days in four different leaching solutions: 0.1 mol/L NaCl, 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>, and 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>. Sample surface area  $(m^2)$  to solution volume  $(m^3)$  ratios 136 (S/V) of all four tests were fixed and maintained at 5/m. The leached solutions were 137 replaced every 24 hours. All reactor vessels were weighed before and after each interval 138 139 to monitor the solution losses which were within 0.5 % of the initial solution mass. In addition, a control test was conducted in deionized water under identical conditions for 7 140 days using the same protocol. All samples after leaching experiments were collected, 141 rinsed by deionized water and ethanol, and air-dried. 142

### 143 **2.2 Characterization**

144	The elements of interest in the leachate solutions are I, Pb, and V. The leached
145	solutions, depending on the solution chemistry, were analyzed by Inductively Coupled
146	Plasma-Mass Spectrometry (ICP-MS, PerkinElmer Elan 9000) and/or Inductively-
147	Coupled Plasma-Optical Emission Spectrometry (ICP-OES, SPECTRO Ametek Spectro
148	ARCOS). Two standard solutions from Inorganic Ventures were used in the solution
149	analysis: 1) 1.001 $\pm$ 0.007 $\mu g/$ mL iodide in H2O solution and 2) 1.000 $\pm$ 0.007 $\mu g/$ mL
150	lead and 1.000 $\pm$ 0.006 $\mu g/$ mL vanadium in 1% HNO3 solution. Solution chemistry at
151	equilibrium state such as pH, ionic strength, speciation, and activity were calculated by
152	Visual MINTEQ package.
153	Samples were characterized by Scanning Electron Microscopy (SEM), Infrared
154	spectroscopy (IR), and X-ray diffraction spectroscopy (XRD). SEM images were taken by
155	a FEI Quanta SEM system with FEI Versa 3D DualBeam. Infrared spectroscopy was
156	nonformed on a Thomas Nicelat Continuum Infranced Microscope under Succession
	performed on a Thermo Nicolet Continuum Infrared Microscope under Specular
157	Reflection mode and transmission mode with a fixed incident angle and an aperture area
157 158	
	Reflection mode and transmission mode with a fixed incident angle and an aperture area
158	Reflection mode and transmission mode with a fixed incident angle and an aperture area of 10 by 10 $\mu$ m covering 4000 to 650 cm <sup>-1</sup> at a spectral resolution of 2 cm <sup>-1</sup> . XRD data
158 159	Reflection mode and transmission mode with a fixed incident angle and an aperture area of 10 by 10 $\mu$ m covering 4000 to 650 cm <sup>-1</sup> at a spectral resolution of 2 cm <sup>-1</sup> . XRD data were collected from PANalytical Empyrean X-Ray Diffractometer equipped with

162 The crystal structures were refined by Le Bail algorithm using Jana2006 program.<sup>42</sup> 163 All parameters were refined by the least-squares method. The pseudo-Voigt function was 164 used as the peak profile function. Structural parameters of Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub> measured by 165 Audubert et al. were used as initial input (hexagonal, space group P63/m, a = b = 10.422 166 Å, c = 7.467 Å,  $\alpha = \beta = 90^{\circ}$ ;  $\gamma = 120^{\circ}$ ).<sup>43</sup>

## 167 **3 Results**

#### 168 **3.1 Leached surface characterization by SEM/EDS**

In Figure 1 (a-c), no changes observable by naked eyes occurred on the surfaces of 169 samples leached by NaCl and NaSO<sub>4</sub> solutions for 14 days, whereas white layers were 170 171 gradually formed on the sample surfaces leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions within the first week of the experiments. The SEM images in Figure 1 (d-i) show that the surface 172 alterations on samples leached by NaCl and Na<sub>2</sub>SO<sub>4</sub> solutions were moderate, similar to 173 174 the water leached surface. However, samples leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions demonstrated significant surface corrosion and possible formation of new phases. The 175 surface leached by Na<sub>2</sub>CO<sub>3</sub> exhibited large grains, while congregated structures of similar 176 size appeared on the surface leached by Na<sub>3</sub>PO<sub>4</sub>. 177

178 According to EDS analysis, the surface chemical compositions in Figure 2 indicate 179 considerable changes between the leached samples and the pristine one. The key features of EDS spectrum of pristine iodoapatite are: a carbon peak at 0.3 keV from background 180 (carbon tape), an oxygen peak at 0.5 keV, a broad Pb band from 2.34 to 2.45 keV 181 182 shouldered with two small Pb peaks at 1.8 and 2.6 keV, three iodine peaks at 3.9, 4.2, and 183 4.5 keV, and vanadium peaks at 4.9 and 5.4 keV. Overall, the iodine peaks at 3.94 keV are nearly diminished in the EDS spectra of all four leached surfaces. The samples 184 leached by NaCl and Na<sub>3</sub>PO<sub>4</sub> exhibited a substantial amount of chloride and phosphorus 185 signals at 2.62 and 2.01 keV, respectively. On the sample leached by NaCl, the Pb peak at 186 2.62 keV is comparable to the Pb peak at 1.8 keV, while the 2.62 keV peaks of the rest 187 samples are much weaker than their corresponding 1.8 keV peaks. Carbon signal at 0.27 188

keV from Na<sub>2</sub>CO<sub>3</sub> leached sample cannot be properly quantified due to the background 189 interference from carbon tape and the graphite impurity introduced during sample 190 synthesis. Sulfur EDS peak at 2.31 keV overlaps with the broad central peak of Pb at 2.34 191 keV. Na<sub>2</sub>SO<sub>4</sub> leached surface exhibited no sulfur peak near 2.3 keV given the 192 resemblance of the band shape between the sample leached by Na<sub>2</sub>SO<sub>4</sub> and the rest. We 193 194 noticed variations of carbon and oxygen EDS signals among these samples which were induced by the instrumentation settings such as sample orientation and beam parameters. 195 Therefore, carbon and oxygen were not considered in the EDS analysis. 196

## **3.2 Leached surface characterization by IR analysis**

The IR spectroscopy results are listed in Figure 3. All these four samples yielded two 198 main peaks near 750 and 890 cm<sup>-1</sup>, which are attributed to V-O bond.<sup>34</sup> Pristine 199 iodoapatite and samples leached by water, Na<sub>2</sub>SO<sub>4</sub>, and NaCl showed nearly identical 200 spectra. Surfaces leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> exhibited position shifts of these two 201 V-O peaks to the region of 700 to 900 cm<sup>-1</sup> and multiple new bands. Sample leached by 202 Na<sub>2</sub>CO<sub>3</sub> yielded sharp bands near 785, 890, 960, 1200, and 1450 cm<sup>-1</sup>, in which the broad 203 band at 1450 cm<sup>-1</sup> is attributed to the stretching vibration of  $CO_3^{2-44,45}$  The Na<sub>3</sub>PO<sub>4</sub> 204 leached surface generated IR peaks near 785, 870, 950, 1110, 1420, 1800, and 2200 cm<sup>-1</sup>, 205 in which some can be assigned to the PO<sub>4</sub><sup>3-</sup> (e.g.  $v_1 - 950$  cm<sup>-1</sup>,  $v_3 - 1100$  cm<sup>-1</sup>).<sup>44</sup> 206 Interestingly, both CO<sub>3</sub><sup>2-</sup> and PO<sub>4</sub><sup>3-</sup> leached surfaces showed visible OH<sup>-</sup> stretching 207 vibration near 3500 cm<sup>-1</sup>,<sup>34,44</sup> wPOhich also occurred on water leached surface under IR 208 transmission mode.<sup>29</sup> 209

## 210 **3.3 Leached surface characterization by XRD**

The XRD data are shown in Figure 4. All these leached samples demonstrated 211 substantial differences compared to the pristine sample. Based on the XRD pattern, these 212 leached samples can be categorized into two groups: I) surfaces leached by NaCl and 213 Na<sub>2</sub>SO<sub>4</sub> solutions, the pristine, and water leached sample; II) surfaces leached by Na<sub>2</sub>CO<sub>3</sub> 214 and Na<sub>3</sub>PO<sub>4</sub> solutions, which were similar to the standard hydroxylvanadinite. The XRD 215 216 patterns of Group I are alike, which indicates no substantial structural changes compared to the pristine. The XRD patterns of Group II display enhanced peak splitting between 217 25° and 28°. The original peak splitting of the pristine sample reflects the apatite structure 218 219 deformation which accommodates the relatively large iodide incorporated in the apatite framework. The peak splitting of Na<sub>2</sub>SO<sub>4</sub> leached surface is slightly enhanced, compared 220 to the pristine, but is weaker than the water leached sample. Interestingly, NaCl leached 221 surface yielded a diminished splitting at 26° and a new peak occurred at 29°, later 222 identified as  $1\overline{3}1$  shown in Figure 5. The Full Width at Half Maximum (FWHM) of XRD 223 from NaCl leached surface was considerably broadened to  $\sim 0.4^{\circ}$  compared to  $\sim 0.2^{\circ}$  from 224 225 other samples, which may be attributed to the peak overlapping resulting from the presence of a secondary phase. Both Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> leached samples exhibited 226 227 nearly identical XRD pattern, resembling the pattern of standard hydroxylvanadinite  $Pb_{10}(VO_4)_6(OH)_2$ . The two highest bands on  $Pb_{10}(VO_4)_6OH_2$  standard are 112 and  $1\overline{3}1$ 228 with an order of intensity  $I_{112} < I_{1\overline{3}1}$ . Same bands 112 and  $1\overline{3}1$  also have the highest 229 intensity on Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> leached samples, however, the intensity of 112 is higher 230 than that of  $1\overline{3}1$ ,  $I_{112} > I_{1\overline{3}1}$ . 231

The Le Bail method was applied to obtain structural information from the XRD data.Table 1 compares the refined lattice parameters between sample surfaces of different

conditions and standards. No noticeable changes occurred in the crystal structures of 234 samples leached by deionized water and Na<sub>2</sub>SO<sub>4</sub> when compared to that of pristine 235 sample (their length of a-, b-, and c-axes are approximately  $\sim 10.4$ ,  $\sim 10.4$ , and  $\sim 7.5$  Å, 236 respectively). On the other hand, a  $\sim 0.2$  Å contraction along both the *a*- and *b*-axes were 237 observed for the samples leached by Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions while the *c*-axis 238 remains the same and is consistent with other samples at ~7.45 Å. The observed and 239 calculated diffraction patterns, the residual and the indices of the main reflections of NaCl 240 leached sample are shown in Figure 5. We identified a secondary phase vanadinite 241 242 Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>Cl, indicating the substitution of iodine by chlorine during NaCl leaching.

#### 243

## 3.4 Solution composition analysis by ICP-MS and ICP-OES

The results of the solution analysis on the leachates collected from the leach tests are 244 shown in Figure 6. The release rates of iodine, lead, and vanadium are depicted as green 245 circles, blue squares, and red triangles, respectively. In Figure 6(a), iodine release in NaCl 246 247 solution gradually increased over time, reaching a maximum rate near 0.8 mmol/ $m^2/d$  at day 11, and then slightly decreased near the end of the 14-day test. The Pb and V release 248 exhibited similar patterns with a relatively high initial rate around 0.075 mmol/ $m^2/d$ , then 249 gradually decreased, and eventually approached a plateau near 0.05 mmol/m<sup>2</sup>/d. In Figure 250 6(b), the release patterns of iodine and vanadium in Na<sub>2</sub>CO<sub>3</sub> are similar: release rates 251 rapidly reached maximum near day 2 and then gradually decreased over time approaching 252 a plateau. However, the long-term rate of Pb in Na<sub>2</sub>CO<sub>3</sub> appears to be constant. In Figure 253 6 (c), the iodine release in  $Na_2SO_4$  exhibited a high initial rate approximately 0.32 254 mmol/m<sup>2</sup>/d and then its rate gradually decreased, eventually approaching a plateau around 255 0.15 mmol/m<sup>2</sup>/d. Despite no high initial release, the Pb and V release patterns follow the 256

trend of iodine release: gradually decreased over time and then rebounded near day 10. The Figure 6(d) describes the element release of iodoapatite in Na<sub>3</sub>PO<sub>4</sub>, which shows constant rates of ~4.5, ~3.5, and ~13 mmol/m<sup>2</sup>/d for the release for iodine, Pb, and V, respectively. Due to the instrumentation limitation and sample consumption, only four leachates from the Na<sub>3</sub>PO<sub>4</sub> experiment was analyzed for their Pb content.

262 Leaching rates of I, Pb, and V based on the solutions analysis are compared in Figures 7(a-c), respectively. In general, leaching tests conducted in the ionic solutions present 263 significantly higher element release rates than those of deionized water in the order of 264  $Na_3PO_4 > Na_2CO_3 > Na_2SO_4 >$  water, except in the NaCl solution. In Figure 7(a), iodine 265 release from Na<sub>3</sub>PO<sub>4</sub>, Na<sub>2</sub>CO<sub>3</sub>, and Na<sub>2</sub>SO<sub>4</sub> solutions exhibited a long-term leach pattern 266 similar to that of water leaching: started with a high initial release, then gradually 267 decreased, and eventually stabilized and reached a plateau. The iodine release in NaCl 268 solution, however, presents a different pattern: iodine rate increased from the beginning 269 of leach test to day 11, when the rate reached maximum and then stabilized. The release 270 rates of Pb and V from NaCl test are relatively constant but not higher than those of water 271 leached as shown in Figures 7(b, c). 272

The molar ratios in leachate solutions are illustrated in Figures 7 (d, e). Except for the anomalous NaCl data, the long-term I/V ratios in Figure 7(d) fluctuate around the ratio of water-leached sample within the range of [0.34, 1.02], which are higher than the stoichiometric value 0.28. In Figure 7(e), the long-term Pb/V ratios of NaCl and Na<sub>2</sub>SO<sub>4</sub> tests are 1.36 and 1.65, approximate to the stoichiometric value 1.64, whereas the longterm ratios from Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> tests are 0.95 and 0.27, significantly lower than 1.64.

## 3.5 Overview of leaching rates in solutions

The phases of interest in this study are the aqueous solutions and the solid surfaces. 281 282 The leachate solution chemistry in Figure 7 shows that iodine release from the sample 283 leached by the NaCl solution has a distinctive pattern. For the other leach tests, the longterm iodine rates (plateau region in Figures 6-7) are at least one magnitude higher than 284 285 that from water leaching. And the order of iodine leach rate, based on solution analysis in Figure 7 (a), is consistent with the orders of Pb and V rates in Figure 7 (b, c):  $R_{Pb/V/I}$ 286  $(Na_3PO_4) > R_{Pb/V/I} (Na_2CO_3) > R_{Pb/V/I} (Na_2SO_4) > R_{Pb/V/I} (deionized water)$ . In the 287 288 following section, we will analyze the anomalous result of NaCl leach test and then explain how element release behaviors differentiate due to the different solution 289 chemistry, such as pH and ionic species. 290

## 291 **4 Discussion**

## 4.1 Anomaly of the sample leached by NaCl solution

Iodoapatite sample leached by 0.1 mol/L NaCl solution exhibited unique surface 293 294 phase composition and iodine release pattern. The XRD data in Figures 4 and 5 show leached surface has no apparent splitting in the region from  $25^{\circ}$  to  $28^{\circ}$  (2 $\theta$ ) and a new 295 peak  $(1\overline{3}1)$ , attributed by a vanadinite phase. This anomaly suggests a reduced structural 296 distortion, which can be contributed by substituting iodide with smaller chloride. The 297 298 refinement in Figure 5 confirmed new phase vanadinite was formed on the surface, which resembles the XRD pattern of iodoapatite Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub>. The XRD data is consistent 299 300 with the EDS result and solution analysis. The Pb EDS band at 2.6 keV, in Fig 2, is 301 comparatively enhanced due to the overlap by chlorine signal at 2.6 keV. The release

rates of iodine from the NaCl test in Figure 6(a) suggest the new phase was growing until 302 the equilibrium state was reached. A similar iodine release pattern was observed in a pH 4 303 semi-dynamic leaching experiment, in which the rate anomaly was caused by the 304 formation of a secondary phase.<sup>37</sup> The molar ratios of Pb/V in Figure 7(e) approximate to 305 the stoichiometric value 1.6, indicating a congruent dissolution of Pb and V. The variation 306 307 of I/V molar ratios in Figure 7(d) is consistent with that of iodine rates in Figure 6(a). Both the I/V ratios and iodine rates suggest an incongruent release for iodine, unlike the 308 congruent Pb and V. The SEM images in Figures 1(b, e) show that both surfaces leached 309 310 by NaCl and deionized water share similar morphology. The new phase vanadinite Pb<sub>5</sub>(VO<sub>4</sub>)Cl, confirmed by the XRD refinement, suggests ion-exchange process between 311 iodide and chloride. This postulation is supported by the solution and surface analysis that 312 1) a significant amount of iodine was released into NaCl solution while the Pb and V rates 313 are comparable to the data of water leach test as shown in Figures 6-7; 2) the surface 314 alteration revealed by SEM in Figure 1 and the surface chemistry by EDS in Figure 2 315 resemble those of deionized water. Interestingly, the structural deformation of the original 316 iodine-bearing apatite Pb<sub>9.85</sub>(VO<sub>4</sub>)<sub>6</sub>I<sub>1.7</sub> appeared to be restored in the chlorine-substituted 317 structure vanadinite Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>Cl. Given that the ionic radius of chloride (Cl<sup>-</sup>,  $1.68 \pm 0.19$ 318 Å) is considerably smaller than that of iodide  $(I^2, 2.11 \pm 0.19 \text{ Å})$ ,<sup>46</sup> exchanging the iodide 319 320 with smaller chloride seems to have repaired the structural deformation.

321

## 4.2 Effect of pH on iodine release and secondary phase formation

The solution pH has a strong effect on the iodine release of the iodoapatite. Parameters of the solution chemistry calculated by VMINTEQ are listed in Table 2. According to our previous studies, iodoapatite dissolution in deionized water can be represented by the

325	congruent release of Pb and V. <sup>29</sup> In Figure 7 (b, c), the Pb and V rates from different
326	solutions are generally constant, indicating a constant-dissolution controlled process. The
327	overall dissolution rates from low to high appears to be: $R$ (deionized water) $< R$
328	$(Na_2SO_4) < R (Na_2CO_3) < R (Na_3PO_4)$ , which corresponds to the solution pH values ~6.1,
329	~6.2, ~10.3, and ~10.9 under 90 °C as listed in Table 2. Therefore, increasing pH from
330	neutral to basic can increase the iodine release by enhancing the overall dissolution of the
331	iodoapatite, which is consistent with previous experimental results on synthetic
332	iodoapatite and natural apatites <sup>33,47</sup> . However, due to the secondary phase formed in
333	Na <sub>2</sub> CO <sub>3</sub> solutions, the dissolution process was being continuously hindered by the
334	accumulating precipitates. Interestingly, the trend of iodine released in Na <sub>2</sub> CO <sub>3</sub> solution
335	of pH 10.3 resembles that of leaching iodoapatite under pH 4.37 Despite the rate
336	difference, both surfaces leached by pH 4 and pH 10.3 formed secondary phases
337	(chervetite and hydroxylvanadinite, respectively). Our previous study showed that the
338	equivalent long-term rate of iodine release under pH 6 is 8.1 mmol/m <sup>2</sup> /d, over two
339	magnitudes higher than that of the deionized water $0.036 \text{ mmol/m}^2/d.^{37}$ Nevertheless, the
340	release rates of iodine leached by the solutions of non-neutral pH are at least one
341	magnitude higher than that of the neutral pH solutions due to the enhanced dissolution
342	process.

Surface characterizations indicate the presence of new phases under the basic
conditions. The XRD analysis in Figure 4 and Table 1 shows the surfaces leached by the
Na<sub>2</sub>CO<sub>3</sub> and Na<sub>3</sub>PO<sub>4</sub> solutions were dominated by secondary phases resembling
hydroxylvanadinite Pb<sub>10</sub>(VO<sub>4</sub>)<sub>6</sub>(OH)<sub>2</sub>. The SEM in Figure 1 reveals different grain shapes
and sizes from the water leached, while the EDS in Figure 2 demonstrates that iodine was

depleted on the surface. The solution analysis also supports the formation of new phase 348 given the similar element release pattern to that of pH 4 and incongruent Pb/V ratios far 349 away from the stoichiometric value. As shown in Figure 7, the leaching rates of all 350 elements are at least one magnitude higher than the water leach rates of corresponding 351 elements. The results from this study and those from relevant literature suggest that the 352 solution pH exerts significant effects on the dissolution rate and the secondary phase 353 formation in aqueous environments such as chervetite and hydroxyvanadinite precipitated 354 under acidic and basic conditions, respectively.<sup>37,48,49</sup> 355

#### 356

## 4.3 Effect of ionic species on the dissolution rate

In this study, dissolved species affected the sample dissolution process by increasing 357 the ionic strength in solution, which consequently reduced the activity coefficient of 358 dissolved species. As a result, saturation state and solution feedback were reduced, which 359 in return increased the dissolution rate.<sup>47</sup> Although the 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub> and 0.1 mol/L 360 NaCl solutions have approximately the same solution pH as deionized water, the 361 dissolution rates in these ionic solutions are significantly higher than that of the deionized 362 water. As shown in Table 2, 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub> solution gives total ionic strength of 0.26 363 mol/L, 0.1 mol/L NaCl solution 0.098 mol/L, and deionized water 2.04×10<sup>-6</sup> mol/L close 364 to zero. The vast difference in ionic strength leads to different degrees of saturation state. 365 The activity coefficient of the major ions Na<sup>+</sup>, Cl<sup>-</sup>, and SO<sub>4</sub><sup>2-</sup> in these ionic solutions are 366 ranging from 0.25 to 0.76, considerably lower than the major ions  $H^+$  and  $OH^-$  with a 367 respective activity coefficient 1.00 in the deionized water. The dissolution rate in 0.1 368 369 mol/L Na<sub>2</sub>SO<sub>4</sub> solution is higher than the rate in the 0.1 mol/L NaCl solution and deionized water under the same pH and reaction mechanism, as shown in Figure 7. 370

Moreover, the average release rate of iodine in  $Na_3PO_4$  (pH 10.9) is about one magnitude higher that of  $Na_2CO_3$  (pH 10.3) despite their similar pHs. The difference in rates can be inferred from the difference in ionic strength: 0.29 mol/L for 0.1 mol/L  $Na_3PO_4$  and 0.25 mol/L for  $Na_2CO_3$  solution.

In addition, no substantial structure change happened to the sample leached by 0.1375 mol/L Na<sub>2</sub>SO<sub>4</sub> solution. It is unlikely that anion SO<sub>4</sub><sup>2-</sup> can be incorporated into apatite 376 377 structure as there is no evidence from surface characterization and solution analysis to support that. No structural change was detected by the XRD characterization. The SEM 378 379 images and EDS analysis in Figures 1 and 2 show that the Na<sub>2</sub>SO<sub>4</sub> and water leached surfaces have a similar grain size, surface morphology, and chemical composition. The 380 element release rates and ratios in Figure 7 and 8 demonstrate a similar leach behavior 381 between samples leached by Na<sub>2</sub>SO<sub>4</sub> and deionized water. The similarities in surface 382 alteration and leaching behavior between samples leached by Na<sub>2</sub>SO<sub>4</sub> and water suggest 383 that the iodine release in Na<sub>2</sub>SO<sub>4</sub> solution was controlled by short-term diffusion and 384 long-term dissolution and the release of Pb and V is controlled by congruent dissolution. 385 No precipitated was observed on Na<sub>2</sub>SO<sub>4</sub> leached surface, which is also similar to the 386 surface leached by water. 387

In terms of the surface precipitation, the SEM images in Figures 1 (c, f) reflect intense surface alterations in the solutions of Na<sub>3</sub>PO<sub>4</sub> and Na<sub>2</sub>CO<sub>3</sub>. The leached surfaces yielded XRD patterns similar to the standard hydroxyvanadinite Pb<sub>5</sub>(VO<sub>4</sub>)<sub>3</sub>(OH). However, significant contractions of *a*- and *b*-axes as shown in Table 2 indicate the size of VO<sub>4</sub> site was reduced, which could be caused by a substitution of smaller groups.<sup>50</sup> The IR spectroscopy of the sample leached by Na<sub>3</sub>PO<sub>4</sub> confirms the existence of P-O bond and

 $OH^{-}$ . Furthermore, the EDS detected phosphorus signal, which also supports that  $PO_4$ 394 group was in VO<sub>4</sub> site. The molar ratios of Pb/V in Figure 7 show a deficiency of Pb 395 relative to V in Na<sub>3</sub>PO<sub>4</sub> leaching test. These evidences suggest the precipitates are a 396 product of hydroxyvanadinite with mixed site:  $Pb_{10}(VO_4)_n(PO_4)_{6-n}(OH)_2$ . The site mixing 397 is possible since  $Pb_{10}(VO_4)_x(PO_4)_{6-x}(OH)_2$  can occur during wet chemistry reactions under 398 similar conditions.<sup>48</sup> Carbonate is known to be incorporated into apatite structure by 399 substitution.<sup>50–53</sup> Given that phosphate (PO<sub>4</sub><sup>3-</sup>, ionic radius  $2.30 \pm 0.42$  Å)<sup>46</sup> can replace 400 vanadate in iodoapatite,<sup>48</sup> it is reasonable to presume that carbonate of a smaller ionic 401 radius  $(CO_3^{2-}, 1.89 \pm 0.19 \text{ Å})^{46}$  can substitute vanadate in a similar crystal structure. 402 Therefore, the secondary phase formed on in the Na<sub>2</sub>CO<sub>3</sub> solution is  $Pb_{10}(VO_4)_{6-1}$ 403  $m(CO_3)_{1.5m}(OH)_2.$ 404

# 405 4.4 Mechanism of iodoapatite dissolution and surface reactions in aqueous 406 environments

Figure 8 generalizes the mechanism of iodoapatite dissolutions with multiple 407 processes contributing to the iodine release. Our previous study on iodine release in 408 deionized water suggests that the iodine release is driven by short-term diffusion and 409 long-term dissolution.<sup>29</sup> Diffusion and dissolution are affected by various factors of the 410 solution chemistry, such as solution ionic strength, pH, and secondary phase formation 411 resulted from a supersaturation of the solution with respect to low solubility species. In 412 neutral pH solutions, the iodine release is subjected to the substitution of iodine by 413 anionic species in solution such as OH<sup>-</sup> and Cl<sup>-</sup>. When dealing with solutions of 414 415 comparable pH, a higher ionic strength, due to the ionic content, can enhance the dissolution by changing saturation conditions. Solution pH other than near neutral can 416

increase the dissolution by exponentially accelerating the dissolution process. The resulting rapid dissolution can often lead to the precipitation of secondary phases when the solution approaches the supersaturation state of low solubility phases. Possible secondary phases include chervetite  $Pb_2V_2O_7$  under acidic condition<sup>37</sup> and hydroxylvanadinite  $Pb_5(VO_4)_3OH$  under basic condition.

## 422 **5** Conclusions

The present study of the effect of solution compositions on iodoapatite dissolution 423 suggests that the higher ionic strength can enhance its dissolution by decreasing the 424 activity coefficient of reacting aqueous species, and thus can promote iodine release from 425 apatite. Non-neutral pH conditions clearly enhance the dissolution rate and can often lead 426 to precipitations of secondary phases, such as chervetite and hydroxylvanadinite. The 427 secondary phase precipitation at the surfaces hinders the dissolution rate because it 428 reduces the available reacting surface area. However, the overall iodine release rates in 429 both basic and acidic solutions are exponentially higher than those in the near-neutral pH 430 conditions, especially in deionized water. These impacts of solution chemistry on 431 dissolution add complexities to the current understanding of dissolution kinetics which is 432 based on leaching experiments conducted solely in deionized water. This study suggests 433 that, compared to fresh water with low ion concentrations, high concentrations of aqueous 434 species commonly found in underground brines can compromise the chemical durability 435 of apatite waste form in a geological repository. For this specific waste form, maintaining 436 neutral pH and low ion content in aqueous solutions are important to ensure the disposal 437 safety of radioactive iodine. Since iodine is one of the most challenging radionuclides to 438

immobilize, building a comprehensive theoretical framework of iodine immobilizationcan significantly advance the research in nuclear waste disposal safety.

## 441 **Conflicts of interest**

442 There are no conflicts to declare.

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#### 453 **Date Availability**

454 Data will be made available on request

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<sup>608</sup> Figure 1.(a) Polished pristine iodoapatite samples before test, (b) iodoapatite leached

surface during the 5<sup>th</sup> replacement of Na<sub>2</sub>CO<sub>3</sub> solution, (c) surface leached by at the end

of 14-day leaching tests, SEM images of (a) a polished pristine iodoapatite and the

samples leached by (b) deionized water, (c) 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, (d) 0.1 mol/L NaCl, (e)

612 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>, and (f) 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>.



- Figure 2. EDS spectra of a pristine iodoapatite and the samples leached by deionized
- water, 0.1 mol/L NaCl, 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>, and 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>
- 617 solutions.



- Figure 3. Infrared spectroscopy of pristine iodoapatite and leached samples by
- deionized water, NaCl, Na<sub>2</sub>SO<sub>4</sub>, Na<sub>2</sub>CO<sub>3</sub>, and Na<sub>3</sub>PO<sub>4</sub> solutions.



Figure 4. XRD patterns of a pristine iodoapatite and the samples leached by deionized

625 water, 0.1 mol/L Na<sub>2</sub>SO<sub>4</sub>, 0.1 mol/L NaCl, 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, and 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>. In

addition, standard XRD spectra of iodoapatite, vanadinite, and hydroxylvanadinite are

627 listed for comparison. \* denotes the graphite impurity introduced during sample

628 synthesis.<sup>25</sup>



- Figure 5. XRD phase analysis of the iodoapatite sample surface leached by 0.1
- mol/L NaCl solution. Two phases were identified: iodoapatite and vanadinite.



Figure 6. Solution analysis of collected leachates from 14 days semi-dynamic leach
tests on iodoapatite samples in (a) 0.1 mol/L NaCl, (b) 0.1 mol/L Na<sub>2</sub>CO<sub>3</sub>, (c) 0.1 mol/L
Na<sub>2</sub>SO<sub>4</sub>, and (d) 0.1 mol/L Na<sub>3</sub>PO<sub>4</sub>.



Figure 7. Comparison of element release rate of iodine (a), vanadium (b), and lead (c) in

the leachate solutions from different leach tests. Molar ratios of Pb/V (d) and I/V (e) in
 leachate solutions from leach tests in NaCl, Na<sub>2</sub>SO<sub>4</sub>, Na<sub>2</sub>CO<sub>3</sub>, Na<sub>3</sub>PO<sub>4</sub>, and deionized

643 water.



646 Figure 8. Schematic diagram illustrates major processes that control the iodine release

647 from iodoapatite in aqueous environments

Table. 1 Crystallographic parameters based on the XRD refinements by Le Bailalgorithm.

Leach test	Refined parameters						
condition	a, b (a=b, Å)	c (Å)	GoF	R <sub>p</sub> (%)	R <sub>wp</sub> (%)		
Pristine	10.4420 (3)	7.4756 (3)	1.32	5.16	6.53		
Water	10.4325 (3)	7.4864 (3)	1.63	6.04	7.73		
0.1 mol/L Na₂SO₄	10.4336 (2)	7.4837 (2)	1.39	4.60	5.93		
0.1 mol/L Na <sub>2</sub> CO <sub>3</sub>	10.1923 (2)	7.4656 (2)	1.65	4.85	6.44		
0.1 mol/L Na₃PO₄	10.1984 (2)	7.4449 (2)	1.43	4.74	6.23		
0.1 mol/L NaCl (2 phases)	10.4443 (6)	7.4796 (5)					
(2 phases)	10.3536 (8)	7.3735(8)	1.17	4.12	5.28		
Pb <sub>4.925</sub> (VO <sub>4</sub> ) <sub>3</sub> I <sub>0.85</sub> [ICDD#04-011-4267]	10.422	7.467	-	Crystal system: hexagonal			
Pb₅(VO₄)₃(OH) [ICDD#01-075-7576]	10.2242	7.4537	Space group: P63/m #176; α=90° β=90° γ=120°				
Pb₅(VO₄)₃Cl [ICDD#01-073-1732]	10.31	7.34					

mol/L 90 °C	Deionized water	0.1 mol/L NaCl	0.1 mol/L Na₂SO₄	0.1 mol/L Na₂CO₃	0.1 mol/L Na₃PO₄
pH (unitless)	6.1	6.1	6.2	10.3	10.9
Ionic strength	2.04 × 10 <sup>-6</sup>	0.098	0.26	0.25	0.29
Major cation	H⁺	Na <sup>+</sup>	Na⁺	Na⁺	Na⁺
Concentration	6.52×10 <sup>-7</sup>	0.098	0.18	0.18	0.22
Activity	6.51×10 <sup>-7</sup>	0.074	0.13	0.13	0.15
Activity coefficient	1.00	0.76	0.72	0.72	0.68
Major anion	OH-	CI-	<b>SO</b> 4 <sup>2-</sup>	CO3 <sup>2-</sup>	PO4 <sup>3-</sup>
Concentration	8.72×10 <sup>-7</sup>	0.098	0.079	0.069	0.012
Activity	8.70×10 <sup>-7</sup>	0.074	0.02	0.017	0.00049
Activity coefficient	1.00	0.76	0.25	0.24	0.041

Table 2. Solution chemistry at equilibrium state calculated by Visual MINTEQ under90 °C.